Stoichiometry of the Photocatalytic Fuel Production by the Reformation of Aqueous Acetic Acid

Von der Naturwissenschaftlichen Fakultät der Gottfried Wilhelm Leibniz Universität Hannover

zur Erlangung des Grades

Doktorin der Naturwissenschaften (Dr. rer. nat.)

genehmigte Dissertation

von

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2018

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Tag der Promotion: 21.06.2018

Dedicated to My Parents

The ultimate measure of a man is not where he stands in moments of comfort and convenience, but where he stands at time of challenges and controversy.

Martin Luther King, Jr.

Acknowledgements

Acknowledgements

First of all, I would like to express my deepest gratitude to my supervisor, **Prof. Dr. Detlef Bahnemann**, for giving me the opportunity to work under his kind supervision. His excellent academic guidance, inspiring and enthusiastic reviews, motivational support and discussions are much esteemed.

I would also like to thank **Prof. Dr. Thomas Scheper** for agreeing to be a referee of my thesis. My sincere thanks also go to **Prof. Dr. Nadja-Carola Bigall** for showing her consent to act as a co-referee of my thesis.

For the financial support during my research work, I would like to thank **Bundesministerium für Bildung und Forschung (BMBF) (Project 'Duasol' Nr. 03SF0482C).**

I would also like to extend my sincere and special appreciation to **Dr. Ralf Dillert** for his valuable input in terms of thoughtful scientific discussions as well as his great help throughout my Ph. D. His efforts and way of teaching is greatly appreciated.

In addition, I would also convey my intimate gratitude to **Dr. Jenny Schneider** and **Dr. Irina Ivanova** for their academic guidance as well as friendly support during my stay in Germany.

For their continuous support to carry out analytical characterizations including XRD, NMR and TEM measurements, I would also like to thank **Prof. Dr. Armin Feldhoff** at the Institut für Physikalische Chemie und Elektrochemie, Leibniz Universität Hannover, **Dr. Jörg Fohrer**, Institut für Organische Chemie, Leibniz Universität Hannover and Laboratorium für Nano- und Quantenengineering, Leibniz Universität Hannover, respectively.

My sincere appreciation also goes to **Mrs. Kerstin Hellmuth** (Leibnizhaus / administrator) for her emotional and friendly support during my stay in Germany.

In any organization, the qualitative and comfortable environment at the work place plays a very constructive role in one's performance towards his/her duties. For this, I would like to thank all members in the research group of Prof. Bahnemann (AK Bahnemann) for their help, cooperation and maintaining a very friendly environment. Ph. D. itself isn't an easy title to earn. However, presence of some loving and caring friends in life makes its realization comparatively easier. I also consider myself lucky enough to have some good friends including **Narmina Balayeva**, and

Dr. Didem Muharrem Seleci, who stood with me in all hard times and, therefore, feel extremely grateful to all of them.

Acknowledgements

Last but by no means the least, I'm extremely indebted to my beloved family which has truly been the driving force behind all this hard work and success! I wouldn't hesitate to acknowledge all their names starting from **Samina Hamid** (my beloved mother), **Hamid Ali Mukhtar** (an affectionate father), **Dr. Muhammad Fahad Ehsan** (my loving husband, without whose continuous support and encouragement this wouldn't have been possible), **Muhammad Zayan Fahad** (the love of my life, my son), **Sadaf Yasir** (my friend cum elder sister), **Ahsan Hamid** (a caring younger brother) and my in-laws. Without their prayers, support, and motivation, I would have never been able to achieve this Ph. D. degree.

Kurzzusammenfassung

In den letzten Jahren haben photokatalytische Reaktionssysteme viel Aufmerksamkeit erregt, um sowohl Energie- als auch Umweltprobleme zu beheben. Eine dieser photokatalytischen Reaktionen umfasst die Umwandlung von wässrigen organischen Schadstoffen, die aus Industrieabfällen resultieren, in nutzbare Kraftstoffe (d.h. H₂ und Kohlenwasserstoffe) mittels Solarlicht. Mangelndes Verständnis für den Reaktionsmechanismus beschränkt jedoch die praktische Realisierung dieser Systeme. Daher ist die Grundlagenforschung auf diesem Gebiet sehr wichtig, um die photokatalytische Effizienz dieser Systeme zu verbessern.

Diese Arbeit befasst sich mit der gleichzeitigen molekularen Wasserstoffproduktion und dem Abbau organischer Schadstoffe. Essigsäure (CH₃COOH) wurde als organischer Modell-Schadstoff und mit Co-Katalysator geladenes TiO₂ als Photokatalysator verwendet. Die Parameter, die die photokatalytische Umwandlung von wässriger Essigsäure in Kohlendioxid (CO₂), molekularen Wasserstoff (H₂), Methan (CH₄) und Ethan (C₂H₆) unter Verwendung von Co-Katalysator-beladenen TiO₂-Partikeln unter anaeroben Bedingungen beeinflussen, wurden untersucht. Verschiedene Metalle und Metalloxide wie Pt, Rh, Au, Ag, IrO2 und RuO2 wurden auf die Oberfläche von TiO2 als Elektronenakzeptoren aufgebracht, was die Reduktionsreaktion (d.h. die Bildung von H₂) erleichterte. Die beobachteten Mengen an CO₂ und CH₄ stiegen in folgender Reihenfolge an: Ag/ $TiO_2 <$ Au/ $TiO_2 <$ Rh/ $TiO_2 <$ RuO₂/ $TiO_2 <$ IrO₂/ $TiO_2 <$ Pt/ TiO₂. Im Gegensatz dazu war die Reihenfolge, in der die entwickelten Mengen an H₂ zunahmen, relativ unterschiedlich. Es wurde beobachtet, dass die Bildungsraten der Hauptreaktionsprodukte (CO₂, H₂, CH₄ und C₂H₆) und ihre entsprechende Produktverteilung stark sowohl von (1) der Konzentration der Essigsäure als auch von (2) der Beladung des Photokatalysators mit verschiedenen Metallen und Metalloxide beeinflusst worden ist. Es wurde gefunden, dass die Co-Katalysatoren mit höheren Werten der Austrittsarbeit, die H2 -Entwicklungsreaktion bei niedrigeren Konzentrationen von Essigsäure erleichtern. Unter Verwendung höherer Essigsäurekonzentrationen wurden die Reaktionsprodukte, die aus einem mit Kohlenwasserstoffen angereicherten Gasgemisch bestanden, unter Verwendung des Co-Katalysators mit niedrigeren Werten der Austrittsarbeit (Ag und IrO₂) erhalten. Es wurde festgestellt, dass der pH-Wert der verwendeten Suspension eine Schlüsselrolle bei der Wahl der

Kurzzusammenfassung

Reaktionswege für die photokatalytische Zersetzung von wässriger Essigsäure spielt. Es wurde festgestellt, dass eine Erhöhung des pH-Werts vom Sauren zum Basischen zu völlig unterschiedlichen Verhältnissen zwischen den entwickelten Mengen an H₂ und Kohlenwasserstoffen führt. Zum Beispiel ist bei einem pH-Wert von 2 das Verhältnis $\frac{n(H_2)}{n(CH_2)} = 0.6$ und bei einem pH-Wert von 9 das Verhältnis $\frac{n(H_2)}{n(CH_4)}$ = 58. Stöchiometrische Berechnungen für die entwickelten Mengen der Hauptreaktionsprodukte zeigen eindeutig die Bildung anderer organischer Zwischenprodukte während der photoinduzierten Umwandlung von wässriger Essigsäure an. In Abhängigkeit vom pH-Wert der Suspension wurde beobachtet, dass der photokatalytische Abbau von Essigsäure unterschiedlichen Reaktionsmechanismen folgt. Um die Ergebnisse der lichtinduzierten Umwandlung von wässriger Essigsäure zu interpretieren, wurden Experimente mit markierten Isotopen durchgeführt. Diese Experimente sollen Aufschluss über den Ursprung von entwickeltem H₂ und CH₄ durch Analyse der Protonenaustauschreaktion zwischen Essigsäure und Wassermolekül geben. Ein detaillierter Mechanismus für die photokatalytische Zersetzung von wässriger Essigsäure wurde anhand der Resultate erstellt.

Stichwörter: Photokatalyse, Essigsäure, Cokatalysator-beladenes TiO₂, Oberflächenladung, H/D-Austauschreaktion, Solarbrennstoff.

Abstract

Abstract

In recent years, photocatalytic reaction systems gained much attention to address both energy and environmental issues. One of these photocatalytic reactions involve the conversion of aqueous organic pollutants resulting from industrial waste into value added fuels (*i.e.*, H₂, and hydrocarbons) by means of solar-light. However, less understanding about reaction mechanism limits the practical realization of such vital process. Therefore, fundamental research in this field is very important to improve the photocatalytic efficiency of these systems.

This work is an assessment for the simultaneous molecular hydrogen production and organic pollutant degradation. Acetic acid (CH₃COOH) has been used as a model organic pollutant and co-catalyst loaded TiO₂ as the photocatalyst. The parameters influencing the photocatalytic conversion of aqueous acetic acid into carbon dioxide (CO₂), molecular hydrogen (H₂), methane (CH₄) and ethane (C₂H₆) employing co-catalysts loaded TiO₂ particles under anaerobic conditions have been investigated. Various metals and metal oxides such as Pt, Rh, Au, Ag, IrO₂, and RuO₂ were loaded onto the surface of TiO₂ acting as efficient electron traps while facilitating the reduction reaction (*i.e.*, formation of H₂). The evolved amounts of CO₂ and CH₄ were observed to increase in the following sequence: $Ag/TiO_2 < Au/TiO_2 < Rh/TiO_2 < RuO_2/TiO_2 < Ch/TiO_2 < Ch$ $IrO_2/TiO_2 < Pt/TiO_2$. On the contrary, the order in which evolved amounts of H₂ increased was relatively different. The formation rates of the main reaction products (CO₂, H₂, CH₄, and C₂H₆) and their corresponding product distribution were observed to be strongly affected by both (1) the concentration of acetic acid, and (2) the loading of photocatalyst with various metals and metal oxides. The co-catalysts having higher values of work function were found to facilitate the H₂ evolution reaction at lower concentrations of acetic acid. Employing higher acetic acid concentrations, the reaction products consisting of a gas mixture enriched with hydrocarbons were obtained by using the co-catalyst with lower values of the work function (Ag and IrO₂). The pH value of the employed suspension was found to play a key role in defining the reaction pathways for the photocatalytic decomposition of aqueous acetic acid. An increase in pH value from more acidic to more basic media was observed to result in entirely different ratios between evolved amounts of H₂ and hydrocarbons. For example, at pH 2 the ratio: $\frac{n(H_2)}{n(CH_4)} = 0.6$, which becomes: $\frac{n(H_2)}{n(CH_4)} = 58$ at pH 9. Stoichiometric calculations for the evolved amounts of the main

Abstract

reaction products clearly indicate the formation of other organic probe molecules during the photo-induced transformation of aqueous acetic acid. Depending on the pH value of the suspension, the photocatalytic degradation of acetic acid was observed to follow different reaction mechanisms. For the first time, isotopic labelling experiments were performed in order to interpret the results obtained from the light-induced conversion of aqueous acetic acid. These experiments were carried out mainly to see the origin of evolved H_2 and CH_4 by analysing the proton exchange reaction between acetic acid and water molecules. A detailed mechanism for the photocatalytic decomposition of aqueous acetic acid has been elucidated.

Keywords: photocatalysis, acetic acid, co-catalyst loaded TiO₂, surface charge, H/D exchange reaction, solar fuel.

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Abbreviations

SC	Semiconductor
XRD	X-ray Diffraction
TEM	Transmission Electron Microscopy
BET	Specific Surface Area (Brunauer-Emmett-Teller)
UV	Ultraviolet
Vis	Visible
QMS	Quadrupole Mass Spectrometer
NMR	Nuclear Magnetic Resonance
EPR	Electron Paramagnetic Resonance
HER	Hydrogen Evolution Reaction
NHE	Normal Hydrogen Electrode
PER	Proton Exchange Reaction
c_0	Initial Concentration
n_0	Initial Number of Moles

Symbols

ΔG^0	Gibbs Free Energy
E _{CB}	Conduction Band Edge
E _{VB}	Valance Band Edge
Eg	Band Gap Energy
e _{CB}	Conduction Band Electrons
h_{VB}^+	Valance Band Holes
Φ	Work Function
ζ	Photonic Efficiency
λ	Wavelength
h	Planck's Constant
С	Speed of Light

Abbreviations

I ₀	Number of Absorbed Photons
N _A	Avogadro Constant
Α	Illuminated Area
d	Diameter
π	Mathematical Constant
рК _а	Dissociation Constant
pH _{zpc}	Point of Zero Charge
•ОН	Hydroxyl Radical
•CH ₃	Methyl Radical

Units

TW	Terawatt
μmol	Micromole
h	Hour
mL	Mililiter
a.u.	Arbitrary Units
%	Percentage
wt %	Percentage by Weight
°C	Grad Celsius
g	Grams
М	Molar Mass
V	Volume
L	Liter
J	Joule
eV	Electron Volt
mW	Milliwatt
cm	Centimeter
nm	Nanometer
Å	Ångström

1. Introduction

Energy demands and related environmental problems are the growing concern of the present era. In 2010, the worldwide average energy consumption rate was $\approx 15 - 17$ TW, which is expected to boost around 25 - 27 TW by 2050 [1]. Currently, $\approx 85\%$ of world's energy requirements is fulfilled by the fossil fuels (Figure 1). However, the 21st century started with the realization to explore long term solutions for readily depleting fossil fuels, which dominated in the past. Other than the depletion, their combustion also results in the formation of carbon dioxide (CO₂) being released directly into the environment which is a greenhouse gas and a primary contributor towards global warming [2]. In order to meet the world's energy demands, photocatalytic water splitting into molecular hydrogen (H₂) and molecular oxygen (O₂) as well as the photocatalytic reforming of aqueous organic/inorganic compounds from industrial wastes into value-added fuels (*i.e.* H₂ and hydrocarbons) has been the focus of attention for scientists since the last four decades.

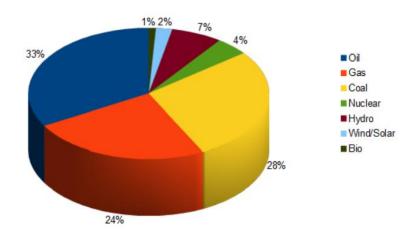


Figure 1: Global primary energy consumption by 2016 [3]

1.1 Historical background

For the first time in 1911, the word 'photocatalysis' appeared in some scientific communications, almost 76 years later the term 'catalysis' introduced by Berzelius. Only preliminary experiments

had been done in this field by 1970's [4-7]. However, in early 1970's, the first world's energy crisis came into view due to the economic situation in Arab petroleum exporting countries thus leading to the future scarceness of oil availability. This oil crisis then forced scientists to think about an alternative as well as renewable energy source. During this time (in 1972), two Japanese scientists, Fujishima and Honda [8], performed water (H₂O) photolysis experiments on an electrochemical set-up employing rutile TiO₂ as anode and platinum (Pt) as cathode. They used near UV light and obtained a water splitting reaction into H₂ and O₂. The idea behind these experiments was to obtain H₂ gas from solar light induced water splitting, which then can be used as a renewable energy fuel. In particular, H₂ is a main energy-dense fuel and acquired from an abundantly available source (H_2O). When H_2 is used either in a fuel cell or burnt directly, it only generates H_2O in reversible reaction and does not result in any pollutants or greenhouse gases [9, 10]. The report published by Fujishima and Honda [8] opened new horizons for scientists to develop the possibilities for significant H₂ production from immensely available sources *i.e.*, H₂O and sunlight. The concept of photocatalysis is actually generated from the natural photosynthesis process, where plants absorb solar energy from sunlight and convert it into the chemical energy (Figure 2).

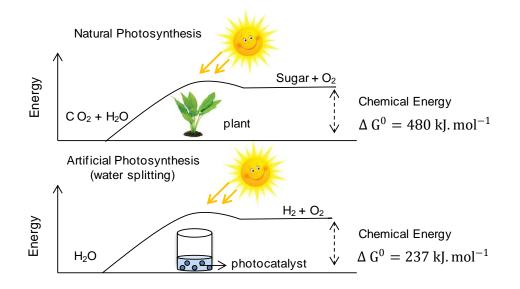


Figure 2: Natural photosynthesis vs. artificial photosynthesis.

The chemical energy is stored in the bonds of glucose along with a huge positive change in the Gibbs free energy ($\Delta G^0 = 480 \text{ kJ} \cdot \text{mol}^{-1}$) as shown in Figure 2. Similarly, the decomposition of H₂O molecule into H₂ and O₂ employing sunlight and a photocatalyst material mimics the natural photosynthesis reaction thus providing a very attractive method for the conversion of readily available solar energy into the chemical energy (*i.e.*, H₂) [11, 12]. The solar H₂ produced by this method can efficiently fulfill the world's electricity as well the chemical energy needs, by powering a small mobile phone to submarine [13].

In photocatalytic reactions, usually semiconductor (SC) materials are employed as photocatalysts [14]. According to the pioneering report published by Fujishima and Honda [8], a complete photocatalytic water splitting reaction was achieved only in the presence of a single-crystal titania (TiO₂) anode and Pt cathode while applying an external bias along with UV irradiation. From a practical point of view, the fabrication of appropriate photo anode materials with suitable band gap structures is rather an expensive and complicated process. Therefore, by 1980's, the principle of photocatalytic SC cell was extended to the SC particulate suspension systems in order to obtain the required reactions.

The use of SC particulate system was first initiated by Bard and co-workers [15-17], where they employed Pt loaded TiO_2 particles representing a short-circuit photoelectrochemical (PEC) cell. These SC particulate systems appeared to be cost effective as well as much simpler to synthesize in comparison to the single crystal SC electrodes. Moreover, the light absorption efficiency of suspensions can be much higher than SC electrodes. Another advantage of using the particulate system is that a variety of materials can be employed as photocatalysts which might not be available as single-crystal electrodes due to their high resistivity[18]. Finally, the photocatalytic particulate SC reaction systems exhibit a vast range of potential applications, when large-scale H₂ production is considered [19].

On the contrary, in a photocatalytic reaction system, the SC particulates have very low spatial separation among oxidative and reductive sites hence giving rise to an undesired back reaction *i.e.*, formation of H₂O [17]. Thus, the efficiency of a photocatalytic water splitting reaction into H₂ and O₂ employing particulate system becomes very low in comparison to a PEC cell system. It has been reported in literature that by using photocatalytic particulate semiconductor systems, the H₂O decomposition reaction into H₂ and O₂ can only be obtained at higher temperature or reduced pressure values [20]. Therefore, according to the economical perspective, the

photocatalytic splitting of H_2O into H_2 and O_2 seemed to be uncompetitive. Alternatively, many scientific reports are also published in literature demonstrating the mineralization of organic waste water by means of photocatalysis [21, 22]. Technical systems for the photocatalytic waste water treatment were already designed and tested successfully on the pilot plant scale [23-25]. However, at ambient temperature, the photocatalytic conversion of H_2O into considerable amounts of H_2 employing semiconductor particles can only be obtained in the presence of organic/inorganic compounds *i.e.*, alcohols, carboxylic acids, and sulfides [13, 26-29]. Hence, simultaneous waste water treatment and H_2 evolution *via* photocatalysis has been recommended while employing a SC particulate system [30]. The advantage of this reaction system is that in one reaction, two important aspects of current era can be addressed *i.e.*, (1) formation of H_2 , which can be used as a fuel and (2) degradation of organic compounds present in waste water resulting from the industrial wastes thus solving the environmental problems.

Even though a large number of efforts have been made in the past 40 years after the initiative work of Bard and co-workers, a photocatalytic reaction system producing significant amounts of H_2 has not been achieved for its practical realization. So, it is very important to continue the fundamental research in this field with the aim to develop a reproducible and efficient reaction system in order to meet world's energy requirements, where H_2 can be used as a solar fuel and industrial waste can be converted into useful reaction products.

1.2 Literature survey

1.2.1 Molecular hydrogen and methane as energy fuels

1.2.1.1 H₂ production

 H_2 is amongst the most common elements present on the earth, while the occurrence of H_2 in its elemental form does not exist in significant amounts. Usually, it appears in H_2O and biomass. At present, the primary sources for the production of H_2 gas include: organic wastes, hydropower, heavy oil, coal, solar and wind energy etc., [26]. Now a day, for the production of ammonia, H_2 gas is a pre-requisite. Also the use of H_2 in chemical processes *e.g.*, sulfur removal from gasoline, transformation of heavy hydrocarbons into the diesel fuel, etc., cannot be neglected. Therefore,

the demand of H_2 gas is increasing day by day. Other than these traditional uses, the idea to use H_2 gas as an energy fuel is considered as a breakthrough in order to meet the worldwide energy requirements. The advantage of using H_2 gas as a transportation fuel is that the chemical energy stored in the H-H bond can be utilized by reaction with O_2 while forming H_2O as the final product. Consequently the combustion of H_2 fuel will result in a pollution-free environment. Currently, the steam methane reforming (SMR) process has been used by the industries for the synthesis of H_2 gas [31]. However, SMR is a complicated process which involves many catalytic steps for the H_2 production. According to the present scenario, the conversion of wastewater, resulting mainly from industries, into H_2 and valuable fuels employing sunlight would be an intermediate step in-between the current fossil fuel reforming process and the dream of solar energy utilization for various applications. Thus, simultaneous H_2 production and organic pollutant degradation achieved in one reaction system employing solar light is assumed to provide a clean environment and long-term solutions for global energy needs.

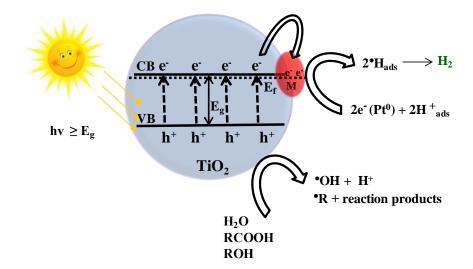
1.2.1.2 CH₄ production

Almost 95% of natural gas consists of CH₄, while it also contains other hydrocarbons such as ethane (C₂H₆) and propane (C₃H₈) in minor percentages. Generally, CH₄ is regarded as a clean energy fuel because its molecular structure is comprised of one carbon (C) atom attached to the 4 hydrogen (H) atoms. In comparison to the diesel which contains complicated long chain organic molecules and produces hazardous compounds upon its combustion, the burning of CH₄ results in the formation of minor amounts of CO₂ and water only (CH₄ + 2O₂ \rightarrow CO₂ + 2H₂O + energy). While using it as a transportation fuel, CH₄ releases almost 29 % less CO₂ in the environment as compared to the diesel and petroleum. However, the current process (fossil fuels incineration) for CH₄ generation is not environment friendly and requires elevated temperature conditions. Also, the burning of fossil fuels, in order to produce CH₄, directly releases dangerous gases to the environment thus contributing in the air pollution. Hence, the idea to produce CH₄ by photocatalytic conversion of industrial organic waste can simultaneously solve both energy and environmental problems.

1.2.2 The principle of semiconductor photocatalysis

In photocatalytic reactions, semiconductor (SC) materials are of great importance with respect to their electronic structure and corresponding electronic properties. For instance, SC materials are comprised of a band structure which includes valence band (VB) and conduction band (CB), while the difference between VB and CB with an appropriate width is regarded as the band-gap energy (E_g) of SC. The E_g of SC materials plays a key role while defining the wavelength sensitivity for its irradiation [32]. According to the electronic properties of a SC, it can be further categorized as a (1) direct band-gap and (2) indirect band-gap semiconductor. For example, cadmium sulfide and zinc sulfide which are direct bad-gap SC materials having higher absorption coefficients and exhibit a steep absorption onset. In comparison to this, TiO₂ which is an indirect band-gap SC material shows an absorption tail and flat onset [32].

Upon illumination, a SC material absorbs photons having energy equal or higher than its E_g . As a result, electrons (e⁻) and holes (h⁺) are generated in the CB and VB of SC, respectively. These photo-generated charge carriers (conduction band electrons (e_{CB}^-) and valence band electrons (h_{VB}^+)) can either migrate to the SC surface or they can recombine while releasing energy in the form of heat/photons. The direct photocatalytic water splitting for H₂ production is mainly limited by the fast recombination rate of photo-generated charge carriers, which results in a poor photocatalytic activity [14]. However in a photocatalytic reaction, where organic pollutants are employed as sacrificial reagents and a metal is loaded on the surface of the photo-generated charge carriers (h_{VB}^+ and e_{CB}^-). For example, adsorbed molecules of H₂O and employed organic pollutant oxidized by h_{VB}^+ lead to the formation of H⁺, [•]OH, [•]R intermediates and other reaction products. On the other hand, at the same time, a reduction reaction mainly at the surface of metal loaded onto the SC particles is carried out by the e_{CB}^- leading to the formation of H₂ as a final product.



 $R = CH_3$, M = metal loaded on SC surface

Figure 3: Basic principle of photocatalysis employing metal loaded semiconductor (SC) particulate system and aqueous organic pollutant.

1.2.3 Semiconductor surface modifications

1.2.3.1 TiO₂ based photocatalysts

A wide variety of semiconductor (SC) materials has been employed as photocatalysts [38]. Among various n-type SC materials, titanium dioxide (TiO₂) is found to be one of the most active photocatalysts for the hydrogen evolution reaction (HER) till date [14, 39, 40]. On one side, its low cost, high stability and non-toxic nature, and on the other side, its suitable electronic band alignments such as position of conduction band (CB) and valence band (VB) to achieve a simultaneous redox reaction for aqueous organic compound decomposition makes TiO₂ one of the most attractive photocatalysts [40]. A large number of reports have been published in literature demonstrating the efficient photocatalytic activities employing TiO₂ for HER [33, 34, 41-44]. In general, the photocatalytic activity by using bare TiO₂ particles even in the presence of organic electron donors is very low. Therefore, TiO₂ has been used with various surface modifications, so that an efficient amount of H₂ can be produce.

1.2.3.2 Nobel metal co-catalysts

The activity of a photocatalytic reaction is primarily reliant on the efficient separation of photogenerated charge carriers (*i.e.*, e_{CB}^- and h_{VB}^+) and their transport. However, the fast recombination of photo-generated charge carriers is one of the biggest limitations in this field and hence very challenging to overcome. In order to solve the complexity of rapid e_{CB}^- and h_{VB}^+ recombination, metal/SC heterojunction systems have been used extensively. Usually, noble metals are loaded on the surface of SC material where they play a key role while improving the efficiency for hydrogen evolution reaction (HER) [45-49].

When noble metals are deposited on the semiconductor (SC) surface, the migration of photogenerated charge carriers is significantly enhanced instead of their prompt recombination [50, 51]. Typically, in metal/SC heterojunction systems, a Schottky barrier is formed at the metal/SC interface due to which noble metals act as efficient electron traps while facilitating the reduction reaction (*e.g.*, formation of H₂) [52]. In addition to this, the noble metals and SC material have different Fermi level positions (E_t). Therefore, when they combine with each other, the electrons start migrating from the CB of SC located at more negative values to the CB of metal having comparatively more positive values. As a result, the metal surface gets saturated with electrons while leaving the SC depleted with electrons. Due to the excess negative charges appeared at the metal/SC interface, the SC bands bend in the direction of metal/SC contact. Hence, this formed barrier is called a Schottky barrier which acts as to hinder the unwanted back reaction *e.g.*, reverse transport of electrons to the SC as shown in Figure 4 [40]. During a photocatalytic reaction, when photo-generated e_{CB}^- are trapped at the surface of so called co-catalyst (noble metals), the photogenerated h_{VB}^+ remain at the surface of host SC photocatalyst thereby facilitating the efficient charge separation [53, 54].

In particular, the concept of Schottky barrier formation is recommended for photoelectrochemical (PEC) cell, where an interfacial contact is developed between metal (*e.g.*, Pt electrode) and n-type SC (*e.g.*, TiO₂ electrode). Conversely, in particulate systems where the surface of SC is loaded with metal nanoparticles, the formation of a Schottky barrier could be highly questionable. For instance, Litter *et al.* [55] reported the formation of different oxidation states for Pt nanoparticles as Pt⁰, Pt⁺² and Pt⁺⁴ while employing Pt/TiO₂ particles.

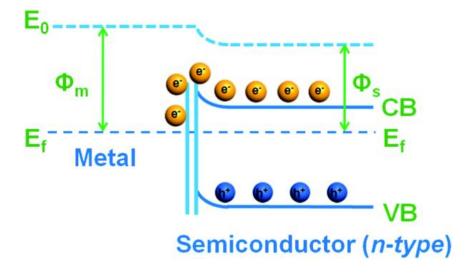


Figure 4: Formation of a Schottky barrier at the metal/SC interface in the equilibrium. $E_f =$ Fermi level of metal, $E_0 =$ vacuum level, $\Phi_M =$ the work function of metal, $\Phi_S =$ Schottky barrier height [54].

One of the most important parameter while choosing the suitable co-catalyst is its work function (Φ) value. The Φ is defined as the energy needed to transfer an electron from the E_f to the vacuum. The higher Φ means a lower E_f and bigger energy difference between metal/SC interface thus enhancing photo-generated charge separation [56].

Typically, two methods are commonly used for the deposition of metal nanoparticles on the surface of photocatalyst: (1) Impregnation method, where the specific metal precursor in the form of solution is mixed with the photocatalyst. Afterwards, a thermal treatment is given to this mixture according to the desired co-catalyst requirements [53]. (2) The second method is called as: *in*-situ photodeposition, where the mixture of SC powders and specific metal ions is irradiated in the presence of an appropriate holes scavenger. The metal cations are reduced by the SC electrons thus creating active sites on the SC surface in the form of metal nanoparticles [53]. Eastman *et al.* [57] examined the effect of various metal loadings including platinum (Pt), gold (Au) and silver (Ag) on the surface of TiO₂. In their studies, Pt was found to be the most active co-catalyst followed by Au and Ag. The author explained the difference in the catalytic activities with respect to the Φ values of the employed metal. For instance, the $\Phi_{Pt} = 5.65 \text{ eV}$, $\Phi_{Au} = 5.10 \text{ eV}$ and $\Phi_{Ag} = 4.00 \text{ eV}$. Anpo *et al.* [58] studied the light-induced electron transfer reaction from TiO₂ to Pt particles *via* electron spin resonance (EPR) spectroscopy. Anpo and co-workers

observed that the presence of Pt islands on the surface of TiO_2 results in a reduced Ti^{3+} species meaning that the significant electron migration occurs from TiO₂ to the Pt particles. The electrons gathered at Pt particles can then react with the surface adsorbed protons (H⁺) thus reducing the H^+ into hydrogen atoms (H^{\bullet}). These adsorbed H^{\bullet} subsequently combine with each other while forming H₂ as a reaction product. They also stated that the H₂O reduction overpotential is reduced in the presence of Pt nanoparticles, so a significant hydrogen evolution reaction (HER) can be obtained. Nevertheless, depending on the electronic structures of various photocatalysts, Pt does not always illustrate the highest photocatalytic activity when compared with other noble metal co-catalysts. Hara et al. [59] observed the effect of numerous metal loadings on tantalum oxynitride (TaON) photocatalysts and found only Ru/TaON as an active photocatalyst. Their study showed that the deposition of Pt, Ir and Rh on the surface of TaON results in a poor HER as compared to Ru/TaON. The authors related this observation with the electronic properties developed in between the Ru and TaON, which efficiently promote the electron transfer from TaON to Ru. In another study, Kennedy et al. [60] demonstrated the bimetallic/TiO₂ particulates resulting in a significant HER. They deposited Au-Ag particles on the surface of TiO₂ and compared the obtained results with those acquired by the deposition of Au and Ag separately on the surface of TiO₂. The enhanced amounts from HER were observed by Kennedy and coworkers only in the presence of bimetallic/TiO₂ particles. They claimed that the presence of two metals on TiO₂ surface leads the electron transportation from one metal surface to another, hence resulting in the longer life time of photo-generated charge carriers thus significantly increasing the amounts of H₂ formation.

Recently, Chen *et al.* [61] published a report exhibiting the comparison between the employment of expensive metal (Au) and low cost metallic Nickel (Ni) nanoparticles onto TiO₂ for HER. They prepared Ni nanoparticles with particle size ranging between of 1- 2 nm, and provided experimental evidences confirming the formation of Ni⁰/TiO₂ as the leading Ni specie. The authors claimed that the comparative amounts of H₂ were produced while employing Au/TiO₂ and Ni/TiO₂ as photocatalysts. Chen and co-workers also claimed that Ni particles were highly dispersed on the surface of TiO₂, and can be efficiently employed as a replacement of expensive noble metal co-catalysts *e. g.*, Pt or Au. This means that, while choosing a suitable co-catalyst, the high Φ value of metal co-catalysts is not the only parameter that should be considered. There are other factors that should not be neglected, for instance, the size of metal nanoparticles, the physical characteristic of interface between the metal and SC, and the contact between metal ions and the photocatalyst surface, etc., [62].

1.2.3.3 Metal-oxide co-catalysts

In general, there are two main properties a co-catalyst should have: (1) the ability to extract either photo-generated e_{CB}^- or h_{VB}^+ from the surface of photocatalyst, and (2) the capability to create active reaction sites while decreasing the activation energy for the gas formation. Even though noble metal co-catalysts act as competent electron traps, a major drawback of their utilization is that they also catalyze the undesired reverse reaction, *e.g.*, H₂O formation from the dissolved H₂ and O₂ in the suspension system [63]. In addition to this, the higher cost of noble metals limits their practical realization. Therefore, research has now also focused on the use of transition metal oxides *e.g.*, Ru₂O, IrO₂, Cu_xO, CuO as co-catalysts. However, depending on their oxidation states, metal oxides often facilitate the oxidation reaction such as the degradation of H₂O or employed organic pollutant molecules [13, 64-67].

Foo and co-workers [68] studied the effect of copper (II) oxide (CuO) nanoparticles on the TiO₂ surface for HER. In their work, three types of copper such as Cu–CuO–Cu₂O were detected during different reaction stages. The authors state that the Cu is reduced to Cu₂O during the photocatalytic reaction. They also observed the formation of Cu–Cu₂O where Cu served as a core and Cu₂O depicts the formation of thin shells around Cu core. Hence, the significant amount of H₂ formation was attributed in their studies to the high surface area of Cu–Cu₂O_{thin shell}/TiO₂ particles and the corresponding less surface defects. In another study, Moon *et al.* [69] showed that the size-tuneable CuO nanodots deposited on the TiO₂ surface result in an enhanced amount of H₂ formation. In the presence of a sacrificial reagent, they observed the reduction of CuO nanoparticles into Cu⁰. The Cu nanoparticles then fulfil the requirements of an efficient electron trap while acting as a co-catalyst and assisting the reduction reaction *i.e.*, formation of H₂. They asserted that the H₂ formation rates obtained by the employment of Cu nanodots/TiO₂ particulate systems could reach to the half of the H₂ formation rate achieved by expensive Pt/TiO₂ system.

In many studies, RuO_2 has also been investigated and assumed to be an appropriate co-catalyst for HER due to its metallic characteristics [70]. Recently, Uddin *et al.* [71] examined the role of RuO_2 loadings for HER on the surface of mesoporous TiO₂ particles. The mechanistic studies

have been carried out in their work *via* EPR spectroscopy. The obtained results from EPR investigations for the bare TiO₂ particles demonstrated fewer amounts of trapped electrons (Ti³⁺) and trapped holes (O⁻). On the other hand, RuO₂/TiO₂ particles revealed the generation of Ti³⁺ and O⁻ species in much higher amounts. This means that deposition of RuO₂ onto the surface of TiO₂ gives an efficient photo-generated charge separation thus leading to an enhanced amount of H₂ formation. In comparison to this, the recombination of photo-generated charge carriers was observed to be very high in case of bare TiO₂ and was confirmed by the EPR signal intensity. Moreover, the authors also observed that the amount of co-catalyst loading is a very important parameter and should be chosen appropriately. Uddin and co-workers found 5 wt % RuO₂/TiO₂ as the optimized photocatalyst while exhibiting H₂ formation rate as 618 µmol h⁻¹. Conversely, bare TiO₂ produced only 29 µmol h⁻¹ in their experiments. They ascribed significant amount of H₂ formation to the favourable band-bending which occurs at the RuO₂/TiO₂ interface.

Nevertheless, the use of metal oxides as co-catalysts mainly for HER is a tricky process and, therefore, requires an activation treatment. For example, special synthesis parameters are applied to achieve an appropriate oxidation state that should be suitable to attain an efficient HER [72, 73]. Also, there appear limitations while applying this approach for some photocatalyst materials e.g., oxynitrides, which are thermally unstable and cannot stand with all the treatments required to acquire desired oxidation states for transition metal oxides co-catalysts [74]. Hence, it has been suggested by Domen *et al.* [75] that the utilization of dual co-catalysts consisting of a metal core such as Rh, Ir, Pt and a metal oxide shell such as Cr_2O_3 can solve this difficulty to some extent. Another advantage of employment of these core-shell particles is that they can be deposited on the surface of photocatalysts by a simple *in*-situ photodeposition method.

Moreover, Khan *et al.* [76] illustrated the effect of dual co-catalyst in one of their latest reports where one co-catalyst is considered to lead the reduction reaction and other improves the simultaneous oxidation reaction. In their studies, experiments were performed by using CoO_x/TiO_2 and Palladium (Pd)/CoO_x/TiO_2 composites. It has been observed by Khan and coworkers that the presence of CoO_x on the surface of TiO_2 acts as to scavenge h_{VB}^+ from TiO_2 instead of their reduction into Co^{2+} hence resulting in an enhanced amount of H₂ formation. Further analysis of their data depicts that the deposition of Pd nanoparticles onto the composite CoO_x/TiO_2 increased the H₂ formation to a great extent. They stated that the transfer of electrons arises from the VB of CoO into the VB of TiO₂ thus improving the oxidation reaction for H₂O

molecules. At the same time, Pd nanoparticles provide more reduction sites hence improving the formation of H_2 . In this way, the undesired back reaction *i.e.*, formation of H_2O , can be overcome.

1.2.4 Acetic acid as an organic pollutant

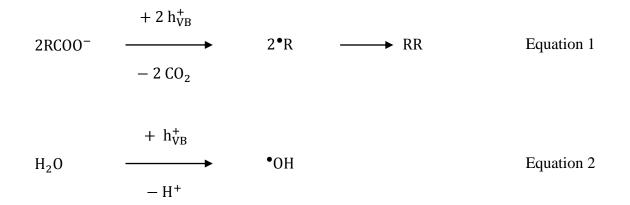
Generally, in photocatalytic reforming reactions, alcohols, formaldehydes and carboxylic acids are employed as organic pollutants acting as sacrificial reagents [13]. Acetic acid (CH₃COOH) is one of the common organic compounds resulting from industrial waste. At higher temperatures (> 39 °C) values, the concentrated form of acetic acid converts into explosive vapours [77], so its degradation is very important. At present, the decomposition of acetic acid is widely carried out by the acidolysis process. A major drawback of the acidolysis method is the requirement of elevated temperatures and special experimental conditions [78]. However, the conversion of acetic acid by means of photocatalysis into useful fuels is an environment friendly procedure that doesn't necessitate expensive experimental techniques and high temperature conditions. The photocatalytic decomposition of aqueous acetic acid has been reported under both: (1) aerobic (in the presence of air/O₂) [79-81], and (2) anaerobic (in the absence of air/O₂) [37, 82, 83] conditions. However, depending on different reaction conditions, the reaction products and their distribution were observed to vary greatly.

Usually, the photocatalytic degradation of aqueous acetic acid results in the formation of alcohols and organic acids *e.g.*, CH₃OH, HCHO, HCOOH, HOCH₂COOH, and OHCCOOH etc., as final reaction products in an air/O₂ atmosphere [79]. On the other hand, the photocatalytic conversion of aqueous acetic acid in the absence of air/O₂ yields H₂ and hydrocarbons (*i.e.*, CH₄ and C₂H₆) in significant amounts which can be used as renewable solar fuels [83].

1.2.4.1 Photocatalytic oxidation of aqueous acetic acid in the presence of air/O₂

For a typical reaction system containing SC photocatalyst, the photocatalytic oxidation of carboxylic acids follows a photo-Kolbe reaction mechanism [84]. An electrochemical reaction in which the decomposition of aqueous carboxylic acid (RCOOH, $R = CH_3$) results in the formation of CO₂ as the primary reaction product and [•]R as the primary reaction intermediate is called a

Kolbe reaction as shown in Equation 1 [85, 86]. Here, the initial step of the Kolbe mechanism includes a reaction between the semiconductor (SC) surface adsorbed carboxylic acid molecule and the photo-generated SC h_{VB}^+ (Equation 1). At the same time, the adsorbed H₂O molecules on the surface of SC material react with h_{VB}^+ and result in the formation of [•]OH and H⁺ (Equation 2).



During the light-induced oxidation of acetic acid/acetate under aerobic conditions, the Kolbe reaction intermediate ($^{\bullet}CH_3$) further reacts with the O₂ adsorbed on the surface of SC thus forming $^{\bullet}O_2CH_3$ (Equation 3).

$$^{\bullet}CH_3 + O_2 \rightarrow ^{\bullet}O_2CH_3$$
 Equation 3

Moreover, a non-Kolbe reaction between acetic acid/acetate molecule and $^{\circ}OH$ occur simultaneously giving $^{\circ}CH_2COO^-$ as a reaction intermediate (Equation 4). Subsequently, the formed $^{\circ}CH_2COO^-$ reacts with the SC adsorbed O₂ molecules yielding $^{\circ}O_2CH_2COO^-$ (Equation 5).

$$CH_3CO_2^- + {}^{\bullet}OH \rightarrow {}^{\bullet}CH_2CO_2^- + H_2O \qquad \text{Equation 4}$$

$${}^{\bullet}CH_2CO_2^- + O_2 \rightarrow {}^{\bullet}O_2CH_2CO_2^- \qquad \text{Equation 5}$$

Wolff and co-workers [80] studied the photocatalytic decomposition of aqueous acetate solutions in the presence of O_2 while employing TiO₂ as a photocatalyst. Due to the presence of air/O₂ acting as an electron scavenger, the presence of a co-catalyst at the TiO₂ surface was not

necessary in their experiments. Wolff *et al.* investigated the effect of varying pH values from acidic to alkaline region and observed that the reaction mechanism follows two different pathways: (1) at pH values < 6, the reaction proceeds through direct oxidation of acetic acid molecule by TiO_2 valence band hole (h_{VB}^+) yielding Kolbe intermediate (Equation 1). While, (2) at pH values > 6, an indirect reaction path exists for the photocatalytic decomposition of acetate, where the acetate molecule reacts with a hydroxyl radical ($^{\bullet}OH$) (Equation 4).

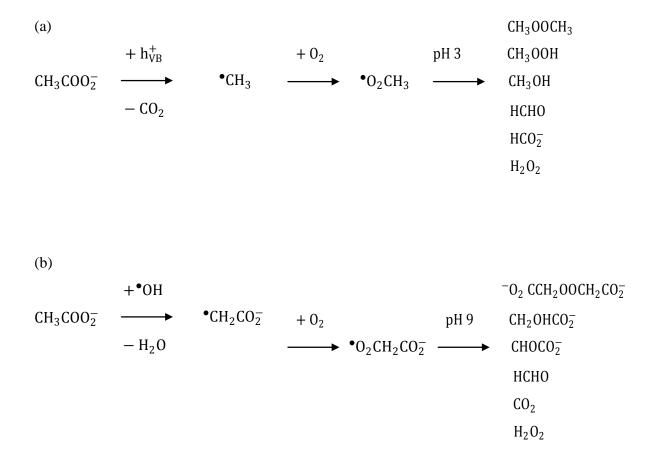


Figure 5: proposed reaction mechanism for the photocatalytic decomposition of aqueous acetate at (a) pH 3, (b) pH 9 [81].

Belhadj *et al.* [81] examined the photocatalytic oxidation of aqueous acetate in the presence of air/O_2 *via* ATR-FTIR and EPR spectroscopy. Their FTIR analysis showed that the change in pH values from more acidic to more basic region results in the adsorption of acetate molecule on the

surface of TiO₂ with different orientations. For instance, at acidic pH values the adsorption of acetate molecule onto the surface of TiO₂ occurred in the form of bidentate structure while basic pH favours the adsorption of acetate in the form of monodentate structure. This means that the major and minor reaction products at different pH values would be different. Through EPR investigations, they also confirmed that the photocatalytic oxidation of aqueous acetate by h_{VB}^+ is a dominant reaction pathway for pH < 7 while the reaction proceeds by the oxidation of acetate molecule with •OH at pH \geq 7. These observations were related to the intensity of EPR signals at different pH values. A reaction scheme leading to different reaction products at different pH regions has been reported by Belhadj and co-workers (Figure 5) [81].

1.2.4.2 Photocatalytic conversion of aqueous acetic acid in the absence of air/O₂

About 40 years ago, numerous reports were published by Bard and co-workers [36, 87, 88] where they discussed the photo-induced transformation of aqueous acetic acid into H₂, CH₄, C₂H₆ and CO₂ as the primary reaction products under anaerobic conditions. They investigated both Pt/TiO₂ particles as well as Pt/TiO₂ electrode systems. As a general conclusion, the authors stated that the photocatalytic degradation of aqueous acetic acid in the absence of air/O₂ proceeds by a photo-Kolbe reaction mechanism (Equation 1). Subsequently, the formation of alkanes is expected by the reaction of primary intermediates as given in Equations 6 – 10 [89].

RCOOH + h_{VB}^+	\rightarrow	$^{\bullet}R$ + CO_2 + H^+	Equation 6
H_{ads}^+ + e_{CB}^-	$\stackrel{\text{Pt}}{\rightarrow}$	•H _{ads}	Equation 7
2•H _{ads}	$\stackrel{\text{Pt}}{\rightarrow}$	H ₂	Equation 8
$^{\bullet}R$ + $^{\bullet}H_{ads}$	\rightarrow	RH	Equation 9
2•R	\rightarrow	R ₂	Equation 10

During the light-induced decarboxylation reaction of aqueous acetic acid, the occurrence of ${}^{\bullet}CH_3$ as a primary reaction intermediate has been confirmed by Kraeutler *et al.* [84] *via* EPR spectroscopy. Hence, the overall reaction mechanism for the photocatalytic degradation of aqueous acetic acid (CH₃COOH) in acidic pH media was expressed as follow (Equation 11 – 12) [36, 84, 87]:

CH ₃ COOH	hv, Pt@TiO ₂ →	$CO_2 + CH_4$	Equation 11
2CH ₃ COOH	hv, Pt@TiO₂	$2\mathrm{CO}_2 + \mathrm{H}_2 + \mathrm{C}_2\mathrm{H}_6$	Equation 12

However, no proof for the stoichiometric reaction (Equation 11 - 12) by the complete degradation of employed acetic acid concentration can be found in literature. Yoneyama et al. [90] investigated the parameters affecting the distribution of reaction products during photocatalytic decomposition of aqueous acetic acid employing Pt/TiO₂ particles both in the absence and in the presence of Pd^{2+} acting as an oxidizing agent. They observed the formation of H_2 and C_2H_6 as minor reaction products while CH_4 and CO_2 as main reaction products in the absence of Pd^{2+} . In their study, CH₄ was found to be the major reaction product with higher yields, even in the presence of Pd^{2+} , where H_2 production was completely suppressed. They claimed that the deposition of Pd²⁺, a H₂ generation catalyst, acts as an electron scavenger in the solution during photo-deposition process and therefore suppresses the hydrogen evolution reaction. Yoneyama and co-workers also examined the reaction kinetics by varying the light intensity. They found a linear relationship between the formed amount of [•]CH₃ resulting from decarboxylation of acetic acid and the light intensity of the employed lamp. Moreover, the effect of different acetic acid concentrations (1 - 8.2 M) has also been studied by Yoneyama and co-workers [90]. They observed that the increase in the concentration of acetic acid from 1 - 5 M also results in an enhanced formation rates for all reaction products, while further increase in the concentration was found to result in lowering the formation rates for all reaction products.

Recently, Mozia *et al.* [35, 91-94] published a series of papers conferring the photocatalytic degradation of aqueous acetic acid under anaerobic conditions while utilizing TiO₂ with various surface modifications (such as Fe, Fe₃O₄, Fe₂O₃ and CuO). In all of their studies, H₂, CO₂, and CH₄ were observed as main reaction products while C_2H_6 and C_3H_8 were detected as the minor reaction products. However, the formation rates of these reaction products were observed to vary with respect to the TiO₂ surface modifications. For instance [35], Fe-modified TiO₂ exhibits a significant amount for HER and CH₄ only when 20 wt % Fe/TiO₂ powders were calcined at 500 °C. They also stated that an increase in the acetic acid concentration form 0.01 to 1 M results in the enhanced amounts of all reaction products, whereas, the formation rates of all reaction products start to decrease at higher concentration values. Mozia and co-workers [91] also

investigated the effect of CuO nanoparticles over TiO₂ (rutile) photocatalyst. They did not observe significant HER in these experiments, while considerable amounts of CO₂ and CH₄ were obtained when CuO/TiO₂ (rutile) was employed as a photocatalyst. In another study, Heciak *et al.* [95] utilized CuO/TiO₂ composites mainly for the photocatalytic transformation of aqueous acetic acid into H₂. The presence of metallic Cu nanoparticles was confirmed by XRD measurement. Higher formation rates for all reaction products were observed only when both CuO and Cu₂O were present on the TiO₂ surface.

Sakata *et al.* revealed that the change in pH values from acidic to basic media leads to the different reaction mechanisms during photocatalytic decomposition of aqueous carboxylic acids. They examined aqueous acetic, propionic and butyric acids employing Pt/TiO₂ (anatase, rutile) particles. By doing both liquid phase and gas phase analysis for all employed carboxylic acids, they observed that the photo-decomposition of carboxylic acid proceeds by a photo-Kolbe reaction only at pH < 7. On the other hand, in alkaline pH media (pH > 7) the photo-Kolbe reaction occurs only as a minor reaction. There exists another mechanism known as Hofer-Moest reaction for the light-induced decomposition of carboxylic acids. According to which, the carboxylate anions discharged anodically (Equation 13) while forming [•]R and CO₂. However, in the subsequent reactions, alcohols, olefins and aldehydes are formed as reaction products [96, 97]. The Hofer-Moest reaction is expressed in Equations 13 – 16.

RCOO-	\rightarrow	$RCOO^{\bullet} + e^{-}$	Equation 13
RCOO•	\rightarrow	$^{\bullet}R + CO_2$	Equation 14
$^{-}OH + h_{VB}^{+}$	\rightarrow	•ОН	Equation 15
•R + •OH	\rightarrow	ROH	Equation 16

Following the Hofer-Moest reaction, at pH values > 7, the overall reaction for complete degradation of aqueous acetic acid can be explain as follow (Equation 17):

$$CH_3COOH + 2H_2O \rightarrow 2CO_2 + 4H_2$$
 Equation 17

For deep insight about the reaction mechanism of photocatalytic aqueous acetic acid degradation, only two reports are present in literature discussing the isotopic labelling experiments. The

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experiments were performed to see the origin of H₂, and CH₄ formation during photocatalytic decomposition of aqueous acetic acid. Bard and co-workers [84] examined the influence of mono-deuterated aqueous acetic acid in a photocatalytic reaction by using Pt/TiO₂ as a photocatalyst. In their study, for HER, the reaction system Pt/TiO₂-CH₃COOD-H₂O was found to exhibit the formation of D₂: HD: H₂ as reaction products with a ratio of 2: 1.1: 0.6, respectively. Moreover, the analysis for methane depicts the formation of CH₃D \approx 45 % and CH₄ \approx 55 % as reaction products. It has been argued by authors that there does not occurs any proton exchange reaction at the methyl group (CH₃) of acetic acid. Sakata *et al.* [37] also carried out isotopic labelling experiment with a reaction system containing Pt/TiO₂-CH₃COOH-D₂O. The photocatalytic experiments were performed in the presence and in the absence of AgNO₃ as an electron scavenger. Sakata and co-workers performed these experiments mainly to see the reaction pathways for CH₄ formation. Their data analysis revealed that without the employment of AgNO₃, the main reaction product was CH₃D while the presence of AgNO₃ gives rise to the formation of CH₄ as a major reaction product.

Huck *et al.* [98] investigated the light-induced proton exchange reaction in carboxylic acids *via* photolysis. Their studies demonstrated that the carboxylic acids formed methyl substituted aromatic ketones upon illumination. Hence, the methyl group becomes activated and, in the presence of D_2O as a solvent, a fast proton exchange reaction is very likely to occur at the methyl group of carboxylic acid. Recently, Mirich *et al.* [99] inspected the gas-phase heterogeneous catalytic reaction to scrutinize the proton exchange reactions for decomposition of carboxylic acids. The authors found that in the presence of a suitable catalyst (Pd/Al in their study), a proton exchange reaction at the methyl group of carboxylic acid occur at elevated temperature values.

1.3 Objectives

Recently, the synthesis of large variety of new photocatalytic materials has been the focus of research in order to obtain competent HER. However, mechanistic aspects of photocatalytic reaction system while utilizing the standard SC materials (i.e., TiO_2) are still unclear. Moreover, photocatalytic test reactions are usually performed in the laboratories *via* a classical gas chromatograph (GC) system attached to a batch photoreactor. The long term experiments over a

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large scale of time cannot be carried out in batch system due to the overpressure in the photoreactor. Also, a GC does not allow doing any isotopic labelling studies while permitting only limited detection of gases (*i.e.*, H_2 , CO_2 , and O_2). Therefore, in this work, we have used a photoreactor attached to the quadrupole mass spectrometer (QMS) which allows continuous detection of all gaseous products evolved during the photocatalytic reaction.

The scientific objective of this thesis is not the development of new photocatalytic materials but the elucidation of the mechanistic aspects during the photocatalytic aqueous organic pollutant degradation into value-added fuels (*i.e.*, H₂, hydrocarbons) employing Pt/TiO₂ as a photocatalyst. The Pt/TiO₂ particles employed in this work have been synthesized *via* an impregnation method and were provided by H.C. Starck Company (Goslar, Germany) within the frame work of a joint BMBF project ('Duasol'). Here, acetic acid, which is hazardous and highly corrosive in its concentrated form, and exists in the industrial wastes, has been chosen as a model organic compound. Generally, the mineralization of acetic acid requires expensive experimental techniques. Comparatively, the conversion of aqueous acetic acid into useful fuels (i.e., H₂, and hydrocarbons) by means of photocatalysis is an environment friendly method and does not require special conditions.

Starting from the preliminary work of Krauetler and Bard [36, 87], many reports have been published in literature while discussing the reaction mechanism for the photocatalytic decomposition of aqueous acetic acid [35, 37, 90, 100, 101]. Many published papers reported the formation of CO_2 , H_2 , CH_4 , and C_2H_6 as main reaction products during the photo-induced transformation of aqueous acetic acid by using Pt/TiO₂ powders and electrodes. However, details with respect to following important parameters are still unclear and missing in the literature:

- (1) Effect of TiO₂ surface modification by various co-catalysts.
- (2) Effect of different acetic acid concentrations.
- (3) pH values (ranges from acidic to basic).
- (4) Isotopic labelling experiments.

Hence, the central aim of this thesis is to address above mentioned points in order to clarify the reaction mechanism for photocatalytic degradation of aqueous acetic acid in more detailed way. The questions that need to be answered include:

Do different co-catalysts loadings onto the surface of photocatalyst affect the product distribution?

Whether various initial concentrations of the reactant affect product distribution?

Do pH values changing from acidic to alkaline media affect the primary reaction intermediates and respective reaction products? Does pH variation over a range of values lead to different reaction mechanisms?

How isotopic labelling experiments will help to understand the reaction mechanism? How experimental results can be interpreted mechanistically?

Regarding the possibility of a technical application, how photocatalytic fuel production from effluents containing acetic acid can be improved?

The effect of various co-catalysts loaded TiO_2 including noble metals (Pt, Rh, Au and Ag) and metal oxides (IrO₂, and RuO₂) on the reaction intermediates and reaction products resulting from the photocatalytic transformation of aqueous acetic acid has been examined. These experiments are considered to help in identifying the most appropriate co-catalyst for the production of valuable energy fuels.

It has been reported by Yoneyama *et al.* [90] that the increase in initial concentration of acetic acid up to 5 M results in an enhanced amounts of all reaction products including CO₂, H₂, and hydrocarbons. On the contrary, Zheng *et al.* [100] demonstrated that an increase in the initial concentration of aqueous acetic acid between 0.04 - 0.11 M results in the formation of higher amounts of H₂ but they observed a gradual decrease in the formed amounts of H₂ when concentration was further increased to 0.26 M. Considering these opposing reports, the initial concentration of acetic acid is varied in the range of 0.05 - 5 M, and the effect of various concentrations on the reaction rates and product distribution has been inspected in detail.

It has been published in literature [37] that the photocatalytic decomposition of aqueous acetic acid results in the formation of CO₂, H₂, and hydrocarbons (*i.e.*, CH₄ and C₂H₆) over Pt/TiO₂. However, an increase in the initial pH of the employed suspension from strong acidic to strong basic regime results in a significantly increased amount of H₂ formation and drastically decreased amounts of hydrocarbons. In another study, [100] the photocatalytic degradation of aqueous acetic acid with Pt/TiO₂ depicts a significant decrease in H₂ as well as hydrocarbons formation

1. Introduction

rate when initial pH of the suspension was shifted from acidic to basic media. Due to these contradictory reports, the effect of initial pH values on the reaction rates and product distribution has been re-investigated in the present work.

Conflicting reviews exist in literature while discussing the photocatalytic hydrogen evolution reaction (HER) with simultaneous degradation of an organic probe molecule. According to a group of scientists, H₂ is produced by a H₂O splitting reaction even in the presence of an organic electron donor [102, 103], whereas, other group of scientists regarded this as a photocatalytic reforming phenomenon [13, 26-28]. In order to solve the controversies about H₂ evolution reaction, isotopic labelling experiments are very important. In addition, the model organic pollutant such as acetic acid results in the formation of H₂ as well as CH₄ as the major reaction products. In such systems, it becomes even more complicated to gather details about the origin of formed reaction products. Only few reports are published in literature demonstrating the origin of H₂ evolution by means of isotopic labelling experiments during photocatalytic decomposition of aqueous acetic acid. In these papers, authors only discussed the proton exchange reaction (PER) at carboxylic group (COOH) of acetic acid while PER at the methyl group (CH₃) of acetic acid has not been discussed. Also, inadequate information is available about the effects of different isotopes on the reaction rates and product distribution resulting from photocatalytic decomposition of aqueous acetic acid. In this study, the analysis for HER employing different isotopes of acetic acid as well as solvents has been done. For the first time, the PER at both carboxylic, and methyl group of acetic acid has been investigated via spectroscopic techniques such as quadrupole mass spectrometer (QMS) and nuclear magnetic resonance (NMR). The effect of different isotopes on the reaction rates, reaction intermediates and reaction products has also been investigated for the first time.

2. Materials and experimental methods

2.1 Materials

In order to modify the surface of TiO₂ with various metals and metal oxides, all required chemicals were bought from Sigma Aldrich and used as received. For the preparation of all aqueous solutions and suspensions, deionized water was used from a SARTORIUS ARIUM 611 device with a resistivity of 18.2 M Ω ·cm. Pure Acetic acid (purity \geq 100 %) and different isotopes of acetic acid such as CD₃COOD (purity, 99.9 atom % D) and CH₃COOD (purity, 99 atom % D) were purchased from Sigma Aldrich with highest purity. Deuterium oxide (D₂O) (purity, 99.9 atom % D) was also bought from Sigma Aldrich. The pH as well as pD adjustments were done by using perchloric acid (HClO₄) which was also purchased from Sigma Aldrich.

2.2 Noble metals loaded TiO₂

Commercial TiO₂ (P25) powders were obtained from Evonik Aeroxide, Germany. 1 wt % Ptdeposited-TiO₂ (P25) powders were synthesized and supplied by H.C starck company, Goslar, Germany. The Pt/TiO₂ powders were prepared in H. C. Starck Company by a conventional impregnation method employing commercial TiO₂ (P25) powders and chloroplatinic acid $(H_2PtCl_6 \cdot 6H_2O)$ as a Pt precursor. In brief, a conical flask was filled by 20 g of TiO₂ powder, 100 mL deionized water and 4.45 mL H₂PtCl₆ (≥ 8.9 %) solution. The conical flask then sealed with a rubber septum stopper and given an ultrasonic bath for about 6 hours. In the next step, obtained solution was washed, dried and grinded properly. The Pt/TiO₂ powders were used for our experiments without any further purification. Other than Pt/TiO₂, the effect of rhodium (Rh), gold (Au) and silver (Ag) depositions on the surface of TiO₂ acting as a co-catalyst has also been investigated in this work. For this purpose, a typical in-situ photodeposition method has been used as described in the literature [104]. In order to obtain 1 wt % metal-loaded-TiO₂, aqueous solutions of $(NH_4)_3RhCl_6$ with $Rh \ge 99.99$ %, $HAuCl_4 \cdot 3H_2O$ with $Au \ge 49.00$ %, and $AgNO_3$ with Ag \geq 99.99 % were used. For instance, a stock solution of 0.01 M was prepared from (NH₄)₃RhCl₆ metal precursor. Afterwards, 254 µL from 0.01M (NH₄)₃RhCl₆ was added into the photoreactor containing 25 mg TiO₂ (P25) powder, 50 mL water and 0.5 M acetic acid.

2. Materials and experimental methods

Subsequently, the suspension was purged with Argon (Ar) for 20 minutes along with continuous stirring in order to remove the dissolved O_2 from the suspension. In the next step, the photoreactor was air sealed followed by a continuous 1 hour Ar flow in the head space of the photoreactor. As a last step, the lamp was switched on thus the 1 wt % Rh loadings on the TiO₂ surface were expected to occur during the photocatalytic reaction. The same method was used for the deposition of other noble metal co-catalysts. For example, 128 µL from a stock solution of HAuCl₄·3H₂O prepared with 0.01 M gives 1 wt % Au/TiO₂ particles and 234 µL from AgNO₃ prepared with 0.01 M results in the formation of 1 wt % Ag/TiO₂ powders.

2.3 Metal-oxides loaded TiO₂

An impregnation method has been used for the synthesis of metal oxide-loaded TiO₂ particles. The procedure was chosen according to the published literature [105]. A stock solution of 0.01 M from $(NH_3)_6RuCl_3$ with $Ru \ge 99.98$ % was prepared to get ruthenium oxide (RuO_2) loaded TiO₂ powders. In order to obtained 1 wt % RuO_2/TiO_2 , 9.99 mL of 0.01 M $(NH_3)_6RuCl_3$ was introduced into a porcelain crucible containing 1g TiO₂ (P25) powder. This suspension was evaporated by giving a thermal treatment (water bath). Afterwards, the dried powder was calcined in a furnace under air/O₂ environment at various temperature values (*e.g.*, 350, 400, and 450 °C). The calcined powders were then grinded in the mortar and pestle to get homogeneous particles. The same method was repeated to get iridium oxide (IrO₂) loaded TiO₂ where 5.255 mL from a 0.01 M Na₂IrCl₆ .H₂O with Ir \ge 99. 99 % assumed to give 1 wt % IrO₂/TiO₂ particles.

2.4 Characterization techniques

2.4.1 X-ray diffraction

For the phase analysis of TiO₂ powders X-ray diffraction (XRD) patterns were recorded by using Bruker D8 Advance instrument. The XRD patterns for all samples were obtained at room temperature employing Cu K α radiations over a range of 2 θ from 5° – 110° in Bragg-Brentano geometry. For the interpretation of the obtained results Rietveld method was used in the TOPAS 4.2 (Bruker-AXS) software.

2.4.2 Transmission electron microscopy

The analysis for particle size and their distribution were done by Transmission electron microscopy (TEM). The instrument TEM Tecnai G2 F20 TMP (FEI) with field emission gun at 200 kV acceleration voltages was used.

2.4.3 Specific surface area measurements

The single point specific surface area of pure and surface modified TiO_2 powders were calculated by Brunauer-Emmett-Teller (BET) model [106]. For this purpose, FlowSorb II 2300 device from Micromeritics, USA with a gas mixture of nitrogen (N₂) (30 %) and helium (He) (70 %) in order to determine the adsorption was used. Prior to the BET measurements, a heat treatment of up to 130 °C was given to the samples for about an hour so that all the impurities will be removed.

2.4.4 Diffuse UV-vis spectroscopy

The diffuse reflectance spectra of pure, metals and metal oxides loaded TiO_2 were obtained *via* Varian Cary 100 Scan UV-vis spectrophotometer. The spectral ranges were adjusted as 200 - 800 nm employing an Ulbricht sphere. As a reference material barium sulfate was used, that provides a measurement with 100 % reflectance. The conversion of reflectance signals into F(R) for all materials was done according to the Kubelka-Munk theory [107].

2.5 Photocatalytic measurements

A 100 cm³ double jacket quartz photoreactor with two necks (one for gas in and other for gas out) was used to carry out all the photocatalytic experiments. For the analysis of gaseous products during the photocatalytic reaction, the photoreactor was combined with Hidden HPR-20 quadrupole mass spectrometer (QMS). A continuous Ar flow was used during the measurements, while the adjustment of Ar flow was handled by a mass flow controller. A schematic illustration of photocatalytic set-up is given in Figure 6. This experimental set-up facilitates the monitoring of product formation rates during the entire course of photocatalytic reaction. For a reaction, 25

2. Materials and experimental methods

mg photocatalyst was added into the 0.5 M aqueous solution of acetic acid with a total photoreactor volume of 50 mL. This photoreactor was then put on a continuous stirring and the suspension was purged with Ar for 20 - 30 minutes so that the dissolved O_2 will be removed. Afterwards, the reactor was air tighten with the help of rubber septum and attached to the QMS by metal flanges. The Ar flow with a rate of 50 cm³ min⁻¹ was continued for 10 - 20 minutes again in the headspace of the photoreactor to ensure the removal of O_2 from the system. In the next step, the Ar flow switch to $10 \text{ cm}^3 \text{ min}^{-1}$ and held constant during the complete photocatalytic reaction. Prior to the illumination, the photoreactor was kept under dark for at-least one hour to obtain a stabilization of all gaseous compounds with respect to their assigned signals. Once the stabilization of all signals was achieved, the lamp was switched on for 15 hours in most of the experiments. An Osram XBO 1000 Watt Xenon (Xe) arc lamp enclosed in a Müller LAX 1000 lamp housing was used as a light source in all of the experiments. After 15 h, once the lamp was switched off a decrease in the formation rate for all reaction system was obvious and possible to see on the experimental set-up. However, the signals were continued to be calculated by QMS until all the formed products reached to the baseline.

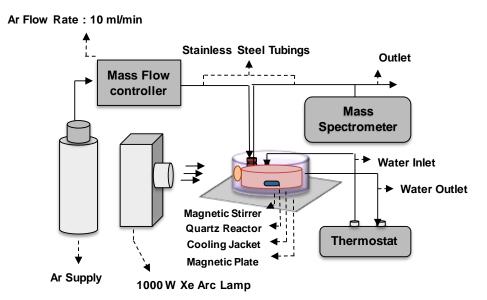


Figure 6: Schematic illustration of Photocatalytic-Set up.

During all photocatalytic reactions, the temperature of the photoreactor was kept constant by attaching it to a thermostat from Julabo Company. The QMS was calibrated with diluted gasses (1 - 2% in Ar) obtained from Linda Company. The QMS calibration was done to do quantitative analysis of all reaction products formed during the photocatalytic reaction.

2.6 Photonic efficiency determination

In order to determine the photocatalytic activity, the photonic efficiency (ζ) for all reaction products was calculated as described in the literature [108]. The photonic efficiency is generally defined as:

$$\zeta [\%] = \frac{production \, rate}{photon \, flux} \times 100$$
 Equation 18

Here, production rate represents the formation rate of the gaseous products exiting the photoreactor, and photon flux corresponds to the incident number of photons per unit area per time.

The photon flux can be defined as follow:

$$Photon flux = I_0 \times A \qquad Equation 19$$

The area of the window of photoreactor is represented by A whereas I_0 illustrates the absorbed number of photons and explain as follow:

$$I_0 = \frac{I \cdot \lambda}{N_a \cdot h \cdot c}$$
 Equation 20

Here, *I* is the total number of photons coming to the window of photoreactor by, λ illustrates the wavelength according to the TiO₂ band gap energy, $N_a = 6.023 \times 10^{23} \text{ mol}^{-1}$ is Avogadro constant, $h = 6.63 \times 10^{-34}$ Js is the Planck's constant and $c = 3 \times 10^8 \text{ ms}^{-1}$ corresponds to the speed of light.

2. Materials and experimental methods

For the calculations of photonic efficiency in the present work, $\lambda = 365$ nm and I = 30 mW cm⁻² was used. The area is given by the diameter (D = 3.5 cm) of the window of photoreactor and was calculated to be A = ($\pi/4$) × D² = 9.6162 cm²

2.7 Nuclear magnetic resonance spectroscopy

For mechanistic investigations, Bruker 400 MHz Ascend with Avance-III console and broadband Prodigy Probe proton nuclear magnetic resonance (NMR) spectroscopy was used. For the NMR sample preparation, first a photocatalytic experiment was performed. After 15 h of illumination, the suspension was taken from the photoreactor and was shifted to the Ar purged NMR quartz tube through an Ar purged syringe. The NMR tube was then immediately put in the NMR sample holder to analyse the sample. All the samples for NMR analysis were prepared in the same way.

3.1 Material characterizations

3.1.1 Structural and optical properties

The photocatalyst materials including commercial TiO₂ P25 as well as synthesized noble metals and metal-oxides loaded TiO₂ particles were characterized by analytical techniques in order to get the information about their morphological and optical characteristics. Figure 7 exhibits the XRD patterns for pure as well as synthesized metals and metal oxides loaded TiO₂ particles. In addition to this, an XRD pattern for 1 wt % RuO₂/TiO₂ powders calcined at different temperature values (350 – 450 °C) can also be seen in Figure 8. Data presented both in Figure 7 and 8 demonstrated that the loading of 1 wt % metal or metal oxide on the surface of TiO₂ particles is beyond the detection limit of the XRD instrument and cannot be seen in the obtained results. For instance, in all of the synthesized materials, TiO₂ anatase (A) (JCPDS # 01-075-2545) and rutile (R) (JCPDS # 01-073-1782) peaks are obvious and comparable with those obtained from pure P25 TiO₂. However, no other peak corresponding to any metal or metal oxide compound can be seen. Also, 1 wt % metal or metal oxide loadings on the surface of TiO₂ does not exhibit any shift in its crystal structure. Additionally, the thermal treatment up to 450 °C does not seem (Figure 8) to affect the crystal structure of P25 TiO₂ particles. These results can be ascribed to the fact that the deposited metals and metal oxides cocatalysts stayed on the surface of TiO₂ particles and do not enter in its crystal lattice.

The Particle size of the synthesized powders was determined by means of TEM and is given in the Figures 9 and 10. Here, the dark spherical structures depict the corresponding metal or metal oxide nanoparticles (NP) while the bright spheres exhibit TiO_2 particles (Figure 9). The distribution of metal or metal oxide NP (Figure 9) seems to be quite uniform in most of the synthesized materials. However, in case of RuO_2/TiO_2 , agglomerates are more obvious. The particle size of both metal as well as metal oxide and TiO_2 was observed to be in the range of 15 – 25 nm.

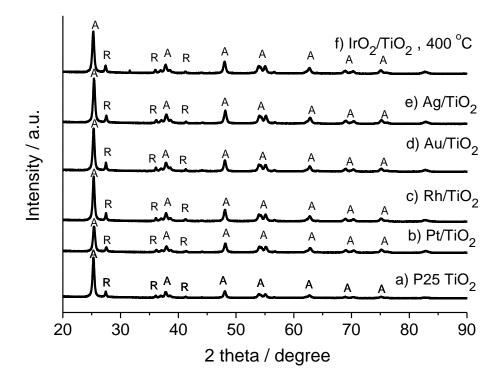


Figure 7: XRD patterns for the (a) Bare P25 TiO₂ powders, (b – e) metal loaded TiO₂powders and (f) metal-oxide loaded TiO₂ particles calcined at 400 °C.

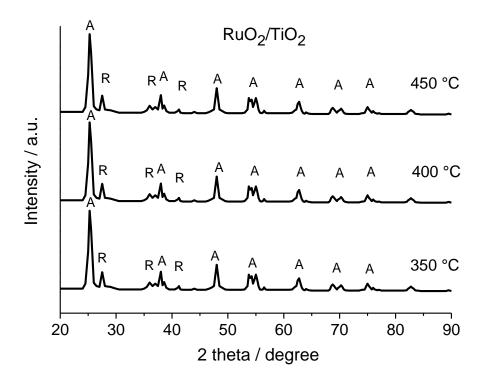


Figure 8: XRD patterns for the RuO₂/TiO₂ powders calcined at 350, 400 and 450 °C.

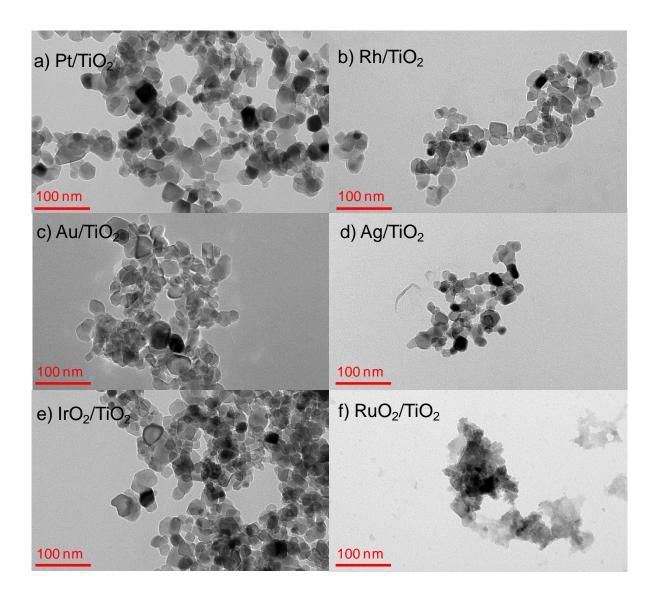


Figure 9: TEM micrographs for (a - d) metal loaded TiO₂ and (e - f) metal oxide (calcined at 400 °C) loaded TiO₂ particles.

In the high resolution TEM micrographs (Figure 10), the crystal lattice is quite obvious for all synthesized materials. Also, a metal or metal oxide-TiO₂ interface can be seen very clearly. Once again, the RuO_2/TiO_2 powders represent big agglomerates and do not give any appropriate information about particle size and distribution.

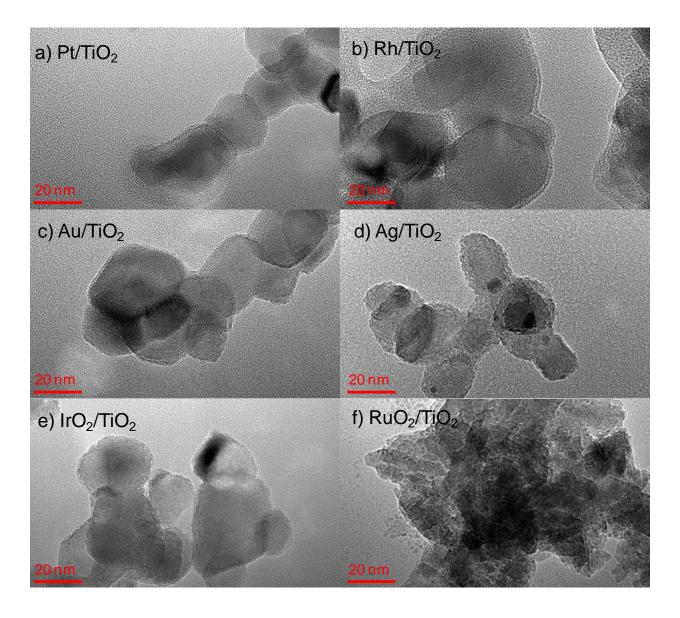


Figure10: High resolution TEM micrographs for (a - d) metal loaded TiO₂ and (e - f) metal oxide (calcined at 400 °C) loaded TiO₂ particles.

The single point BET surface areas of all prepared noble metals and metal oxides loaded TiO_2 particles were calculated by N₂ adsorption measurements and are presented in Table 1 and Table 2. It can be seen in Table 1 that the loading of various metals on the surface of TiO_2 gives negligible changes in BET surface area as compared to the pure TiO_2 particles. It is also obvious in Table 2 that the calcination of metal oxide modified TiO_2 powders at different temperature values results in almost same values for the BET surface areas. This means, once again, that the

thermal treatment up to 450 °C on the TiO_2 powders does not affect their physical and chemical properties. Hence, these results match well with the obtained XRD data for all the samples.

Photocatalyst	Synthesis Method	BET Surface Area / $m^2 g^{-1}$
P25 TiO ₂	commercial powder	51
Pt/TiO ₂	impregnation method	51
Rh/TiO ₂	photodeposition method	50
Au/TiO ₂	photodeposition method	50
Ag/TiO ₂	photodeposition method	48

Table 1: BET surface areas for pure and metal loaded TiO₂.

Table 2: BET surface areas for pure and metal loaded TiO₂.

Photocatalyst	Synthesis Method	BET Surface Area / $m^2 g^{-1}$
IrO ₂ /TiO ₂	impregnation method, 350 °C	50
IrO ₂ /TiO ₂	impregnation method, 400 °C	51
IrO ₂ /TiO ₂	impregnation method, 450 $^{\circ}\mathrm{C}$	48
RuO ₂ /TiO ₂	impregnation method, 350 $^{\circ}$ C	50
RuO ₂ /TiO ₂	impregnation method, 400 $^{\circ}\mathrm{C}$	49
RuO ₂ /TiO ₂	impregnation method, 450 °C	49

The optical properties of the employed materials were observed by using diffuse reflectance UVvis spectroscopy. In a photocatalytic reaction, one of the most crucial steps is the choice of a photocatalyst material with suitable absorption properties. Figure 11, 12 and 13 demonstrate the absorption spectra of pure, metals loaded TiO₂ as well as metal oxides loaded TiO₂ at varying temperatures (*i.e.*, 350, 400, and 450 °C), respectively. The conversion of diffuse reflectance signals into absorption was done according to the Kubelka-Munk theory. It can be seen in Figure 11 that the employment of various noble metals on the surface of TiO₂ does not result in the shift

of their absorption spectra (F(R)) as compared to the absorption spectrum of bare TiO₂. It is also obvious from Figure 12 and 13 that the thermal treatment of up to 450 °C does not cause any changes in the absorption spectra of metal oxide loaded TiO₂ powders. The obtained results also show that the synthesis methods used in this study for the loading of noble metals as well metal oxides does not support extension of TiO₂ absorption in the visible range.

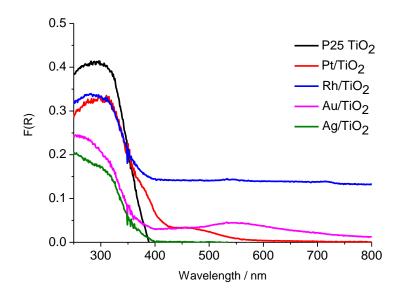


Figure 11: Diffuse reflectance spectra of pure and noble metals loaded TiO₂ particles.

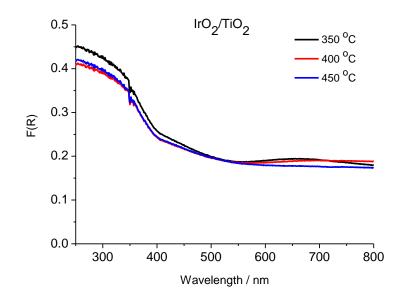


Figure 12: Diffuse reflectance spectra of IrO₂/TiO₂ particles.

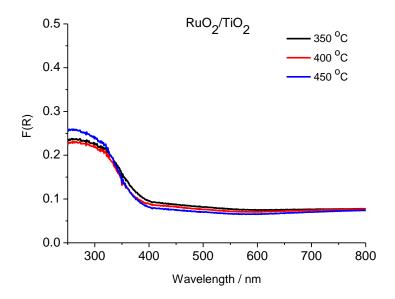


Figure 13: Diffuse reflectance spectra of RuO₂/TiO₂particles.

3.2 Photocatalytic experiments

3.2.1 Bare P25 TiO₂ as a photocatalyst

Blank experiments for the anaerobic photocatalytic degradation of aqueous acetic acid into useful solar fuels have been done (1) in the presence of TiO_2 as a photocatalyst suspended in H₂O, without employing any sacrificial reagent while illuminating with UV (A) light, (2) in the presence of a co-catalyst and aqueous solution of acetic acid but without any semiconducting material and illuminating with UV (A) light, and (3) bare TiO₂ suspended in aqueous acetic acid illuminating with UV (A) light. No formation of molecular hydrogen or hydrocarbons was observed from controlled experiments with reaction system 1 and 2. However, reaction system 3, where bare TiO₂ was used as a photocatalyst and aqueous acetic acid as an electron donor or sacrificial reagent, exhibits poor photocatalytic activity as presented in Figure 14. It can be seen (Figure 14) that the photo-induced transformation of aqueous acetic acid into CO₂, CH₄, H₂ and C₂H₆ occurred with very low formation rates (Figure 14a) and corresponding less formed amounts (Figure 14b), which are close to the detection limits of the quadrupole mass spectrometer (QMS).

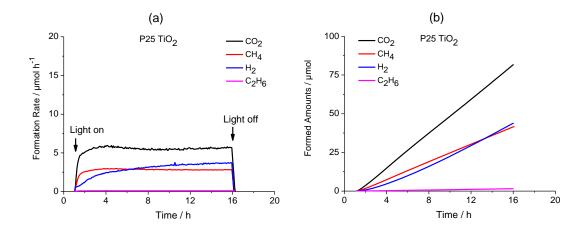
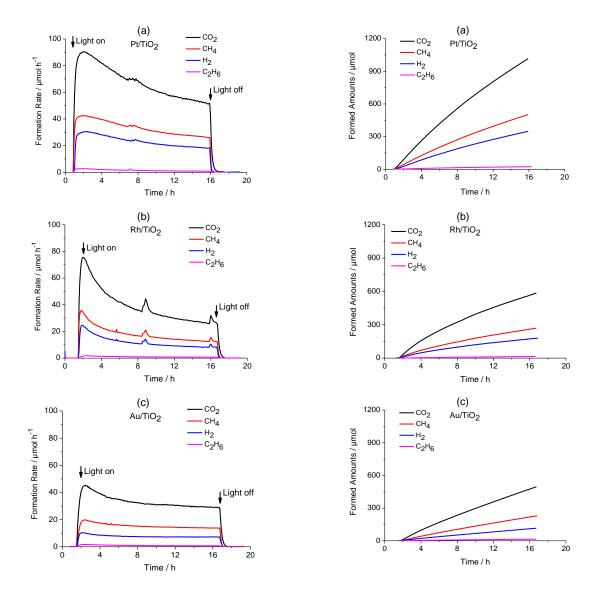


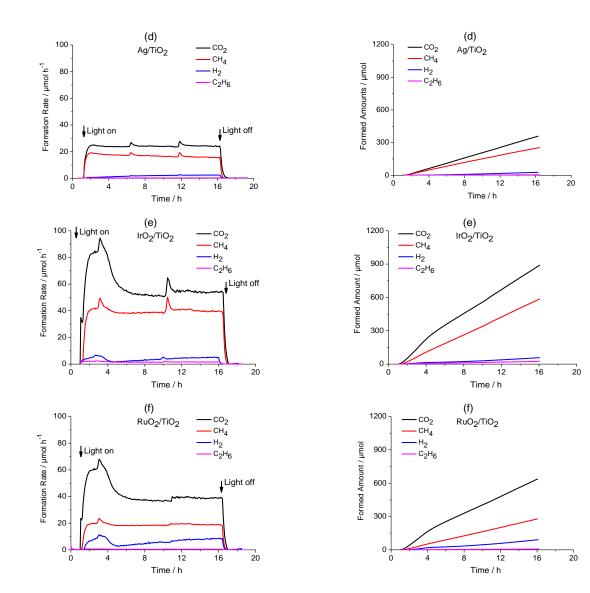
Figure 14: Formation rates (a) and amounts (b) of the main reaction products *i.e.*, CO₂, H₂, CH₄ and C₂H₆, photocatalytically formed from aqueous suspensions containing P25 TiO₂ as the photocatalyst. *Experimental conditions:* photocatalyst concentration = 0.5 g L⁻¹, initial acetic acid concentration = 0.5 M, pH 2, suspension volume = 50 mL, irradiation time = 15 h, irradiation intensity I₂₅₀-I₄₅₀ = 30 mW cm⁻².

3.2.2 Surface modified TiO₂ as a photocatalyst

In order to improve the photocatalytic activity, the surface of TiO₂ powders was loaded with various metals (Pt, Rh, Au, and Ag) and metal oxides (IrO₂ and RuO₂). Photocatalytic runs performed with metal or metal oxide loaded TiO₂ particles suspended in 0.5 M aqueous acetic acid solutions are given in Figure 15 and 16. For metal oxides (IrO₂ and RuO₂) loaded TiO₂ particles, the calcination treatment of 400 °C was found to result in higher photocatalytic activities (data not shown) than 350 °C and 450 °C. Therefore, IrO₂/TiO₂ and RuO₂/TiO₂ calcined at 400 °C were used for further analysis in this work. The main reaction products resulting from the photocatalytic decomposition of acetic acid are CO₂, CH₄, and H₂ while various alkanes C_XH_{2X+2} , where $x \leq 3$ are also formed as minor reaction products. Details regarding the minor reaction products can be found in the published report [83]. Figure 15 represents the plots obtained from quadrupole mass spectrometer (QMS) for the formation rates of the main reaction products versus irradiation time. Before starting the photocatalytic reaction, the photoreactor was kept under dark for at least 1 h with continuous magnetic stirring and Ar flow rate of 10 cm³·min⁻¹ so that a stabilization of the corresponding gaseous signals can be achieved in the

QMS. Immediately after the lamp was switched on, formation of all gaseous compounds (Figure 15) was determined by QMS. Usually, the formation rates of all gaseous products require 30 - 40 minutes (depending on the reaction conditions) to achieve their maximum observed value. Once the maximum observed rate was achieved by the evolved reaction products, a decreasing trend in most of the experimental runs has been observed. However, after a few hours of irradiation, the reaction rates seemed to become constant indicating the surface changes in the photocatalyst in the presence of light. This means that the total time of irradiation is a key factor to determine the efficiency of a photocatalytic reaction. The amounts of the formed gases have been calculated by doing the integration of formation rates as given in Figure 16.





and C_2H_6 , from aqueous acetic acid employing TiO₂-based photocatalysts. *Experimental conditions:* photocatalyst concentration = 0.5 g concentration = 0.5 M, pH 2, suspension volume = 50 mL, irradiation time = 15 h, irradiation intensity I_{250} - $I_{450} = 30 \text{ mW cm}^{-2}$.

Figure 15: Photocatalytic formation rates of Figure 16: Photocatalytically formed amounts the main reaction products *i.e.*, CO₂, H₂, CH₄ of the main reaction products *i.e.*, CO₂, H₂, CH₄ and C₂H₆, from aqueous acetic acid employing TiO₂-based photocatalysts. Experimental conditions: photocatalyst L^{-1} , co-catalyst loading = 1 wt %, acetic acid concentration = 0.5 g L^{-1} , co-catalyst loading = 1 wt %, acetic acid concentration = 0.5 M, pH 2, suspension volume = 50 mL, irradiation time = 15 h, irradiation intensity I_{250} - I_{450} = 30 mW cm^{-2} .

The data analysis of the obtained results shows that the loading of various co-catalysts on TiO₂ surface does not affect the reaction products but affects the formation rates $r_i = dn_i/dt$ to a great extent (Figure 15). As a result, the formed amounts $n_i = \int_t r_i dt$ changed significantly (Figure 16). In all experimental runs, CO₂ was observed as the major reaction product within the range of 1027 (Pt/TiO₂) – 357 (Ag/TiO₂) µmol while keeping all experimental conditions (such as initial acetic acid concentration, pH, photocatalyst amount etc.,) same (Figure 17). The order in which formed amounts of CO₂ decrease employing different co-catalysts was acquired as: Pt/TiO₂ > IrO₂/TiO₂ > RuO₂/TiO₂ > Rh/TiO₂ > Au/TiO₂ > Ag/TiO₂ (Figure 17), demonstrating the use of metal oxides as an appropriate co-catalyst.

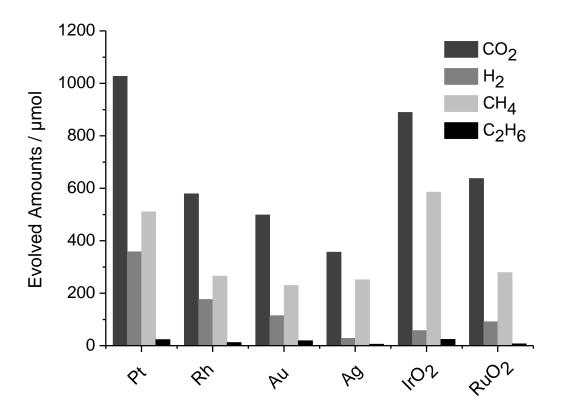
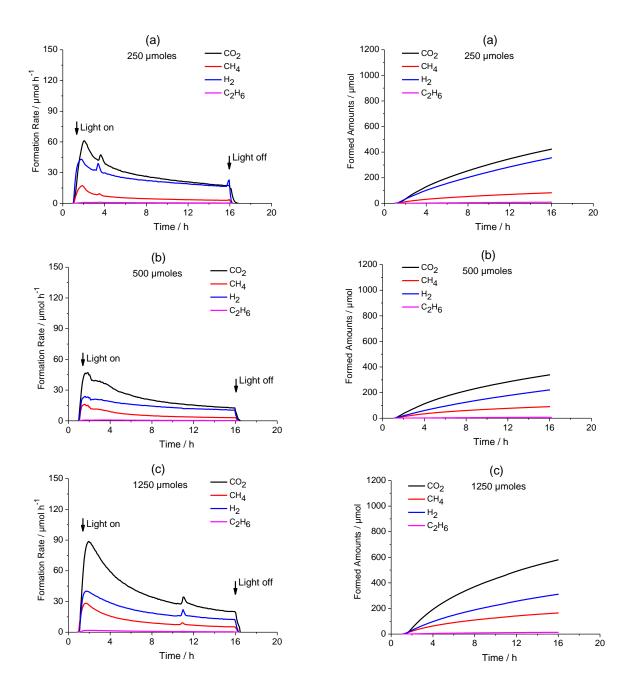


Figure 17: Amounts of the main reaction products, *i.e.*, CO₂, H₂, CH₄, and C₂H₆, photocatalytically formed from aqueous acetic acid after an irradiation time of 15 h in the presence of noble metal and metal oxide loaded TiO₂ as the photocatalysts. *Experimental conditions:* as in Figure 15 – 16.

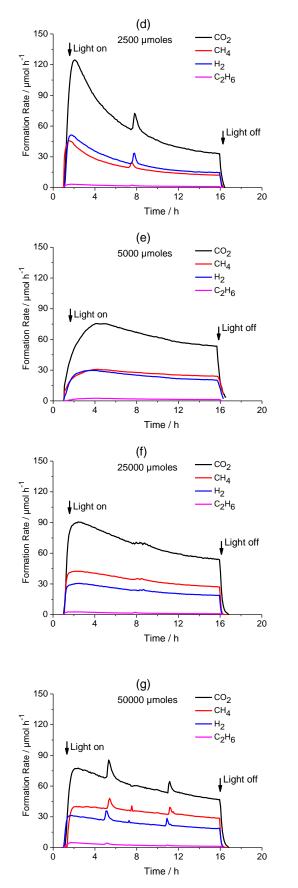
The second main reaction product, resulting from the photocatalytic decomposition of aqueous acetic acid which is very useful for the energy applications was CH_4 . The amounts of CH_4 formation during 15 h of illumination was found to vary from 586 $(IrO_2/TiO_2) - 230 (Au/TiO_2)$ µmol. As the third major reaction product, H_2 was observed to be varying in the range of 375 $(Pt/TiO_2) - 29 (Ag/TiO_2)$ µmol. The formed amounts as well as formation rates for H_2 were observed to decrease in the following order: $Pt/TiO_2 > Rh/TiO_2 > Au/TiO_2 > IrO_2/TiO_2 > RuO_2/TiO_2 > Ag/TiO_2$ (Figure 17) meaning that the metal oxides are poor co-catalysts for the reduction reaction of H⁺ generated during the photocatalytic reaction. However, in general, it can be seen (Figure 17) that the significant amounts for simultaneous oxidation and reduction products were obtained for Pt loaded TiO₂ particles. For example, at the same time, 495 µmoles of CH₄ and 375 µmoles for H₂ were obtained for Pt/TiO₂ only. Therefore, Pt/TiO₂ powder was employed as the optimal photocatalyst in this study for further investigations.

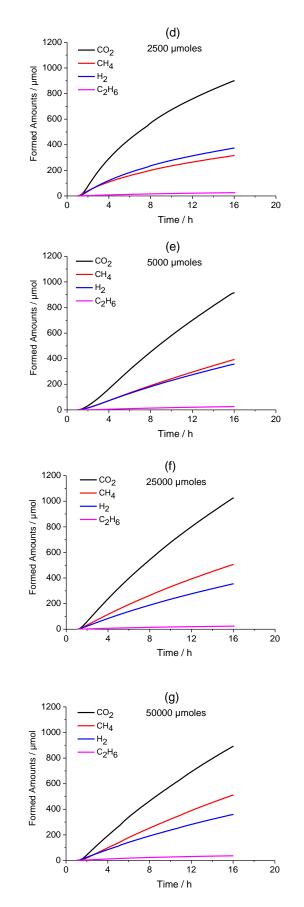
3.2.3 Effect of various acetic acid concentrations

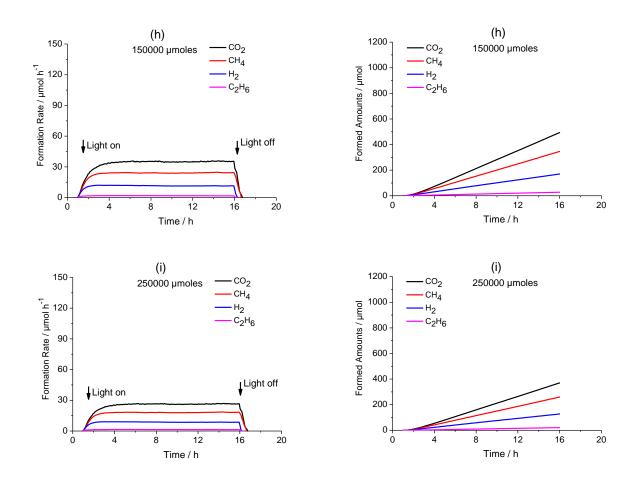
It is well known that the varying concentration of reactants affects the reaction rates. The effect of initial acetic acid concentrations (c_0) ranging between 0.005 M $\leq c_0 \leq$ 5 M corresponding to 250 µmol $\leq n_0 \leq$ 250000µmol (n_0 = initial number of acetic acid moles) over Pt/TiO₂ particles have been examined while keeping other reaction conditions constant (*i.e.*, photocatalyst amount 25 mg, reactor volume 50 mL, pH 2). Results depicting the effect of various acetic acid concentrations on the formation of reaction products and their distribution are given in Figure 18 and 19. Here, Figure 18 demonstrates the formation rates of the main reaction products while relating formed amounts are presented in Figure 19.



3. Results







and C_2H_6 , formed from aqueous suspensions **Experimental** conditions: photocatalyst cm^{-2} .

Figure 18: Photocatalytic formation rates of Figure 19: Photocatalytically formed amounts the main reaction products *i.e.*, CO₂, H₂, CH₄ of the main reaction products *i.e.*, CO₂, H₂, CH_4 and C_2H_6 , formed from aqueous containing 1 wt % Pt/TiO₂ as the photocatalyst suspensions containing 1 wt % Pt/TiO₂ as the and varying initial amounts of acetic acid. photocatalyst and varying initial amounts of acetic acid. *Experimental* conditions: concentration = 0.5 g L^{-1} , 0.005 M \leq initial photocatalyst concentration = 0.5 g L^{-1} , 0.005 acetic acid concentration \leq 5 M, pH 2, M \leq initial acetic acid concentration \leq 5 M, pH suspension volume = 50 mL, irradiation time = 2, suspension volume = 50 mL, irradiation time 15 h, irradiation intensity I_{250} - I_{450} = 30 mW = 15 h, irradiation intensity I_{250} - I_{450} = 30 mW cm^{-2} .

It can be seen in Figure 20 that the change in the concentration (c_0) of acetic acid from lower (0.005 M) – higher (5 M) value results in the formation of CO₂, CH₄ and H₂ as the main reaction products while C₂H₆ as a minor product. These results match well with those obtained by changing the TiO₂ surface with various metal and metal oxide co-catalysts. However, again, the different c_0 seemed to affect the formation rates and subsequent amounts of the formed reaction products to a great extent. For example, 0.005 M $\leq c_0 \leq 0.05$ M analogous to 250 µmol $\leq n_0 \leq 2500$ µmol exhibits an efficient increase in the formed amounts of all reaction products (Figure 20).

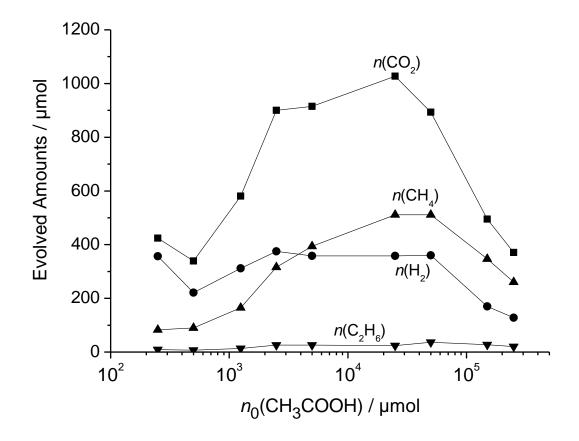
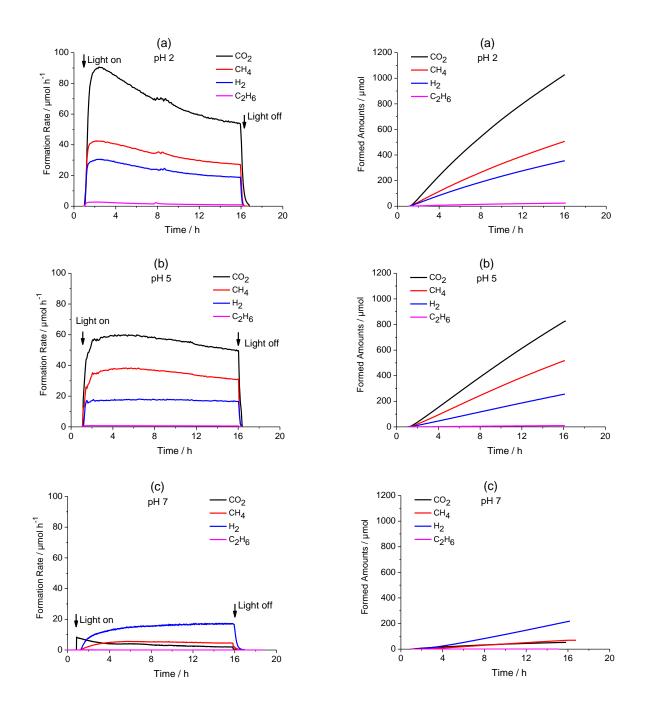


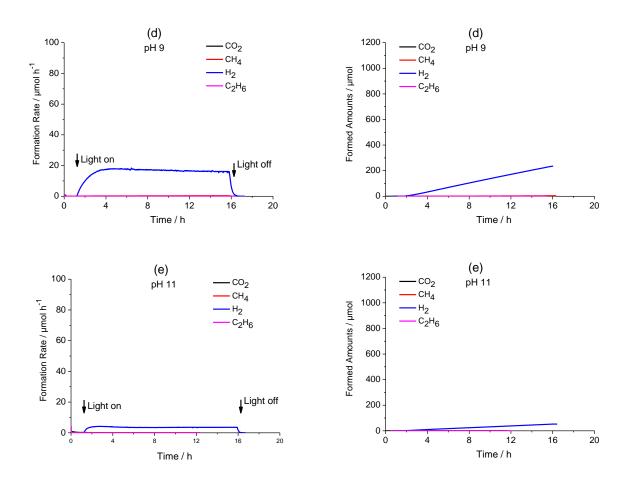
Figure 20: Amounts of the main reaction products *i.e.*, CO₂, H₂, CH₄, and C₂H₆, photocatalytically formed from aqueous suspensions containing 1 wt % Pt/TiO₂ as the photocatalyst and varying amounts of acetic acid after an irradiation time of 15 h. *Experimental conditions:* as in Figure 18 – 19.

The change in the c_0 of acetic acid among 0.05 M – 1 M corresponding to (2500 µmol $\leq n_0 \leq$ 5000 µmol, n_0 = initial number of acetic acid moles) gives the reaction products with approximately constant amounts with the experimental error of ±10 %. However, a further increase in the acetic acid $c_0 > 1$ M (5000 µmol) illustrates a decreasing trend in the formation of all reaction products. It should also be noted that over the range of 0.005 M $\leq c_0 \leq$ 0.05 M (250 µmol $\leq n_0 \leq$ 2500 µmol), the principal reaction product is H₂. On the other hand, 0.1 M $\leq c_0 \leq$ 5 M (5000 µmol $\leq n_0 \leq$ 250000 µmol) demonstrates CH₄ as the main reaction product. Hence, a composition enriched in H₂ with hydrocarbons mixture then changes to a composition poor in H₂ with increasing the c_0 of acetic acid. It is obvious that both energy fuels (*i.e.*, H₂, CH₄) depict the highest evolved amounts simultaneously when initial concentration of acetic acid concentration.

3.2.4 Effect of different pH values

For the mechanistic investigations, pH value is one of the key parameters. After analysing the optimized conditions for the suitable co-catalyst and acetic acid concentration, effect of various pH media on the reaction rates and product distribution from photo-induced degradation of aqueous acetic acid has been studied in the present work. The results obtained by varying the initial pH value of suspension over a range of values such as: $2 \le pH \le 11$ employing Pt/TiO₂ and 0.5 M acetic acid are shown in Figure 21, 22, 23 and 24. Here, CO₂, CH₄, and H₂ were found to be the main reaction products and C₂H₆ as the minor product at pH < 7, while an increase in the pH (\ge 7) results in decreasing amounts of the CO₂, CH₄ and C₂H₆. Moreover, the H₂ formation seemed to be constant in between the range of $5 \le pH \le 9$, but further increase in the pH > 9 value results in lowering the H₂ formation. Figure 21 illustrates the formation rates of the main reaction products and Figure 22 is a representation of the formed amounts for $2 \le pH \le 11$.





1 wt % Pt/TiO₂. *Experimental conditions*: irradiation intensity I_{250} - $I_{450} = 30 \text{ mW cm}^{-2}$.

Figure 21: Photocatalytic formation rates of Figure 22: Photocatalytically formed amounts the main reaction products, *i.e.*, CO₂, H₂, CH₄ of the main reaction products, *i.e.*, CO₂, H₂, and C₂H₆ from aqueous acetic acid employing CH₄ and C₂H₆ from aqueous acetic acid employing 1 wt % Pt/TiO₂. Experimental photocatalyst concentration = 0.5 g L^{-1} , initial *conditions:* photocatalyst concentration = 0.5 gacetic acid concentration = 0.5 M, $2 \le$ initial L^{-1} , initial acetic acid concentration = 0.5 M, 2 $pH \leq 11$ (adjusted by NaOH), suspension \leq initial $pH \leq 11$ (adjusted by NaOH), volume = 50 mL, irradiation time = 15 h, suspension volume = 50 mL, irradiation time = 15 h, irradiation intensity I_{250} - $I_{450} = 30$ mW cm^{-2} .

It is obvious from the Figure 21 that the photocatalytic reaction system containing Pt/TiO₂ as a photocatalyst suspended in 0.5 M acetic acid at pH 2 quantitatively demonstrates the formation of reaction products in their atomic ratios as: $\left(0.6 < \frac{n(C)}{n(O)} < 0.9, 1.0 < \frac{n(H)}{n(O)} < 2.0, \text{ and } 1.4 < \frac{n(H)}{n(C)} < 2.1\right)$ after 15 h of irradiation. In comparison to this, the expected ratios of the atoms forming CH₃COOH molecule is: $\left(\frac{n(C)}{n(O)}=1, \frac{n(H)}{n(O)}=2, \text{ and } \frac{n(H)}{n(C)}=2\right)$ (Equation 10 – 11). The obtained results thus suggest the formation of other by-products than the main reaction products. The qualitative data analysis through QMS confirmed the existence of a large number of by-products such as CO, C₃H₈, CH₃OH, C₂H₅OH, HCHO, CH₃CHO, and HCOOH in the gas phase (Figure 23).

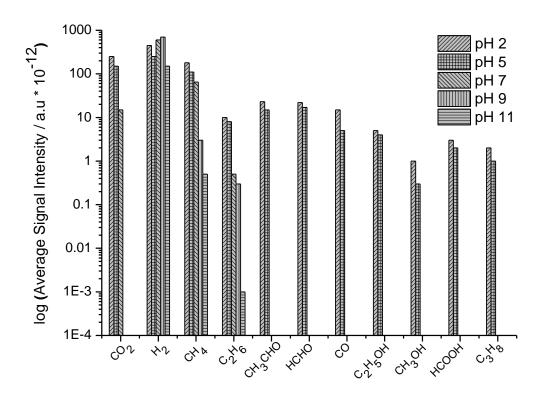


Figure 23: Time-averaged signal intensities of all gaseous reaction products formed during the photocatalytic conversion of aqueous acetic acid employing 1 wt % Pt TiO₂, *Experimental conditions:* photocatalyst concentration = 0.5 g L⁻¹, initial acetic acid concentration = 0.5 M, $2 \le$ initial pH \le 11 (adjusted by NaOH),suspension volume = 50 mL, irradiation time = 15 h, irradiation intensity I₂₅₀-I₄₅₀ = 30 mW cm⁻².

It can be seen in Figure 23 that the amounts of formed by-products are insignificant as compared to the main reaction products (CO₂, CH₄, and H₂). Therefore, a quantitative analysis of only main reaction products and one minor product (C₂H₆) has been done. In Figure 24, the amounts of the evolved gaseous product are presented over a range of pH values such as: $2 \le pH \le 11$. It should be noted that at pH < 7, the ratio between the formed amounts of H₂ and CH₄ is: $\frac{n(H_2)}{n(CH_4)} < 1$ meaning that the formation of CH₄ is preferred. On the contrary, for pH \ge 7 the ratio between the formed amounts of $\frac{n(H_2)}{n(CH_4)}$ and $\frac{n(H_2)}{n(C_2H_6)}$ continue to rise with increasing the pH value indicating the suppression of alkanes formation (Figure 24). Thus, H₂ was observed as the only reaction product in higher amounts. Additionally, at pH \ge 7, the CO₂ is converted into carbonate (CO₃²⁻) and bicarbonate (HCO₃⁻) [109]. So, CO₂ cannot be detected in the gas phase by QMS but it remains present in the aqueous suspensions.

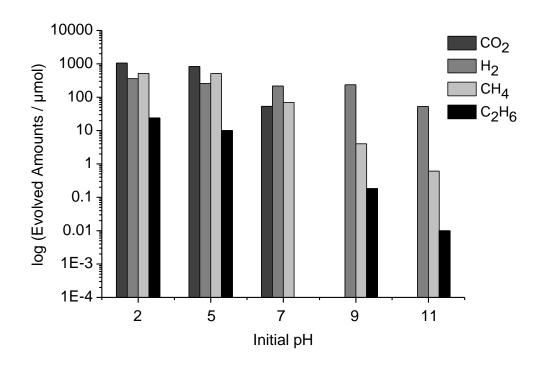


Figure 24: Amounts of the main reaction products *i.e.*, CO₂, H₂, CH₄, and C₂H₆, photocatalytically formed from aqueous suspensions containing 1 wt % Pt/TiO₂ as the photocatalyst and varying initial pH values after an irradiation time of 15 h. *Experimental conditions:* as in Figure 21 - 22.

3.2.5 Isotopic labelling study

Mechanistic investigations for the photocatalytic decomposition of aqueous acetic acid were done by means of isotopic labelling studies. For this purpose, photocatalytic reaction systems containing isotopically different solutions of acetic acid and water were analysed. The details of the reaction systems are as follow:

- (i) Pt/TiO_2 -CH₃COOH-H₂O
- (ii) $Pt/TiO_2-CD_3COOD-H_2O$
- (iii) Pt/TiO₂-CH₃COOD-H₂O
- (iv) $Pt/TiO_2-CD_3COOD-D_2O$
- (v) Pt/TiO_2 -CH₃COOH-D₂O
- (vi) Pt/TiO_2 -CH₃COOD-D₂O

For these experiments, only the main reaction products were quantified. In general, carbon dioxide (CO₂) molecular hydrogen (H₂), molecular deuterium (D₂), HD and methane in different isotopic composition (*i.e.*, CH₄, CH₃D, CD₃H, and CD₄) were detected as the reaction products from all reaction systems (i – vi). The formation rates and the product distribution were observed to vary according to the employed reaction conditions. Here, Pt/TiO₂ was used as a photocatalyst employing 0.5 M acetic acid at pH \approx pD = 2. The pD adjustments were carried out according to the Gross-Butler-Purlee-theory (pD = pH + 0.44) [110].

3.2.5.1 Formation of carbon dioxide

In all six reaction systems (i - vi), CO₂ was found as the major reaction product evolved in highest amounts as compared to the H₂, D₂, HD, CH₄, CH₃D, CD₃H, and CD₄. Figure 25 and 26 show the CO₂ formation rates and corresponding formed amounts, respectively, for all reaction systems (i - vi). During 15 h of illumination, the decrease in the CO₂ formation rate was found to be much larger in suspensions containing H₂O as a solvent (Figure 25a) in comparison to the suspensions having D₂O as a solvent (Figure 25b).

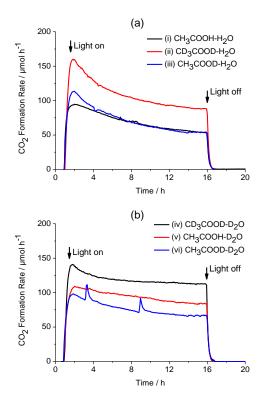
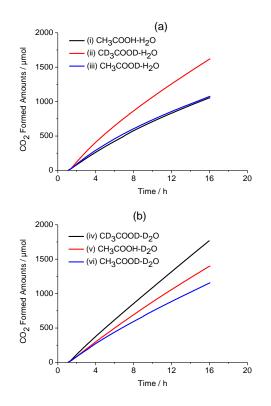


Figure 25: Photocatalytic formation rate of Figure 26: Photocatalytically formed amount CO_2 for (a) reaction systems i, ii, iii and (b) TiO₂, photocatalyst concentration = 0.5 g L^{-1} , acetic acid concentration = 0.5 M, pH \approx pD = 2, reactor volume = 50 m L, irradiation time = cm^{-2} .



of CO_2 for (a) reaction systems i, ii, iii and (b) reaction systems iv, v, vi employing 1 wt % Pt reaction systems iv, v, vi employing 1 wt % Pt TiO₂, photocatalyst concentration = 0.5 g L^{-1} , acetic acid concentration = 0.5 M, pH \approx pD = 2, reactor volume = 50 m L, irradiation time = 15 h, irradiation intensity: I_{250} - I_{450} = 30 mW 15 h, irradiation intensity: I_{250} - I_{450} = 30 mW cm^{-2} .

The solvent (*i.e.*, H₂O, D₂O) also seems to affect the photo-decarboxylation rate (Figure 25). For example, the higher evolved amount of CO₂ from reaction system (v) having D₂O as solvent than (i) containing H₂O as a solvent determines that the decarboxylation of CH₃COOH is fast in D₂O than in H₂O. Moreover, Figure 27 shows that the reaction systems (ii and iv) containing CD₃COOD depicts higher amounts of CO₂ formation in comparison to the system (i, iii, iv, and

v) having CH₃COOH or CH₃COOD. This means that the photo-decarboxylation of CD₃COOD is easier than CH₃COOH and CH₃COOD.

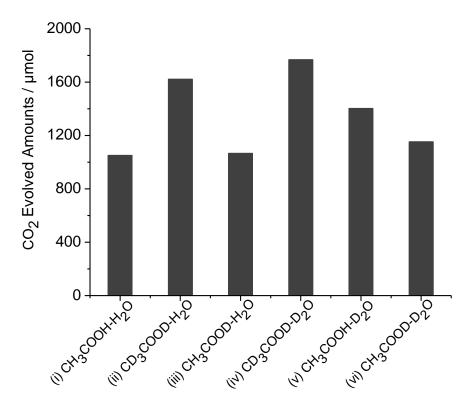
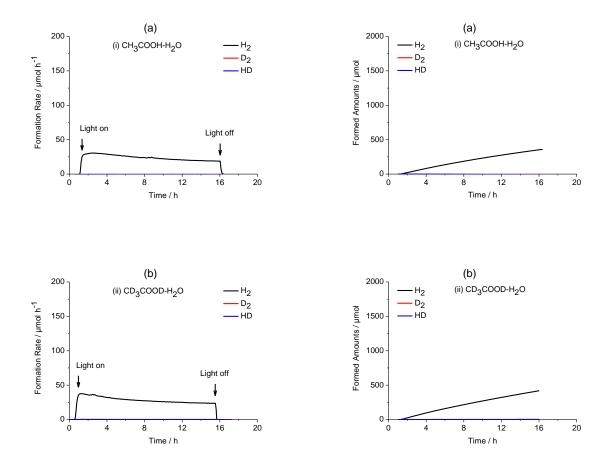


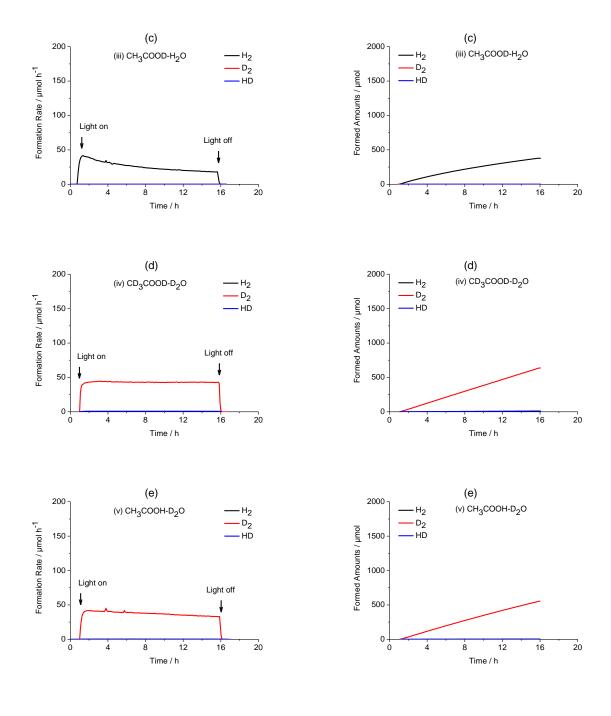
Figure 27: Amounts of the CO₂, photocatalytically formed from aqueous suspensions containing 1 wt % Pt/TiO₂ as the photocatalyst after an irradiation time of 15 h. *Experimental conditions:* as in Figure 25 - 26.

3.2.5.2 Formation of molecular hydrogen and molecular deuterium

The photocatalytic decomposition of acetic acid employing reaction systems (i - vi) results in the formation of molecular hydrogen (H₂), molecular deuterium (D₂) and HD as presented in Figure 28 and 29. Here, Figure 28 represents the formation rates and Figure 29 illustrates the evolved amounts of H₂, D₂, and HD. It can be seen in Figure 30 that the formation of main species (i.e., H₂, D₂, and HD) depends on the solvent being employed. For instance, H₂ and D₂ are produced as the major reaction products with significant amounts employing reaction systems (i) containing H₂O and (iv) having D₂O as a solvent, respectively. No traces for HD were detected in system (i)

but negligible traces of HD were observed in reaction system (iv) as shown in Figure 30. It should also be taken into account that the reaction rates for D_2 formation remain quite stable during the 15 h of illumination in systems (iii, iv, and v) having D_2O as a solvent. In comparison to this, the reaction rates for H_2 formation in reaction systems (i, ii, and iii) during 15 h of illumination exhibit a decreasing trend (Figure 28a, 28d).





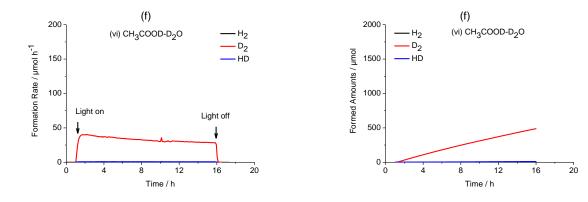


Figure 28: Photocatalytic formation rates of Figure 29: Photocatalytically formed amounts reaction system-iv (e) reaction system-v (f) reaction system-vi, employing 1 wt % Pt TiO₂, photocatalyst concentration = 0.5 g L^{-1} , acetic acid concentration = 0.5 M, pH \approx pD = 2, reactor volume = 50 m L, irradiation time = 15h, irradiation intensity : I_{250} - $I_{450} = 30$ mW cm^{-2} .

the H_2 , D_2 and HD for: (a) reaction system-i (b) of the H_2 , D_2 and HD for: (a) reaction system-i reaction system-ii (c) reaction system-iii (d) (b) reaction system-ii (c) reaction system-iii (d) reaction system-iv (e) reaction system-v (f) reaction system-vi, employing 1 wt % Pt TiO₂, photocatalyst concentration = 0.5 g L^{-1} , acetic acid concentration = 0.5 M, pH \approx pD = 2, reactor volume = 50 m L, irradiation time = 15h, irradiation intensity : I_{250} - $I_{450} = 30$ mW cm^{-2} .

Moreover, the evolved amounts for D₂ (642 µmol) in system (iv) Pt/TiO₂-CD₃COOD-D₂O were approximately two times higher than the evolved amounts of H₂ in system (i) Pt/TiO₂-CH₃COOH-H₂O (Figure 30). These results support the data obtained for CO₂ evolution (chapter 3.2.5.1). The higher amount of D_2 formation (iv, v, and vi) in comparison to H_2 formation illustrates that the decarboxylation of CD₃COOD is faster than CH₃COOH.

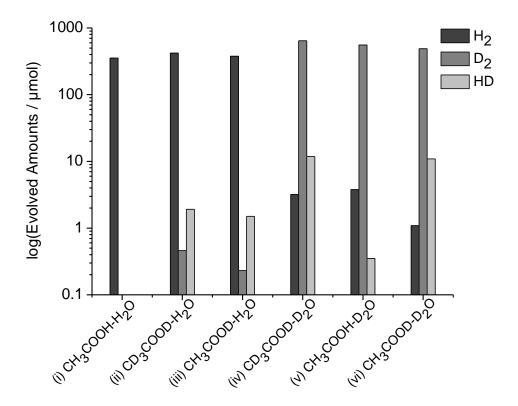
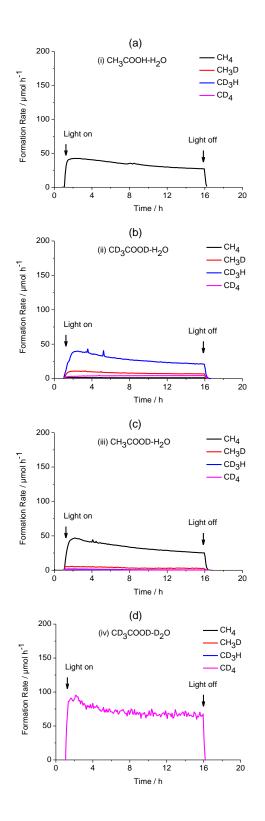
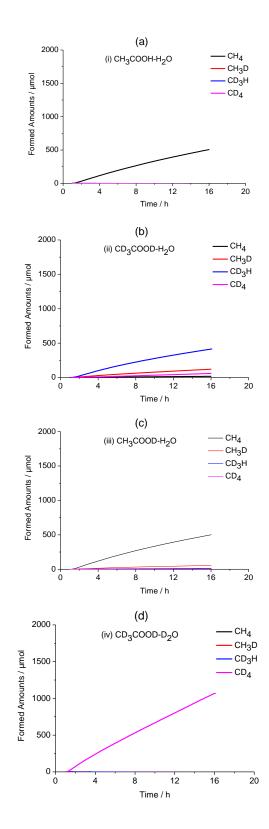


Figure 30: Amounts of the H₂, D₂, and HD, photocatalytically formed from aqueous suspensions containing 1 wt % Pt/TiO₂ as the photocatalyst after an irradiation time of 15 h. *Experimental conditions:* as in Figure 28 - 29.

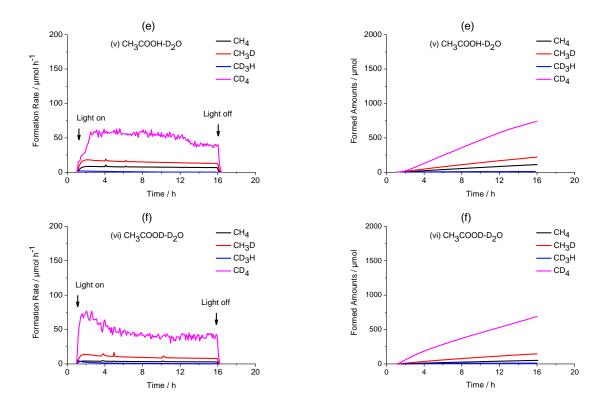
3.2.5.3 Formation of methanes

Figure 31 and 32 represent the formation rates and relative formed amounts, respectively, for the methane formation resulting from the photocatalytic degradation of acetic acid employing reaction systems (i – vi). It can be seen in Figure 31a, 31d, 32a, and 32d that CH_4 (507 µmol) and CD_4 (1066 µmol) were found to be the only reaction products in reaction systems (i) Pt/TiO₂-CH₃COOH-H₂O and (iv) Pt/TiO₂-CD₃COOD-D₂O, respectively. However, further analyses for the reaction systems (ii, iii, v, and vi) consisting of H/D mixtures illustrate the formation of four types of methane being different in isotopic composition such as: CH₄, CH₃D, CD₃H, and CD₄ (Figure 31b, 31c, 31e, and 31f).





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the CH₄, CD₄, CH₃D and CD₃H for: (a) reaction system-ii, (b) reaction system-iii, (c) concentration = $0.5 \text{ g } \text{L}^{-1}$, acetic acid concentration = 0.5 M, pH \approx pD = 2, reactor volume = 50 m L, irradiation time = 15 h, irradiation intensity : I_{250} - I_{450} = 30 mW cm⁻².

Figure 31: Photocatalytic formation rates of Figure 32: Photocatalytically formed amounts of the CH₄, CD₄, CH₃D and CD₃H for: (a) reaction system-ii, (b) reaction system-iii, (c) reaction system-v and (d) reaction system-vi, reaction system-v and (d) reaction system-vi, employing 1 wt % Pt TiO₂, photocatalyst employing 1 wt % Pt TiO₂, photocatalyst concentration = 0.5 g L⁻¹, acetic acid concentration = 0.5 M, pH \approx pD = 2, reactor volume = 50 m L, irradiation time = 15 h, irradiation intensity : I_{250} - I_{450} = 30 mW cm⁻².

A comparison between the evolved amounts of methane being different in isotopic composition is presented in Figure 33. The results obtained for methanes (i.e., CH₄, CH₃D, CD₃H, CD₄) are different from the published literature [36, 37, 84, 111]. According to the reported literature, CD₃H and CH₄ are the expected species from reaction systems (ii and iii) having H₂O as a solvent with CD₃COOD and CH₃COOD, respectively. Here, data presented in Figure 33 shows

that the reaction systems (ii and iii) result in the formation of CD_3H and CH_4 , respectively, as major reaction products besides CH_3D as the minor product. Moreover, the expected reaction product from reaction systems (v and vi) containing D_2O as a solvent with CH_3COOH and CH_3COOD is CH_3D . Unlike the published reports [84, 111], a proton exchange at methyl group (CH_3) of acetic acid has been observed for these reaction systems (v and vi). Unexpectedly, CD_4 was found to be the major reaction product in higher amounts from reaction systems having D_2O as a solvent with CH_3COOH and CH_3COOD .

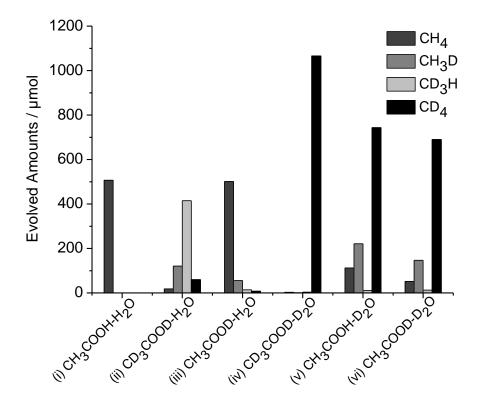


Figure 33: Amounts of the CH₄, CH₃D, CD₃H, and CD₄, photocatalytically formed from aqueous suspensions containing 1 wt % Pt/TiO₂ as the photocatalyst after an irradiation time of 15 h. *Experimental conditions:* as in Figure 31 - 32.

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3.2.5.4 Nuclear magnetic resonance study

Nuclear magnetic resonance (NMR) spectroscopy with H_2O suppression has been performed in order to confirm the proton exchange reaction (PER) determined by quadrupole mass spectrometer (QMS) mainly at the methyl group (CH₃) of acetic acid during photocatalytic experiments for the reaction systems (ii) Pt/TiO₂-CD₃COOD-H₂O and (v) Pt/TiO₂-CH₃COOH-D₂O. The NMR studies were carried out for reaction systems (ii) and (v) only, in the solid liquid phase before and after the illumination. For a typical experiment, suspension from reaction system (ii) Pt/TiO₂-CD₃COOD-H₂O was deaerated and transferred to the NMR tube before illumination. The NMR tube was then transferred to the sample holder and the NMR spectrum was measured. The spectrum taken before illumination for reaction system (ii) is presented in the Figure 34. It can be seen in Figure 34 that only a resonance peak corresponding to the H₂O signal is obvious while no other signal was detected. The same procedure was repeated for the suspension from reaction systems (v) Pt/TiO₂-CH₃COOH-D₂O. Figure 35 shows the NMR spectrum obtained from reaction system (v) prior to the illumination. Here, the resonance signals corresponding to the H₂O and methyl (CH₃) group of acetic acid were observed only (Figure 35).

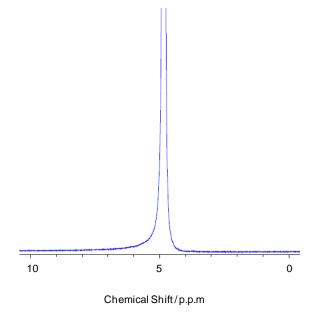


Figure 34: ¹H NMR spectra for reaction system (ii) Pt/TiO₂-CD₃COOD-H₂O, employing 1 wt % Pt/TiO₂, photocatalyst concentration = 0.5 g L⁻¹, acetic acid concentration = 0.5 M, before illumination.

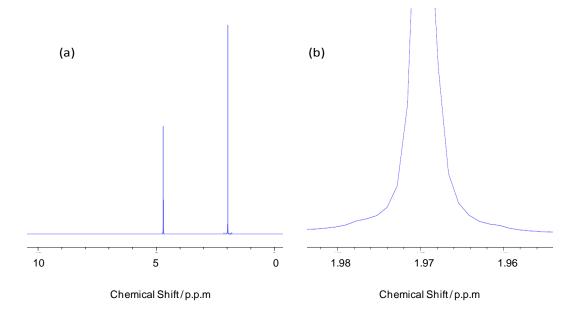


Figure 35: ¹H NMR spectra for reaction system (v) Pt/TiO₂-CH₃COOH-D₂O, employing 1 wt % Pt/TiO₂, photocatalyst concentration = 0.5 g L^{-1} , acetic acid concentration = 0.5 M, before illumination (a) Full spectrum, (b) Zoom image representing methyl (CH₃) group of acetic acid.

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Afterwards, a photocatalytic reaction was performed in a photoreactor attached to the quadrupole mass spectrometer (QMS) employing suspension from reaction system (ii) Pt/TiO₂-CD₃COOD-H₂O. Immediately after 15 h of illumination, the obtained suspension was transferred to the Argon (Ar) purged NMR tube *via* a syringe. This NMR tube was then placed in the NMR sample holder and measured immediately. The spectrum obtained after the illumination of suspension is shown in Figure 36a. A quintet signal with intensity (1:2:3:2:1, J = 2.2 Hz) as expected for CHD₂ moiety was observed for illuminated suspension from reaction system (ii) Pt/TiO₂-CD₃COOD-H₂O. The multiplicity was calculated according to the following relation:

$$M = 2 \times n \times I + 1$$
 Equation 21

Here, *n* and *I* are the number and spin of the interacting atoms, respectively. The obtained quintet signal from NMR employing reaction systems (ii) $Pt/TiO_2-CD_3COOD-H_2O$ was assigned to the formation of CHD₂COOD(H) species. This is the confirmation of our hypothesis about the occurrence of proton exchange reaction at the methyl group of acetic acid during a photocatalytic reaction.

The spectrum obtained from NMR spectroscopy for the reaction system (v) $Pt/TiO_2-CH_3COOH-D_2O$ is presented in Figure 36b (after illumination). The same procedure for sample preparation was repeated for this system (v) as defined for the reaction system (ii). Prior to the illumination, the suspension from reaction system (v) exhibits a typical resonance peak, which corresponds to the methyl group (CH₃) of acetic acid (Figure 35). After the suspension was illuminated, NMR determines a triplet signal (1:1:1, J = 2.2 Hz) having identical intensities besides the CH₃ signal of acetic acid (Figure 36b). By using the relation described in Equation 21, the obtained NMR signal from reaction system (v) $Pt/TiO_2-CH_3COOH-D_2O$ was assigned to $CH_2DCOOH(D)$ species.

However, in both reaction systems (ii) Pt/TiO₂-CD₃COOD-H₂O and (v) Pt/TiO₂-CH₃COOH-D₂O, the proton exchange reaction at the carboxylic group (COOH) of acetic acid occurred quickly. It should also be kept in mind that due to the employment of reaction systems having (ii) H₂O and (v) D₂O as a solvent, the NMR spectra demonstrated a slight shift (≈ 0.972) in the H₂O signal (Figure 34, and 35b). This shift in H₂O signal leads to a small shift in the quintet and triplet signals within the limits of ≈ 1.1 (Figure 35b and 36). However, the quintet and triplet signals still observed in close approximation with the peak depicting CH₃ from CH₃COOH.

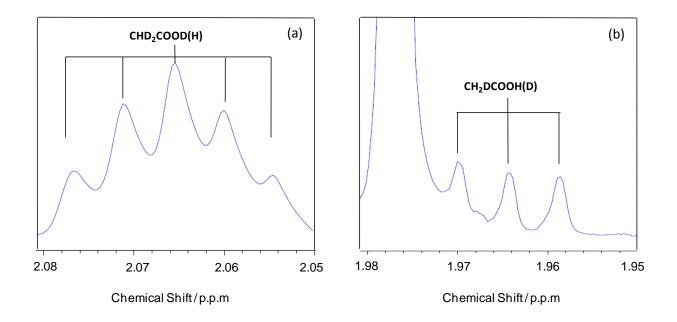


Figure 36: ¹H NMR spectra for (a) reaction system (ii) Pt/TiO₂-CD₃COOD-H₂O and (b) reaction system (v) Pt/TiO₂-CH₃COOH-D₂O, employing 1 wt % Pt/TiO₂, photocatalyst concentration = 0.5 g L⁻¹, acetic acid concentration = 0.5 M, reactor volume = 50 m L, irradiation time = 15 h, irradiation intensity : I_{250} - I_{450} = 30 mWcm⁻².

4. Discussion

This chapter will analyze the results obtained from the experimental work presented in chapter 3. The discussion will start by interpreting the influence of different experimental parameters affecting the product distribution resulting from the photocatalytic conversion of aqueous acetic acid in the presence of co-catalyst loaded TiO₂. Starting from the effect of various co-catalyst loadings on the surface of TiO₂ particles, the effect of different initial acetic acid concentrations (c_0) on the photocatalytic reaction rates and corresponding reaction product distribution will be explained. Depending on the various pH values, different reaction paths for the photo-induced degradation of aqueous acetic acid will be specified. Finally, details about the fundamental process for the photocatalytic decomposition of aqueous acetic acid on the basis of isotopic labelling studies will be elucidated.

4.1 General Remarks

In the present work, the photocatalytic transformation of aqueous acetic acid into main reaction products *e.g.*, carbon dioxide (CO₂), hydrogen (H₂), methane (CH₄) and ethane (C₂H₆) over cocatalyst loaded TiO₂ has been investigated. The quantitative analyses were made only for the gaseous products being generated inside the aqueous suspensions and exiting the photoreactor. Due to the employment of a batch reactor with respect to the suspensions, the possibility of taking the liquid samples during the photocatalytic reaction was limited. However, the employed photoreactor facilitates a continuous flow of the evolved gases to the quadrupole mass spectrometer (QMS). Thus, the data shown in this work refers to the quantitative amounts of gaseous products only. The amounts of the gaseous reaction products exiting the photoreactor are mainly dependent on the equilibrium between liquid – vapour phase [112].

During 15 h of illumination, the formation rates in all experimental runs (Figure 14, 15, 18, 21, 25, 28, and 31) for almost all reaction products did not remain constant. The results presented in literature also show a same behaviour when CH_3COOH or other organic molecules were employed as electron donors [104, 113]. A possible explanation for the observed decreasing trend in the formation rates of the formed reaction products could be that the photoreactor employed in

this study does not allow a continuous flow of suspensions. Therefore, a decrease in the concentration of the reactants results in the decrease of formation rates of all gaseous reaction products. However, it can be seen in Table 3, 4, and 5 that the fractional conversions $X_{\rm C} = \frac{n({\rm CO}_2)+n({\rm CH}_4)+2n({\rm C}_2{\rm H}_6)}{2n_0}$ as well as $X_{\rm H} = \frac{n({\rm H}_2)+2n({\rm CH}_4)+3n({\rm C}_2{\rm H}_6)}{2n_0}$ (where, $n({\rm CO}_2)$, $n({\rm CH}_4)$, $n({\rm H}_2)$, $n({\rm C}_2{\rm H}_6)$, and n_0 are the evolved amounts of CO₂, CH₄, H₂, C₂H₆, and the initial amount of CH₃COOH present in the suspension, respectively) calculated after 15 h of illumination for initial acetic acid concentration ≥ 0.5 M exhibit less than 4 % conversion of acetic acid into the detected reaction products (Table (3 – 5), (columns 8, 9)). Therefore, the change of concentration seems not to be the reason for the observed decrease in reaction rate. This means that during a photocatalytic reaction for the conversion of acetic acid, the surface of photocatalyst is changed. The reason behind these surface changes of the photocatalyst material might be the type of reaction mechanism occurred during photocatalytic degradation of aqueous organic compound.

Moreover, a comparison between the expected atomic ratios of CH₃COOH molecule $\left(\frac{n(C)}{n(O)} = 1, \frac{n(H)}{n(O)} = 2, \text{ and } \frac{n(H)}{n(C)} = 2\right)$ and the experimentally obtained ratios between the atoms composing CH₃COOH $\left(0.6 < \frac{n(C)}{n(O)} < 0.9, 1.0 < \frac{n(H)}{n(O)} < 2.0, \text{ and } 1.4 < \frac{n(H)}{n(C)} < 2.1\right)$ exhibits the existence of other reaction products besides the main products (CO₂, CH₄, H₂, and C₂H₆). The qualitative gas phase analysis in the QMS also provides evidence for the production of other organic compounds (*e.g.*, HCHO, CH₃OH, C₂H₅OH, and HCOOH), but the formed concentrations of these compounds were observed to be rather low in the gas phase exiting the photoreactor (Figure 23). The difference in the obtained amounts from all reaction products in all experimental runs exhibits an experimental error of ±10 %.

In general, the excitation of a semiconductor material by the photons having energy higher than the energy of its band-gap (E_g) leads to the transfer of electrons from valence band (VB) to the conduction band (CB) of the semiconducting material while creating positively charge holes (h_{VB}^+) at the valence band edge (E_{VB}) of semiconductor. Considering the TiO₂ as a semiconducting photocatalyst, under anaerobic reaction conditions, a fast recombination between photo-generated valence band holes (h_{VB}^+) and conduction band electrons (e_{CB}^-) is expected. In the absence of O₂, the light-induced semiconductor e_{CB}^- move freely in TiO₂. Due to the lattice vibration, the photo-excited e_{CB}^- immediately release their energy and recombine with the photo-

generated h_{VB}^+ even in the presence of a h_{VB}^+ scavenger/electron donor. It can be seen in Figure 37, that the driving force for an interfacial electron transfer of the P25 TiO₂ e_{CB}^- to protons (H⁺) being present at the TiO₂ CB is very small. On the other hand, the valence band position of TiO₂ seems (Figure 37) to be suitable for the oxidation reaction of H₂O as well as CH₃COOH. Consequently, a reaction system, containing bare TiO₂ as a photocatalyst and aqueous acetic acid as an electron donor, does not gives the significant amounts of the reaction products (Figure 14) during photo-induced transformation of aqueous acetic acid due to the rapid e_{CB}^- and h_{VB}^+ recombination. In order to suppress the fast recombination between photo-generated charge carriers (e_{CB}^- and h_{VB}^+), the surface of TiO₂ is modified with various co-catalysts such as noble metals or metal oxides. The co-catalysts loaded onto the surface of TiO₂ act as electron sinks thus hindering the rapid e_{CB}^- and h_{VB}^+ recombination. A detailed discussion about co-catalyst loaded photocatalyst has been given in the following chapter (4.2.1).

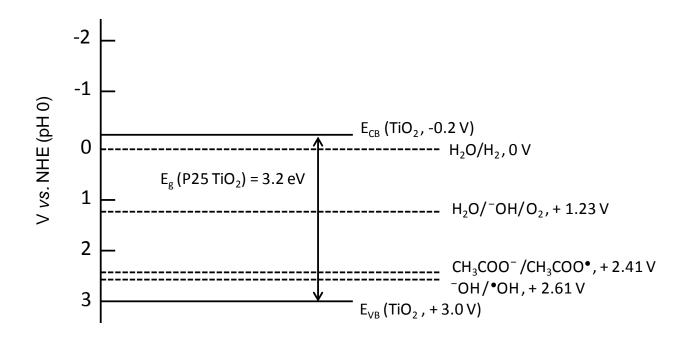


Figure 37: Schematic illustration of energy band diagram for TiO_2 P25 along with the reduction and oxidation potential of H₂O [114], one electron oxidation potential of acetate (CH₃COO⁻) [115], and oxidation potential of [•]OH [114], respectively.

4.2 Factors influencing the reaction rates and product distribution

4.2.1 Effect of co-catalyst

During a photocatalytic reaction, semiconductor (SC) materials play a key role in defining the oxidation and reduction reactions. However, the photocatalytic reactions mainly for the production of H₂ in significant amounts require the assistance of a co-catalyst material. In these reactions, the deposition of co-catalysts such as noble metals or metal oxides on the surface of photocatalyst *i.e.*, TiO₂ acts as an efficient conduction band electrons (e_{CB}^-) trap and facilitates the reduction of protons (H⁺) adsorbed on the surface of co-catalysts into hydrogen atoms ($^{\bullet}$ H) (Figure 38). These adsorbed $^{\bullet}$ H further dimerize to form H₂. In parallel to this reaction, the TiO₂ photo-generated valence band holes (h_{VB}^+) react with the surface adsorbed RCOOH or H₂O yielding RCOO[•] and $^{\bullet}$ OH. The formed $^{\bullet}$ OH further oxidize organic molecules adsorbed on the surface of photocatalyst material (Figure 37, and 38). The deposition of co-catalyst material also improves the reduction of H⁺ by shifting the position of Fermi level towards more negative potential value (Figure 38). Hence, the interfacial charge transport becomes more efficient.

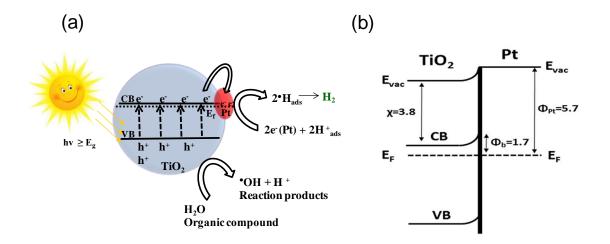


Figure 38: (a) Schematic illustration of photocatalytic H₂ evolution reaction, and (b) energy band diagram for Pt/TiO₂ junction. (E_{vac} , E_F , Φ_{Pt} , χ , Φ_b represents vacuum level, fermi level, work function of Pt, electron affinity of TiO₂ conduction band and Schottky barrier height, respectively (all values in eV)) [116].

The use of a co-catalyst is not limited to the H⁺ reduction reaction only, but it can also assist the transfer of an electron to the excited semiconductor [66, 117-120]. In order to obtain significant yields of the required product, the choice of a suitable co-catalyst is pre-requisite. This work is an appraisal for the photocatalytic decomposition of aqueous acetic acid into useful solar fuels employing various noble metals such as Pt, Rh, Au, and Ag as well as metal-oxides e.g., IrO₂ and RuO₂ loaded TiO₂ particles under anaerobic conditions. The choice of particularly IrO₂ and RuO₂ metal-oxides as co-catalyst mainly for the reduction reaction has been made due to their metallic properties [121, 122]. Numerous published reports demonstrate the significance of IrO₂ and RuO₂ acting as both H₂ evolution and O₂ evolution co-catalysts [123-131]. It is obvious from the Figure 17 that the photocatalytic activity increases significantly when TiO_2 is loaded with the above mentioned co-catalysts as compared to the bare TiO2 (Figure 14). According to the evolved amounts of CO_2 , the photocatalytic activity is found to increase in the following order: Ag/TiO₂ < $Au/TiO_2 < Rh/TiO_2 < RuO_2/TiO_2 < IrO_2/TiO_2 < Pt/TiO_2$. Figure 15 and 16 clearly indicates that during photocatalytic decomposition of aqueous acetic acid, the loading of various co-catalysts onto the surface of TiO₂ strongly affects the reaction rates and the evolved amounts of gaseous products over 15 h of irradiation.

The initial (after 2 h illumination) as well as overall (after 15 h illumination) photonic efficiencies for the main reaction products (CO₂, CH₄, and H₂) have also been calculated and are presented in Figure 39. The details regarding the calculations of photonic efficiency have been given in chapter 2.6. The initial and overall photonic efficiencies measured for CO₂ and CH₄ evolution by utilizing the variety of noble metals as well as metal-oxides exhibits Pt and IrO₂ loaded TiO₂ as the efficient photocatalyst (Figure 39a, and 39c). In comparison to this, only Pt/TiO₂ and Rh/TiO₂ show significant photocatalytic activities for H₂ evolution reaction (Figure 39b). Additionally, It can be seen in Table 3 (column 18) that the ratio between the sum of formed amount of hydrocarbons (CH₄, and C₂H₆) and the formed amount of H₂ was calculated to be varying in the range of 1.5 - 10.5.

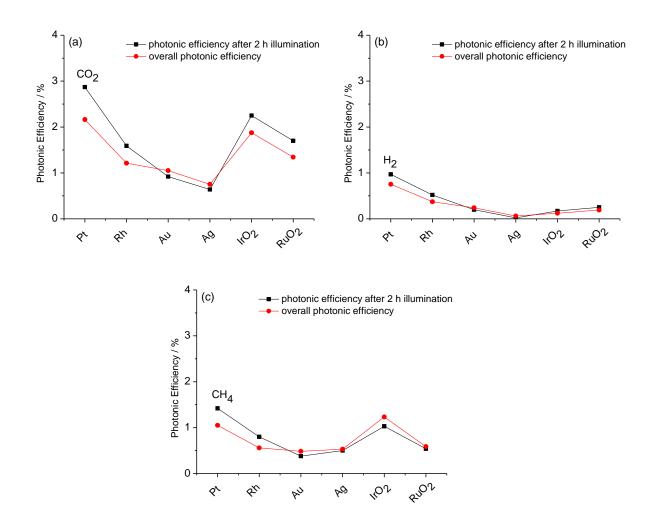


Figure 39: Photonic efficiency for the main reaction products, *i.e.*, (a) CO_2 , (b) H_2 , and (c) CH_4 , calculated for the initial (after 2 h illumination) and overall (after 15 h illumination) formation rates. *Experimental conditions:* as in Figure 15 – 16.

1	2	3	4	5	6	7	8	9	10	11	12	13
M/TiO ₂	C_0	n_0	<i>n</i> (CO ₂)	$n(H_2)$	$n(CH_4)$	$n(C_2H_6)$	X _C	$X_{ m H}$	$n(H_2)$	$n(CH_4)$	$n(C_2H_6)$	$n(C_2H_6)$
	М	μmol	μmol	μmol	μmol	μmol	_	_	$n(CO_2)$	$n(CO_2)$	$n(CO_2)$	$n(CH_4)$
									_	_	_	_
Pt/TiO ₂	0.5	25000	1027	358	511	24	0.032	0.029	0.35	0.50	0.02	0.05
Rh/TiO ₂	0.5	25000	580	177	266	13	0.017	0.015	0.31	0.46	0.02	0.05
Au/TiO ₂	0.5	25000	499	115	230	20	0.015	0.013	0.23	0.46	0.04	0.09
Ag/TiO ₂	0.5	25000	357	29	252	6	0.012	0.011	0.08	0.71	0.02	0.02
IrO ₂ /TiO ₂	0.5	25000	890	58	586	24	0.030	0.026	0.07	0.66	0.03	0.04
RuO_2/TiO_2	0.5	25000	638	92	279	7	0.019	0.013	0.14	0.44	0.01	0.03

Table 3: Effect of the different co-catalyst on the amounts of the main reaction products photocatalytically formed during 15 h of irradiation.

Experimental conditions: photocatalyst concentration = 0.5 g L⁻¹, initial acetic acid concentration (c_0) = 0.5 M, pH 2, suspension volume = 50 mL, irradiation time = 15 h, irradiation intensity I₂₅₀-I₄₅₀ = 30 mW cm⁻².

Table 3 (continued): Effect of the different co-catalyst on the amounts of the main reaction products photocatalytically formed	
during 15 h of irradiation.	

14	15	16	17	18	19
$2n(C_2H_6)$ $n(\cdot CH_6)$	H_{3} = $\frac{n(CH_4) + 2n(C_2H_6)}{n(\cdot CH_3)}$ $\frac{n(\cdot CH_3)}{n(\cdot CH_3)}$	$-\frac{n(CH_4) + 2n(C_2H_6)}{n(H \cdot)}$	$=\frac{n(\mathrm{CH}_4)+2n(\mathrm{H}_2)}{2}$	$n(CH_4)+n(C_2H_6)$	M/TiO ₂
$n(CH_4)+2n(C_2H_6)$ $n(H_6)$	$1 \cdot) = n(CH_4) + 2n(H_2) n(CO_2)$	$n(\mathrm{CO}_2)$ $n(\mathrm{CO}_2)$	$n(CO_2)$	$n(H_2)$	
_	_	_	_	_	
0.09	0.46	0.54	1.19	1.49	Pt/TiO ₂
0.09	0.47	0.50	1.07	1.58	Rh/TiO ₂
0.15	0.59	0.54	0.92	2.17	Au/TiO_2
0.05	0.85	0.74	0.87	8.90	Ag/TiO ₂
0.08	0.90	0.71	0.79	10.52	IrO ₂ /TiO ₂
0.05	0.63	0.46	0.73	3.11	RuO ₂ /TiO ₂

Experimental conditions: photocatalyst concentration = 0.5 g L⁻¹, initial acetic acid concentration (c_0) = 0.5 M, pH 2, suspension volume = 50 mL, irradiation time = 15 h, irradiation intensity I₂₅₀-I₄₅₀ = 30 mW cm⁻².

Figure 40 presents the plots of evolved amounts of $n(CH_4)$, $n(H_2)$, $n(C_2H_6)$, $n(H^{\bullet})$, and $n({}^{\bullet}CH_3)$ (where, $n(H^{\bullet}) = 2n(H_2) + n(CH_4)$, and $n({}^{\bullet}CH_3) = n(CH_4) + 2n(C_2H_6)$) against the formed amounts of CO₂ during 15 h of illumination. The higher amounts of CH₄ seem to be associated with the rapid reaction rate of photo-decarboxylation (*i.e.*, the evolution of CO₂ in higher amounts) in all experimental runs (Figure 40a). However, the formation of H₂ in significant amount does not have any relation with the photo-decarboxylation reaction rate. An increment in the evolved amount of CO₂ was observed to give an augmentation in the formed amounts of both ${}^{\bullet}CH_3$ and ${}^{\bullet}H$ (Figure 40b). On the contrary, the trend shown by metal-oxide loaded TiO₂ particles was found to be different.

Considering the effect of only noble metal co-catalyst loaded TiO₂, it can be seen (Figure 17) that the amounts of CO₂, H₂, CH₄, and C₂H₆ formation increase in the following sequence: Ag/TiO₂ < Au/TiO₂ < Rh/TiO₂ < Pt/TiO₂. Fu *et al.* [132] studied the hydrogen evolution reaction (HER) from aqueous glucose suspensions employing 1 wt % metal-loaded TiO₂ particles. They observed an increase in the photocatalytic activity for H₂ production employing various metal-loaded TiO₂ in the following order: Ag/TiO₂ \approx Ru/TiO₂ < Au/TiO₂ \approx Rh/TiO₂ < Pt/TiO₂ < Pd/TiO₂. The authors ascribed this order to the work function (Φ) values of the noble metals.

In comparison to the TiO₂, the large Φ of noble metals creates a Schottky barrier at the metal/TiO₂ contact thus reducing the rapid recombination of photo-generated charge carriers (e_{CB}^- and h_{VB}^+). Consequently the photocatalytic activity is increased. The higher value of Φ however results in the formation of Schottky barrier with larger barrier height. Hence, the photocatalytic activity becomes more significant [132]. The photocatalytic activity with respect to the Φ value employing metal loaded TiO₂ particles along with 2-propanol and ethanol has also been reported in literature [37, 133, 134]. The Φ of a material does not correspond to its bulk, but it is actually defined with respect to the surface of a material based on its stoichiometry, exposed crystal facets and nearby species [135, 136]. For instance, it has been reported in literature that the deposition of RuO₂ films at ambient temperature onto BaTiO₃, SrTiO₃ and TiO₂ depicts 6.1 and 6.2 eV as Φ values of RuO₂ [137, 138].

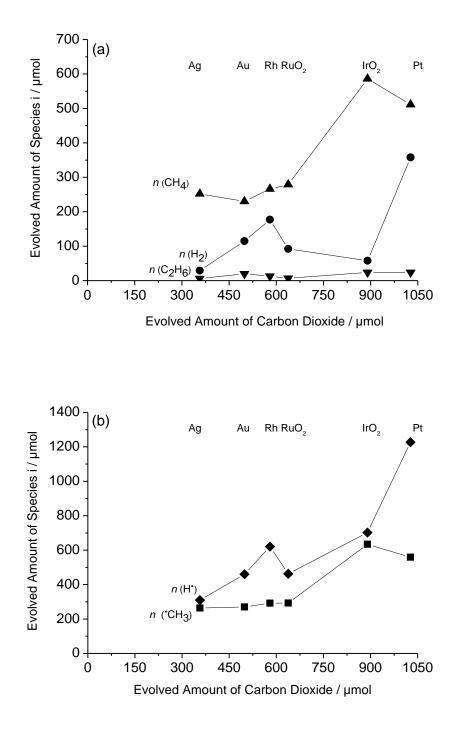


Figure 40: Amounts of (a) CH_4 , H_2 , and C_2H_6 , and (b) H^{\bullet} , and ${}^{\bullet}CH_3$ evolved during 15 h of irradiation of aqueous acetic acid in the presence of co-catalyst-loaded TiO₂ *vs.* amount of CO₂. *Experimental conditions*: as in Figure 15 – 16.

In another study [139], the Φ of RuO₂ films deposited onto the SiO₂-Si was reported as 5.2 eV before any calcination treatment. However, the calcination of the employed RuO₂ films at 300 °C as well as 500 °C resulted in comparatively lower work function values such as 5.17 eV and 5.03 eV, respectively. The authors attributed this decrease in the Φ values to the improved crystallinity of the films at higher temperature values.

This means that the various synthesis methods used to prepare the metal or metal-oxide loaded photocatalyst result in shifting the Φ of the respective co-catalyst. Therefore, the results obtained by loading of the metals or metal oxides onto the surface of photocatalyst employing different synthesis conditions cannot be compared. Sakata *et al.* [37] observed that using various metal loaded TiO₂ powders in the aqueous suspensions of ethanol, the formation rates for H₂ increased as follow: Ag/TiO₂ < Cu/TiO₂ < Au/TiO₂ < Rh/TiO₂ < Pd/TiO₂ < Pt/TiO₂. Sakata and co-workers [37] also examined the role of various metal-loaded TiO₂ for CH₄ formation from aqueous carboxylic acid (acetic acid, and propionic acid) suspensions. They observed the order for the formation rate of CH₄ as: Ag/TiO₂ < Rh/TiO₂ < Au/TiO₂ < Cu/TiO₂ < Pd/TiO₂ < Pd/TiO₂. Even though, the Φ seemed to affect the photocatalytic activity for both H₂ and CH₄ formation to a great extent, the other physio-chemical factors associated with the metal-semiconductor cannot be neglected. For example, (1) the bond dissociation energy for the metal-hydrogen (metal-H) or metal-carbon (metal-C) bonds, (2) the enthalpy of the adsorbed reactants and formed products, etc. However, in the present work, these factors will not be discussed.

Here, Figure 41 depicts the plots of formed amounts of $n(CO_2)$, $n(CH_4)$, $n(H_2)$, $n(H^{\bullet})$, and $n({}^{\bullet}CH_3)$ against reported work function (Φ) values of the metal or metal oxide co-catalyst. It is clear from Figure 41 that the formed amounts of all reaction products such as: $(n(CO_2))$, $(n(CH_4))$, $(n(H_2))$ and reaction intermediates *i.e.*, $(n(H^{\bullet}))$, and $(n({}^{\bullet}CH_3))$ are directly proportional to the increasing Φ values of the respective noble metal co-catalysts. On the contrary, the pattern shown by the metal-oxide (IrO₂ and RuO₂) co-catalysts for the formed amounts of reaction products as well as reaction intermediates *vs*. Φ is different (Figure 41). During the photocatalytic transformation of aqueous acetic acid, IrO₂ and RuO₂ do not seem to be very active for H₂ evolution reaction, but higher amounts of CO₂ and CH₄ were obtained. The formed amounts of CO₂ and CH₄ using IrO₂ as a co-catalyst are comparable with those obtained by utilizing Pt as a co-catalyst (Figure 41).

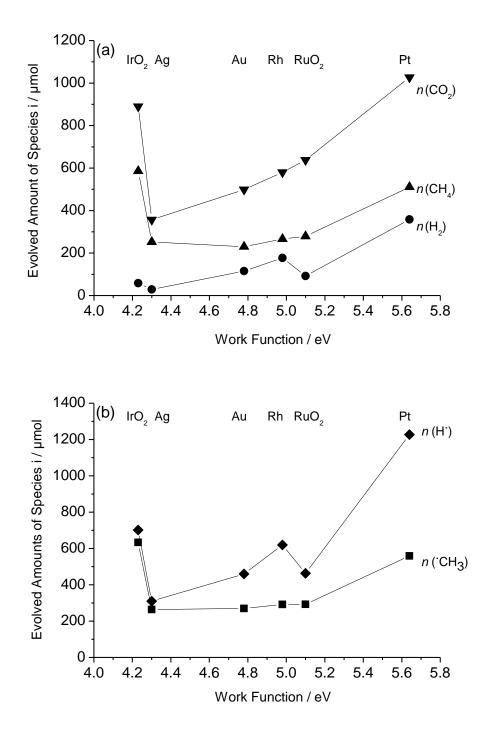


Figure 41: Amounts of (a) CO₂, CH₄, H₂, and C₂H₆, and (b) [•]H, and [•]CH₃, evolved during 15 h of irradiation of aqueous acetic acid in the presence of co-catalyst-loaded TiO₂ *vs*. work function of the respective co-catalyst. The values of the work function have been taken from Ref. [140], [141], and [142]. *Experimental conditions*: as in Figure 15 – 16.

Due to the differences in the obtained photocatalytic activity using metals or metal oxides loaded TiO₂ particles, it is therefore important to discuss the surface reactions occurring at the surface of metal-TiO₂ and metal-oxide-TiO₂ separately. Generally, the higher photocatalytic activity employing noble metal-TiO₂ is attributed to the efficient separation of photo-generated charge carrier caused by the interface formed at metal-TiO₂ contact. An electric field is actually produced at the metal-TiO₂ interface thus the fast recombination between photo-generated e_{CB}^{-} and h_{VB}^{+} is hindered. For metals having large Φ values in comparison to the Φ of TiO₂, the interfacial electron transfer from conduction band of TiO₂ into the metals becomes more efficient. A slight band bending at the metal/TiO₂ interface is also an important factor which facilitates the electron transfer between metal and TiO₂ [137].

Usually, in photocatalytic reaction systems consisting of metal/TiO₂ and aqueous organic suspensions, the H⁺ are reduced on the metal surface resulting in the formation of adsorbed $^{\bullet}$ H (Equation 7). Also, the organic compound *i.e.*, CH₃COOH in the present study, is oxidized at the TiO₂ surface yielding CH₃COO[•], followed by the decomposition of CH₃COO[•] into $^{\bullet}$ CH₃ and CO₂ (Equation 6). The oxidation of the CH₃COOH molecule at the surface of TiO₂ occurs due to the transfer of an electron to the VB of TiO₂. Subsequently, the generated reaction intermediates ($^{\bullet}$ CH₃ and the $^{\bullet}$ H adsorbed at the metal surface results in the formation of CH₄ as the final reaction product (Equation 9). Moreover, the dimerization of $^{\bullet}$ H and $^{\bullet}$ CH₃ gives H₂ and C₂H₆ as the final reaction products (Equation 8, and 10) resulting from the photo-induced degradation of aqueous acetic acid. However, the reactions 8 and 9 seemed to compete depending on the employed reaction conditions (Figure 17).

The photocatalytic degradation of aqueous acetic acid was supposed to follow a slightly different reaction pathway employing metal-oxide loaded TiO₂ as photocatalyst. Depending on the synthesis conditions, the metal-oxide co-catalyst can serve as either (1) electrons sink, or (2) holes trap. It has been reported by Sakata *et al.* [143] that the photocatalytic activity for hydrogen evolution reaction (HER) from aqueous ethanol suspensions increases in the following order: $TiO_2 << RuO_2/TiO_2 < Pd/TiO_2 < Pt/TiO_2$. The authors ascribed the significant amounts of H₂ formation employing RuO₂ to the fact that this acts as a reduction co-catalyst and exhibits the properties like Pt. They claimed that employing metal as well as metal loaded TiO₂ particles, the

photo-generated h_{VB}^+ react with the ethanol molecules and continue the oxidation process at the surface of TiO₂ while e_{CB} gathered in the particles of TiO₂ causing a cathodic shift in its Fermi level. Hence, the H⁺ reduction reaction becomes more favourable. Generally, in the presence of an oxidizing agent such as methanol or ethanol, TiO₂ can store a large number of photo-generated electrons but the driving force of TiO_2 conduction band electron (e_{CB}^-) for an interfacial electron transfer to protons (H⁺) being present at the TiO₂ conduction band is very small [144-146]. Thus, the cathodic shift in the Fermi level caused by the loading of co-catalyst enhances the interfacial charge transfer reaction [45, 46, 147-149]. In another study, Uddin et al. [137] examined the dye degradation reaction employing RuO₂/TiO₂ as a photocatalyst under aerobic conditions. They credited the efficient photocatalytic activity obtained for this reaction to the existence of a Schottky barrier at the RuO₂/TiO₂ contact. The electrons at the surface of TiO₂ captured by the O_2 (acting as electron acceptor) while the transfer of electrons from RuO_2 to the $TiO_2\ VB$ suggests that the RuO₂ acts as an oxidizing co-catalyst. It can be seen from Figure (17 and 40) that the formed amounts of $n(CO_2)$, $n(CH_4)$ and $n({}^{\bullet}CH_3)$ employing RuO₂/TiO₂ as a photocatalyst could be considered in the sequence given by Φ values. However, the formed amounts of $n(H_2)$ and $n(\mathbf{H}^{\bullet})$ were observed to be rather smaller with respect to the order of Φ values.

The use of IrO₂/TiO₂ photocatalyst for the degradation of aqueous acetic acid was found to be very efficient for the CH₄ production (Figure 40, and 41). The calculated ratio (Table 3 (column 15)) between the formed amounts of methyl radical ($^{\circ}$ CH₃) and hydrogen atom (H[•]) $\left(\frac{n(\text{CH}_3)}{n(\text{H}^-)} = 0.9\right)$ depicts the capability of IrO₂ as a reduction co-catalyst *i.e.*, facilitating the formation of H[•]. However, the reaction of H[•] with $^{\circ}$ CH₃ seemed to be a favourable reaction $\left(\frac{n(\text{CH}_4)+n(\text{C}_2\text{H}_6)}{n(\text{H}_2)} = 10.5\right)$ as can be seen in Table 3 (column 18). It should also be noted that Pt/TiO₂ and IrO₂/TiO₂ exhibit comparable photocatalytic activities for CO₂ and CH₄ formation (Figure 42). This suggests that the Φ value for both Pt (5.65 eV) and IrO₂ (4.23 eV) is not the key parameter here. Meekins *et al.* [144] reported that the IrO₂ loaded on the surface of TiO₂ acts as a hole acceptor unless a hole equilibrium is achieved by both oxides. They also stated that the transfer of trapped holes from TiO₂ to IrO₂ is also possible. Liu *et al.* demonstrated the efficient photocatalytic activity for O₂ evolution reaction employing IrO₂/TiO₂ as holes acceptor [150]. Hence, it is assumed that, when metal-oxides are used as co-catalyst, they act as holes acceptor

while facilitating the oxidative step on their surface, whereas the reduction of H^+ occurs at the TiO₂ surface.

It can be concluded from the above discussion that, during a photocatalytic reaction, the chemical nature of metal-oxide co-catalyst does not change. On the other hand, it has been reported in literature that structural changes arise in both RuO_2 and IrO_2 co-catalysts during the electrochemical H₂ production reaction [151-154]. Thus, the structural changes of the employed metal-oxides in the present study for the photocatalytic decomposition of the aqueous acetic acid cannot be neglected. The formation rates of the reaction products as well as reaction intermediates resulting in different product distribution could be attributed to these changes.

However, Pt/TiO_2 was found to be the photocatalyst exhibiting the highest photonic efficiency under the experimental conditions of this study for both oxidation and reduction reaction during light-induced transformation of aqueous acetic acid into valuable solar fuels. Therefore, this photocatalyst has been used to investigate other parameters that affect the photocatalytic reaction.

4.2.2 Effect of concentration

Generally, the concentration of a compound is known to affect its reaction rate. With a specific time interval, the changes in the formed amounts of reaction products are related to the concentration of reactants. However, the variations in the ratios of these reaction products are not essential. It can be seen in Figure 18, 19, 20 as well as in Table 4 that both the formation rates and the corresponding product distribution vary with the change in the initial acetic acid concentration. It is also obvious from Figure 20 that an increase in the initial concentration (c_0) of acetic acid up to 0.05 M ($n_0 = 2500 \mu \text{mol}$, n_0 represents the amount of initial acetic acid molecules present in the suspension) results in an increment of the formed amounts of all reaction products. The concentration over the range 0.05 M $\leq c_0 \leq 1$ M (corresponding to 2500 $\mu \text{mol} \leq n_0 \leq 50000 \mu \text{mol}$), a decrease in the formation rate of all reaction intermediates as well as reaction products is obvious (Figure 18, Table 4). The photonic efficiencies were also calculated for the main reaction products (CO₂, CH₄ and H₂) evolved during the light induced decomposition of aqueous acetic acid at varying initial concentrations and are shown in Figure 42. Usually, at a specific initial concentration of the reactant and particular irradiance intensity,

the number of photons absorbed by the photocatalyst as well as the number of active sites on the surface of the photocatalyst remains constant. An increase in the concentration of the reactant leading to an increase in the formation rates of the reaction products during photocatalytic H_2 evolution reaction (HER) has been published in literature [155]. On the other hand, it has also been shown that an increase in the concentration of reactant up to a specific value results in lowering the HER [104, 156, 157]. However, the results obtained in this study depict the change in formation rate as well as product distribution with respect to the initial concentration of acetic acid.

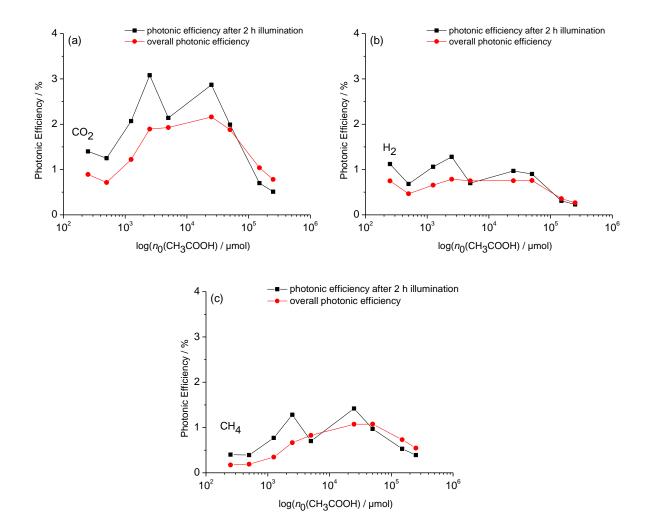


Figure 42: Photonic efficiency for the main reaction products, *i.e.*, (a) CO_2 , (b) H_2 , and (c) CH_4 , calculated for the initial (after 2 h illumination) and overall (after 15 h illumination) formation rates. *Experimental conditions:* as in Figure 18 – 19.

Yoneyama and co-workers [90] studied the effect of various acetic acid concentrations on the formation rates of the main reaction products employing Pt/TiO₂ under anaerobic conditions. The initial concentration values chosen in their work were in the following range: $1 \text{ M} \le c_0 \le 8.2 \text{ M}$, at the constant pH value (3.1). They observed CO₂, CH₄, H₂, and C₂H₆ as main reaction products. They found an increase in the formation rates of all reaction products while increasing the concentration of acetic acid up to 5 M. A further increase in the concentration values results in a decreased formation rate for all reaction products. Zheng et al. [100] also investigated the effect of initial acetic acid concentration on the formation rates of the main reaction products using Pt/TiO_2 under anaerobic conditions. They reported an increase in the formation rates for all reaction products (CO₂, CH₄, H₂, and C₂H₆) up to 0.11 M $\leq c_0$. Though, a further increase of up to 0.26 M $\leq c_0$ results in lowering the formation rates of all reaction products. In another study, Mozia et al. [35] demonstrated the optimal concentration of acetic acid to be 1 M with Fe₂O₃- TiO_2 photocatalyst. The differences in the optimal concentration values might correspond to the different experimental conditions or different photocatalysts. The decrease in the photocatalytic activity after a specific initial concentration of the reactant could be attributed to the blockage of the active sites on the surface of photocatalyst [157].

The experimental results obtained from this study employing Pt/TiO₂ as a photocatalyst at pH 2 show that an increase in initial concentration of acetic acid results in a decrease of $\frac{n(H_2)}{n(CO_2)}$ ratio and increase in $\frac{n(CH_4)}{n(CO_2)}$ ratio as presented in Figure 43 and Table 4 (column 10, and 11). On the other hand, the change in the initial concentration of aqueous acetic acid does not seem to affect the ratio between C₂H₆ and CH₄ formation to a great extent (Figure 43, Table 4 (column 13)).

According to the data presented in Figure 43, it can be estimated that almost 13% of the formed •CH₃ undergo a dimerization while resulting in C₂H₆ formation as the final product. Yoneyama *et al.* [90] observed that a raise in the initial concentration of acetic acid up to 6 M while keeping other parameters constant results in an increase in the ratio of formed amounts of CH₄ and C₂H₆. They stated that the formation rate of C₂H₆ is directly proportional to the increasing concentration of acetic acid. The authors also suggested that the formation rate of •CH₃ and the ratio $\frac{n(CH_4)}{n(C_2H_6)}$ should be inversely proportional to each other *i.e.*, $\left(\frac{1}{n(\cdot CH_3)} \sim \frac{n(CH_4)}{n(C_2H_6)}\right)$. The formation rate (*r*) of methyl radical (•CH₃) is given by : $\left(r(\cdot CH_3) = \frac{n(CH_4) + 2n(C_2H_6)}{\Delta t}\right)$. According to the experimental

conditions of the present work, the relationship between the formed amounts of C_2H_6 and CH_4 should be: $\frac{n(C_2H_6)}{n(CH_4)} \sim (n(CH_4) + 2n(C_2H_6))$. However, it can be clearly seen in Table 4 that the expected linear relationship between formed amounts of C_2H_6 and CH_4 could not be proven.

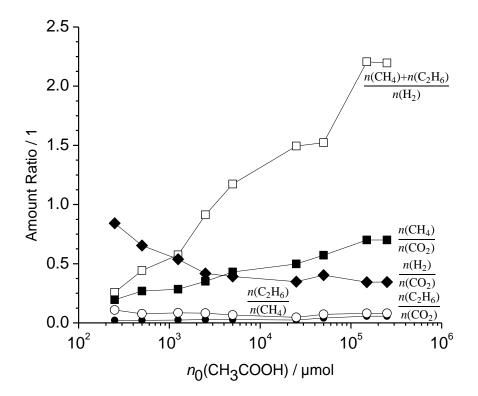


Figure 43: Ratios between the detected amounts of methane $n(CH_4)$, ethane $n(C_2H_6)$, molecular hydrogen $n(H_2)$, and carbon dioxide $n(CO_2)$ *vs.* the initial amount n_0 of acetic acid. *Experimental conditions:* as in Figure 18 – 19.

1	2	3	4	5	6	7	8	9	10	11	12	13
M/TiO ₂	c_0	n_0	<i>n</i> (CO ₂)	$n(H_2)$	$n(CH_4)$	$n(C_2H_6)$	$X_{\rm C}$	$X_{ m H}$	<i>n</i> (H ₂)	$n(CH_4)$	$n(C_2H_6)$	$n(C_2H_6)$
	Μ	μmol	μmol	μmol	μmol	μmol	_	_	$n(CO_2)$	$n(CO_2)$	$n(CO_2)$	<i>n</i> (CH ₄)
									_	_	_	_
Pt/TiO ₂	0.005	250	424	357	83	9	1.050	1.100	0.84	0.20	0.02	0.11
Pt/TiO ₂	0.01	500	338	221	91	7	0.443	0.424	0.65	0.27	0.02	0.08
Pt/TiO ₂	0.025	1250	581	312	165	14	0.310	0.274	0.54	0.28	0.02	0.08
Pt/TiO ₂	0.05	2500	900	375	316	26	0.254	0.217	0.42	0.35	0.03	0.08
Pt/TiO ₂	0.1	5000	915	358	394	26	0.136	0.122	0.39	0.43	0.03	0.07
Pt/TiO ₂	0.5	25000	1027	358	511	24	0.032	0.029	0.35	0.50	0.02	0.05
Pt/TiO ₂	1	50000	893	360	511	37	0.015	0.015	0.40	0.57	0.04	0.07
Pt/TiO ₂	3	150000	495	170	347	28	0.003	0.003	0.34	0.70	0.06	0.08
Pt/TiO ₂	5	250000	371	128	260	21	0.001	0.001	0.35	0.70	0.06	0.08

Table 4: Effect of the acetic acid concentration on the amounts of the main reaction products photocatalytically formed during 15 h of irradiation.

Experimental conditions: photocatalyst concentration = 0.5 g L⁻¹, 0.005 M \leq initial acetic acid concentration (c_0) \leq 5 M, pH 2, suspension volume = 50 mL, irradiation time = 15 h, irradiation intensity I₂₅₀-I₄₅₀ = 30 mW cm⁻².

Table 4 (continued): Effect of the acetic acid concentration on the amounts of the main reaction products photocatalytically formed	
during 15 h of irradiation.	

14		15		16		17	18	19
$2n(C_2H_6)$	$n(\cdot CH_3)$	$n(CH_4)+2n(C_2H_6)$	$n(\cdot CH_3)$	$n(\mathrm{CH}_4) + 2n(\mathrm{C}_2\mathrm{H}_6)$	n(H·)	$n(CH_4) + 2n(H_2)$	$n(CH_4)+n(C_2H_6)$	M/TiO ₂
$\overline{n(\mathrm{CH}_4)+2n(\mathrm{C}_2\mathrm{H}_6)}$	<i>n</i> (H·)	$n(CH_4)+2n(H_2)$	$\overline{n(\mathrm{CO}_2)}$	$n(CO_2)$	$\overline{n(CO_2)}$	$n(\mathrm{CO}_2)$	$n(H_2)$	
_		_		-		-	_	
0.18		0.13		0.24		1.88	0.26	Pt/TiO ₂
0.13		0.20		0.31		1.58	0.44	Pt/TiO ₂
0.15		0.24		0.33		1.36	0.57	Pt/TiO ₂
0.14		0.35		0.41		1.18	0.91	Pt/TiO ₂
0.12		0.40		0.49		1.21	1.17	Pt/TiO ₂
0.09		0.46		0.54		1.19	1.49	Pt/TiO ₂
0.13		0.48		0.66		1.38	1.52	Pt/TiO ₂
0.14		0.59		0.81		1.39	2.21	Pt/TiO ₂
0.14		0.59		0.81		1.39	2.20	Pt/TiO ₂

Experimental conditions: photocatalyst concentration = 0.5 g L⁻¹, 0.005 M \leq initial acetic acid concentration (c_0) \leq 5 M, pH 2, suspension volume = 50 mL, irradiation time = 15 h, irradiation intensity I₂₅₀-I₄₅₀ = 30 mW cm⁻².

Figure 42, 43 and Table 4 clearly demonstrate that the change in initial concentration of acetic acid up to 0.05 M ($n_0 = 2500 \mu mol$) results in the formation of reaction products enriched with H₂ (*i.e.*, $\frac{n(CH_4)+n(C_2H_6)}{n(H_2)} < 1$) suggesting the decomposition of CH₃COOH besides other organic compounds formed during the photo-induced transformation of acetic acid. Conversely, an increase in the initial acetic acid concentration ($c_0 > 1$ M ($n_0 = 50000 \mu mol$)) gives the reaction products enriched in hydrocarbons (*i.e.*, $\frac{n(CH_4)+n(C_2H_6)}{n(H_2)} > 1$). Overall, 0.5 M was found to be the optimum initial concentration of aqueous acetic acid in order to obtain both CH₄ and H₂ in significant amounts using Pt/TiO₂ as a photocatalyst.

4.2.3 Effect of pH

The formation rates and corresponding product distribution is known to be strongly dependent on the pH values of the suspension. During photocatalytic degradation of aqueous acetic acid, the experimental results of the present study show CO₂, H₂, CH₄, and C₂H₆ as the main reaction products from a suspension containing Pt/TiO₂ as a photocatalyst and 0.5 M acetic acid at pH 2. However, change in the pH value over the range $2 \le pH \le 11$, results in completely different formation rates and products distribution as presented in Figure 21, 22, 23, and 24. It can be seen in Figure 24, that the amounts of CO₂, H₂, CH₄, and C₂H₆ evolved after 15 h of irradiation are decreasing with increasing pH values. The photonic efficiencies calculated for the main reaction products at different pH regimes are presented in Figure 44. Figure 44 clearly indicates that the initial and overall photonic efficiencies significantly vary for CO₂ at pH 2, whereas for H₂ and CH₄, it did not seem to change greatly. Moreover, at pH 5, no change was observed in the initial and final photonic efficiencies for all reaction products. This means that the reaction rates for all reaction products remains stable over the entire time of illumination at pH 5. This observation could be attributed to the formation of a buffer system (at pH 5) which acts as to resist the changes occurring during the photocatalytic reaction. Also, the overall photonic efficiencies for H_2 evolution reaction were measured to be almost constant over a range of $2 \le pH \le 9$ (Figure 44). However, a sudden decrease in the photonic efficiencies was measured for CO₂ and CH₄ at pH > 5.

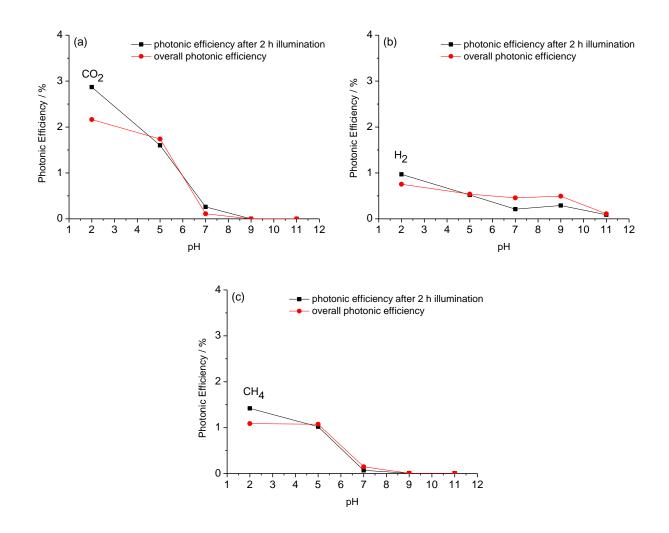


Figure 44: Photonic efficiency for the main reaction products, *i.e.*, (a) CO_2 , (b) H_2 , and (c) CH_4 , calculated for the initial (after 2 h illumination) and overall (after 15 h illumination) formation rates. *Experimental conditions:* as in Figure 21 – 22.

According to the published values of the dissociation constant for acetic acid ($pK_a = 4.75$) [158] and the zero point charge of TiO₂ ($pH_{zpc} \approx 6.25$) [159], three different situations can be assumed in order to explain the different product distribution as shown in Figure 45.

(1) For $pH < pK_a$, the surface of the TiO₂ is saturated with the positive charges whereas acetic acid exists mainly in its protonated form (CH₃COOH).

(2) For $pK_a < pH < pH_{zpc}$, TiO₂ is still positively charged but most of the acetic acid exists in its deprotonated form (CH₃COO⁻) thus a strong attraction between the acetate ions and TiO₂ surface is assumed.

(3) For $pH > pH_{zpc}$, both the surface of TiO₂ and acetate ions are negatively charged, so a repulsion between them is expected. But the adsorption of acetate ion by its methyl group is considered to be more likely in this situation.

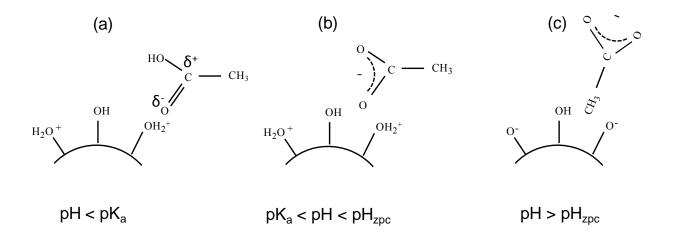


Figure 45: Schematic illustration of the interaction between acetic acid / acetate and the TiO_2 surface in different pH regimes.

During the photocatalytic oxidation of an organic molecule by h_{VB}^+ of the semiconductor, its adsorption onto the surface of semiconductor is a key factor. It can be seen from Figure 45 that the adsorption between acetic acid/acetate ion and the surface of TiO₂ through the carboxylic group of acetic acid/acetate (CH₃COOH/CH₃COO⁻) is possible only in acidic pH medium. Hence, the formation of reaction products resulting from ${}^{\bullet}CH_3$ as the intermediate is more favourable at pH < 7 (Equation 6, Figure 46, and Table 5).

It is also obvious from Figure 46 that the significant amounts of $n({}^{\bullet}CH_3)$ detected by quadrupole mass spectrometer (QMS) only for pH < 7 while an increase in pH (> 7) results in lowering the detection of of $n({}^{\bullet}CH_3)$ intermediate by QMS. Nosaka *et al.* [160] calculated the ratios between amounts of $n({}^{\bullet}CH_3)$ and $n({}^{\bullet}CH_2COOH)$ formed during photocatalytic transformation of 0.1 mol L⁻¹ acetic acid employing Pt/TiO₂ as a photocatalyst. They found that in acidic pH media, almost

75 % of acetic acid molecules are oxidized by a h_{VB}^+ resulting in the formation of ${}^{\bullet}CH_3$ as reaction intermediates (Equation 6). Yoneyama *et al.* [90] also calculated the formed amounts of ${}^{\bullet}CH_3$ for 3.9 < pH < 7.5 with Pt/TiO₂ as a photocatalyst. They observed a decrease in the formation of ${}^{\bullet}CH_3$ by 90 % when pH was changed from 3.9 – 7.5. Same results for total number of ${}^{\bullet}CH_3$ formation over 2 < pH < 11 were given by QMS in this study and can be seen in Figure 46. Therefore, the situation where pH > pH_{zpc}, the dominant reaction for the photocatalytic decomposition of aqueous acetic acid is assumed to be the indirect reaction between acetate ion (CH₃COO⁻) on the side of its methyl group (CH₃) and the ${}^{\bullet}OH$ (generated according to Equation 2) while resulting in the formation of ${}^{\bullet}CH_2COO^-$ intermediate (Equation 4). This argument is based on the results obtained by Wolff and co-workers [80] as discussed in chapter 1.2.4.1.

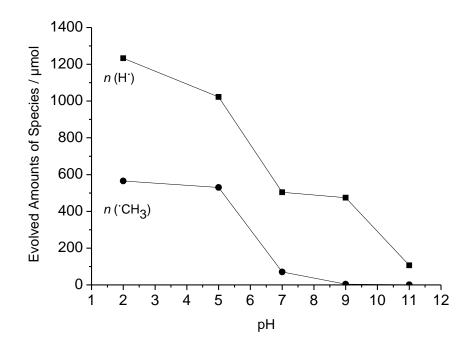


Figure 46: Amounts of H[•], and [•]CH₃, evolved during 15 h of irradiation of aqueous acetic acid in the presence of co-catalyst-loaded TiO₂ *vs.* pH values of the employed suspension. *Experimental conditions*: as in Figure 21 – 22.

1	2	3	4	5	6	7	8	9	10	11	12	13
M/TiO ₂	pH	n_0	<i>n</i> (CO ₂)	$n(H_2)$	$n(CH_4)$	$n(C_2H_6)$	$X_{\rm C}$	$X_{ m H}$	<i>n</i> (H ₂)	<i>n</i> (H ₂)	$n(H_2)$	$n(C_2H_6)$
	_	μmol	μmol	μmol	μmol	μmol	_	_	$n(CO_2)$	$n(CH_4)$	$n(C_2H_6)$	<i>n</i> (CH ₄)
									—	—	—	_
Pt/TiO ₂	2	25000	1027	357	517	24	0.032	0.029	0.34	0.69	15	0.04
Pt/TiO ₂	5	25000	826	256	510	10	0.027	0.026	0.30	0.50	25	0.01
Pt/TiO ₂	7	25000	53	217	70	0.26	0.002	0.007	4.09	3.10	834	0.003
Pt/TiO ₂	9	25000	_	235	4.0	0.18	—	0.004	_	58	1305	0.04
Pt/TiO ₂	11	25000	_	57	0.61	0.01	—	0.001	_	86	5300	0.01

Table 5: Effect of the initial pH value on the amounts of the main reaction products photocatalytically formed during 15 h of irradiation.

Experimental conditions: photocatalyst concentration = 0.5 g L⁻¹, initial acetic acid concentration (c_0) = 0.5 M, 2 ≤ initial pH 2 ≤ 9, n_0 = number of initial acetic acid molecules, suspension volume = 50 mL, irradiation time = 15 h, irradiation intensity I₂₅₀-I₄₅₀ = 30 mW cm⁻².

14	15	16	17	18	19
$\frac{2n(C_2H_6)}{n(CH_4)+2n(C_2H_6)}$	$\frac{n(\cdot \mathrm{CH}_3)}{n(\mathrm{H}\cdot)} = \frac{n(\mathrm{CH}_4) + 2n(\mathrm{C}_2\mathrm{H}_6)}{n(\mathrm{CH}_4) + 2n(\mathrm{H}_2)}$	$\frac{n(\cdot CH_3)}{n(CO_2)} = \frac{n(CH_4) + 2n(C_2H_6)}{n(CO_2)}$	$\frac{n(\mathrm{H}\cdot)}{n(\mathrm{CO}_2)} = \frac{n(\mathrm{CH}_4) + 2n(\mathrm{H}_2)}{n(\mathrm{CO}_2)}$	$\frac{n(\mathrm{CH}_4)+n(\mathrm{C}_2\mathrm{H}_6)}{n(\mathrm{H}_2)}$	pH _
_	-	-	-	_	
0.09	0.46	0.54	1.19	1.49	2
0.04	0.51	0.64	1.23	2.03	5
0.007	0.13	1.33	9.50	0.32	7
0.08	0.009	_	-	0.01	9
0.03	0.005	_	-	0.01	11

Table 5 (continued): Effect of the initial pH value on the amounts of the main reaction products photocatalytically formed during 15 h of irradiation.

Experimental conditions: photocatalyst concentration = 0.5 g L⁻¹, initial acetic acid concentration (c_0) = 0.5 M, 2 ≤ initial pH 2 ≤ 9, n_0 = number of initial acetic acid molecules, suspension volume = 50 mL, irradiation time = 15 h, irradiation intensity I₂₅₀-I₄₅₀ = 30 mW cm⁻².

At pH values 2 and 5, the formed amounts of CH₄ were found to be higher in comparison to the formed amounts of H₂ (Table 5). Other than the formed amounts, the reaction rates also seemed to be quite different when pH of the suspension changes from 2 to 5. Figure 21 illustrates almost constant formation rates during 15 h of illumination for all main reaction products at pH \geq 5. In comparison to this, the formation rates of the main reaction products at pH 2 decreases with the irradiation time. Moreover, the formed amounts of H₂ evolution were found to be in close approximation over a range of 5 \leq pH \leq 9. Zheng *et al.* [100] reported that the significant amounts for H₂ and CH₄ evolution from photocatalytic decomposition of aqueous acetic acidic employing Pt/TiO₂ can only be obtained at acidic pH values. In contrast to the results published by Zheng *et al.* [100] and the results obtained in this work, Sakata and co-workers [37] observed higher amounts of H₂ evolution in alkaline pH medium. Therefore, the reaction pathway for the photocatalytic decomposition of aqueous acetic acid cannot be generalized. Depending on the experimental conditions, it is possible to obtain different product distribution.

It can be seen in Figure 24 that the formation of CO₂ stops at pH > 5. The reason behind this observation is the conversion of CO₂ into carbonate $(CO_3^{2^-})$ and bicarbonate (HCO_{3^-}) at pH \ge 7 [109], thus the detection of CO₂ in the gas phase is not possible. However, CO₂ in the form of $CO_3^{2^-}$ and HCO_{3^-} remain in the suspension. Moreover, the suppression of hydrocarbons formation at pH \ge 7 can be explained with respect to the shift in the position of valence band (VB) and conduction band (CB) of TiO₂ at various pH values. In our study, the value of the flat band potential for TiO₂ P25 has been determined to be: $U_{fb} = -0.58$ V with respect to the normal hydrogen electrode (NHE) at pH 7. Generally, the change in the pH value of the suspension cause a shift in the flat band potential of TiO₂ (Figure 47) according to the following Equation 22:

$$U_{fb}(pH) = U_{fb}(pH0) - 59 \times 10^{-3} \times pH$$
 V vs. NHE Equation 22

It is well known that the band gap (E_g) of TiO₂ P25 is 3.2 eV. According to the relation $E_{VB} = E_{CB} - E_g \approx U_{fb} - E_g$, the VB position of TiO₂ is therefore affected by the change in pH value. Increasing the pH towards more basic regime shifts the VB of TiO₂ towards a more negative value (Figure 47). As a result, the oxidation power of h_{VB}^+ becomes less in order to carry out the oxidation of acetic acid molecule (Figure 37, and 47). It is also reported that the critical potential

value (pH independent) after which the direct h_{VB}^+ oxidation of acetic acid is not possible is \approx + 2.41 V vs. NHE [37, 88, 161, 162]. Thus, the shift in VB position of TiO₂ at pH > 7, which is close to the critical potential values of acetic acid, can explain the suppression of CH₄ formation.

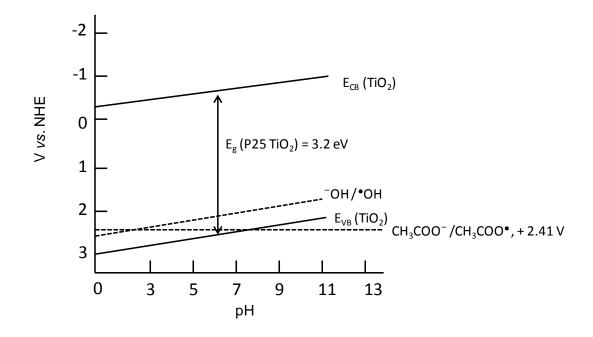


Figure 47: Schematic illustration of energy band diagram for TiO₂ P25 at $0 \le pH \le 11$ along with the one electron oxidation potential of acetate (CH₃COO⁻) [115].

However, the decrease in the formed amounts of all reaction products at pH > 9 also corresponds to the surface agglomeration. In general, at pH > 9, the TiO₂ particles gathered while forming the large aggregates thus affecting the photocatalytic activity [163]. The decrease in the formed amounts of H₂ evolution at pH > 9 can be explained according to surface agglomeration which results in decreasing the surface area of the TiO₂ particles.

4.2.4 Isotopic labelling studies

In a photocatalytic reaction system where H_2 is formed with simultaneous degradation of an organic molecule, controversies exist in the published literature. For instance, according to some researchers during a photocatalytic reaction for simultaneous H_2 production and organic pollutant

degradation, H₂ is formed by a photocatalytic H₂O splitting reaction [103, 164]. In contrast to this, other researchers reported that in the presence of an organic pollutant, H₂ is being formed by the reforming of organic molecules [56, 165]. In order to solve these controversies isotopic labelling experiments have been performed to confirm the origin of H₂ evolution reaction (HER). Most of the published reports explained the HER by means of isotopic labelling experiments for molecules such as CH₃OH [43] or HCHO [166] resulting in only H₂ and CO₂ formation as the final reaction products. Detailed analysis for the isotopic studies of photocatalytic degradation of aqueous acetic acid resulting in H₂ and CH₄ besides CO₂ as main reaction products does not exist in literature. Only few reports are published depicting the HER from photocatalytic transformation of aqueous acetic acid during isotopic labelling experiments [36, 37, 84]. In the present work, we have investigated the effect of various acetic acid (CH₃COOH, CD₃COOD, and CH₃COOD), as well as solvent isotopes (*i.e.*, H_2O/D_2O) on the formation rates and product distribution resulting from photocatalytic conversion of aqueous acetic acid. Additionally, for the first time, proton exchange reaction at both carboxylic and methyl group of aqueous acetic acid in the presence of co-catalyst loaded TiO₂ has been investigated in detail. As already explained in chapter 3.2.5, the employed isotopic reaction systems for the photocatalytic degradation of aqueous acetic acid are as follow: (i) Pt/TiO₂-CH₃COOH-H₂O, (ii) Pt/TiO₂-CD₃COOD-H₂O, (iii) Pt/TiO₂-CH₃COOD-H₂O, (iv) Pt/TiO₂-CD₃COOD-D₂O, (v) Pt/TiO₂-CH₃COOH-D₂O, and (vi) Pt/TiO₂-CH₃COOD-D₂O.

It has been observed in all experimental runs that the photocatalytic transformation of aqueous acetic acid results in the formation of CO_2 as the main reaction product. Using acetic acid and water being different in isotopic composition (i – vi), the formation rates as well as the amounts of the evolved CO_2 during the photocatalytic reaction are presented in Figure 25, 26, 27, and Table 6 respectively. The initial and overall photonic efficiencies calculated for the evolved amounts of CO_2 in all reaction systems (i – vi) are also presented in Figure 48. It can be seen in Figure 48, that the difference between the calculated initial and overall photonic efficiencies is smaller for the reaction systems (iv, v, and vi) having D_2O as a solvent in comparison to the reaction systems (i, ii, and iii) containing H_2O as a solvent. The formation rates and the corresponding formed amounts of CO_2 seemed to be dependent on the employed isotopes (Figure 25, Table 6). For example, the formation rates of CO_2 obtained from reaction systems (iii, iv, and v) containing D_2O as a solvent were observed to be higher as well as more stabilized than the

formation rates of CO_2 acquired from reaction systems (i, ii, and iii) having H_2O as a solvent (Figure 25, Table 6).

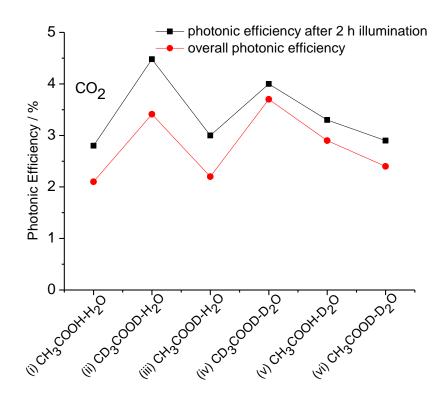


Figure 48: Photonic efficiency of the evolved amounts of CO₂, calculated for the initial (after 2 h illumination) and overall (after 15 h illumination) formation rates for reaction systems (i – vi). *Experimental conditions:* as in Figure 25 - 26.

Additionally, the formation rates and amounts of molecular hydrogen (H₂), molecular deuterium (D₂), and HD from all six reaction systems (i – vi) are presented in Figure 28, 29, 30 and Table 6. Different isotopes *i.e.*, H₂, D₂, and HD were detected from all reaction systems (i – vi) depending on the employed reaction conditions. The photonic efficiencies calculated for H₂ and D₂ evolved from reaction systems (i – vi) are shown in Figure 49. It can be seen in Figure 49, that the reaction systems (i, ii, and iii) having H₂O as a solvent results in a different initial and overall photonic efficiencies. On the other hand, the reaction systems (iv, v and vi) saturated with D₂O exhibits approximately the same initial and overall photonic efficiencies.

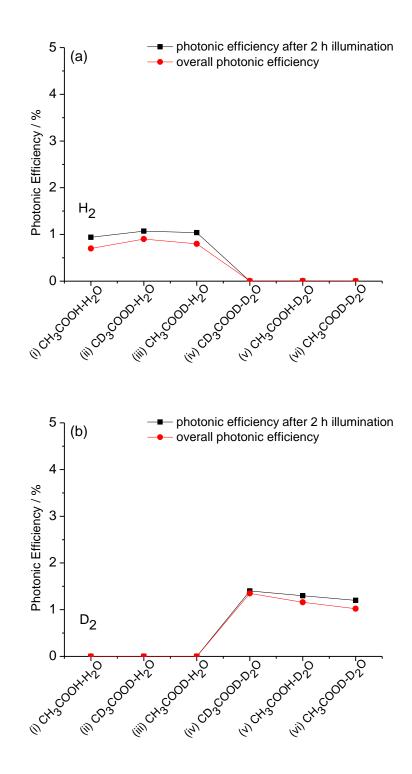


Figure 49: Photonic efficiency of the evolved amounts of (a) H_2 , and (b) D_2 , calculated for the initial (after 2 h illumination) and overall (after 15 h illumination) formation rates for reaction systems (i – iv). *Experimental conditions:* as in Figure 28 – 29.

Sr.	Reaction System	$n(H_2)$	$n(D_2)$	<i>n</i> (HD)	<i>n</i> (CO ₂)	$n(H_2)$	$n(D_2)$	<i>n</i> (HD)
No.						$\overline{n(CO_2)}$	$\overline{n(CO_2)}$	$\overline{n(CO_2)}$
		μmol	μmol	μmol	μmol			
(i)	Pt/TiO ₂ -CH ₃ COOH-H ₂ O	357			1057	0.33		
(ii)	Pt/TiO ₂ -CD ₃ COOD-H ₂ O	421	0.46	1.9	1622	0.26	0.0002	0.001
(iii)	Pt/TiO ₂ -CH ₃ COOD-H ₂ O	377	0.23	1.5	1067	0.35	0.0002	0.001
(iv)	Pt/TiO ₂ -CD ₃ COOD-D ₂ O	3.19	642	11.8	1769	0.001	0.36	0.006
(v)	Pt/TiO ₂ -CH ₃ COOH-D ₂ O	3.77	555	0.35	1404	0.002	0.39	0.0002
(vi)	Pt/TiO ₂ -CH ₃ COOD-D ₂ O	1.09	488	11	1153	0.0009	0.42	0.009

Table 6: Amounts and ratios calculated between the formed amounts resulting from aqueous acetic acid (0.5 M) in the presence of 1wt % Pt/TiO₂ at pH \approx pD = 2.

Table 6 clearly indicates that the reaction systems (i, ii, and iii) containing H_2O as the solvent depict H_2 as the major reaction product while negligible amounts of D_2 and HD were also detected which might come from an impurity. In contrast to this, for reaction systems (iv, v, and vi) D_2 was found to be the dominant reaction product with minor amounts of H_2 and HD, when D_2O was used as the solvent (Table 6).

Overall, the reaction systems having D_2O as solvent or CD_3COOD as sacrificial reagent seem to result in higher reaction rates and higher amounts of the corresponding evolved reaction products (Figure 28, Table 6). For example, the formation rates for D_2 evolution from systems (iv, v, and vi) were observed to be more stable and higher over the entire irradiation time (15 h) in comparison to the H₂ formation rates from systems (i, ii, and iii) (Figure 28).

Moreover, Table 6 and Figure 50 summarize the ratios calculated between the formed amounts of H_2 , D_2 and CO_2 .

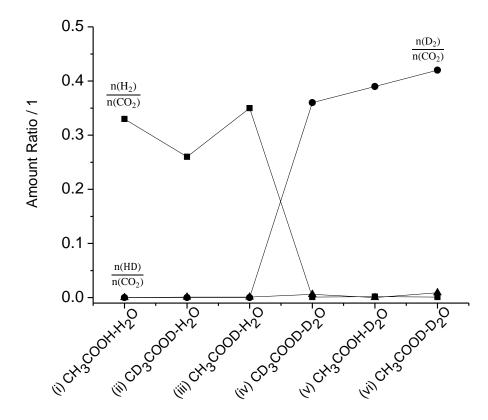


Figure 50: Ratios between the evolved amounts of methane $n(CH_4)$, ethane $n(C_2H_6)$, molecular hydrogen $n(H_2)$, and carbon dioxide $n(CO_2)$ vs. isotopic reaction systems (i – vi). *Experimental conditions:* as in Figure 25 – 30.

It can be seen in Table 6 and Figure 50 that the ratios between the formed amounts of $\frac{n(H_2)}{n(CO_2)}$ and $\frac{n(D_2)}{n(CO_2)}$ for reaction systems containing either (i) H₂O or (iv) D₂O as the solvent, remains almost constant. However, a slight difference (≈ 0.1) between the ratios is observed for H/D mixture reaction systems *i.e.*, ii, iii, v, and vi. Also, negligible amounts of HD do not illustrates any considerable difference for the $\frac{n(HD)}{n(CO_2)}$ ratio.

Moreover, it can be seen in Figure 31, 32, 33, and Table 7 that during the photocatalytic decomposition of aqueous acetic acid employing reaction systems (i – vi), four types of methane being different in isotopic composition *i.e.*, CH₄, CH₃D, CD₃H, and CD₄ were detected by quadrupole mass spectrometer (QMS).

Sr. No.	Reaction System	$n(CH_4)$	$n(CH_3D)$	$n(CD_3H)$	$n(CD_4)$
		μmol	μmol	μmol	µmol
(i)	Pt/TiO ₂ -CH ₃ COOH-H ₂ O	507			
(ii)	Pt/TiO ₂ -CD ₃ COOD-H ₂ O	17.9	121	415	59.3
(iii)	Pt/TiO ₂ -CH ₃ COOD-H ₂ O	501	55.6	14.3	8.04
(iv)	Pt/TiO ₂ -CD ₃ COOD-D ₂ O	2.81	1.05	3.79	1066
(v)	Pt/TiO ₂ -CH ₃ COOH-D ₂ O	112	221	10.4	743
(vi)	Pt/TiO ₂ -CH ₃ COOD-D ₂ O	51.9	147	12.5	690

Table 7: Formed amounts of CH_4 , CH_3D , CD_3H and CD_4 during photocatalytic decomposition of aqueous acetic acid in all reaction systems (i – vi).

For the formation of methane employing reaction systems (i) Pt/TiO₂-CH₃COOH-H₂O, two reaction pathways are reported in literature. For instance, a reaction between ${}^{\circ}CH_3$ and ${}^{\circ}H$, where •H is the product of the reduction of a proton (H^+) formed (1) by deprotonation of CH₃COOH (Equation 6) or (2) by dissociation of solvent (H₂O) (Equation 2) [37]. Clusius et al. [111] investigated a reaction system Pt/TiO₂-CH₃COOH-D₂O, mainly to see the origin for methane formation. They observed CH₃D as the main reaction product when Pt was finely deposited on the surface of photocatalyst. On the other hand, CH_4 was obtained as major reaction product when the Pt particles were present on the surface of TiO_2 in the form of large patches. For the current study, TEM micrographs (Figure 9, and 10) obtained for Pt/TiO₂ particles shows a uniform distribution of Pt particles onto the surface of TiO₂ with a particle size for both Pt and TiO_2 in the range between 15 - 20 nm. Considering the results published by Clusius and coworkers, the major reaction product from reaction systems (v) of this work is expected to be CH₃D. Unexpectedly, the obtained results here from all reaction systems (i - vi) are entirely different in comparison to those already published in literature [37, 84, 111]. Table 6 and Table 7 clearly indicate that a proton exchange reaction at both methyl group and carboxylic group of acetic acid exists in the reaction systems containing H/D mixtures (ii, iii, v, and vi).

Singleton and co-workers [167] investigated the isotopic labelling studies for carboxylic acids. They claimed that the photo-induced conversion of carboxylic acids (RCOOH, R is any atom

attached to carboxylic group) containing H-atoms only results in the formation of large number of by-products. In contrast to this, the photocatalytic transformation of carboxylic acids (RCOOD) where H is replaced by D results in the formation of reaction products more rapidly. Hence, the amounts of formed by-products become lower. This argument seemed to be true in order to explain the results obtained in the present study. If the amounts of formed by-products will be less, there will be more reaction sites available thus facilitating the higher adsorption of acetic acid molecules on to the surface of TiO_2 .

The adsorption of acetic acid molecule is pre-requisite in order to obtain significant photocatalytic activity for all reaction products (chapter 4.2.3). On the other hand, if the generation of by-products during the photocatalytic reaction will be higher, the active reaction sites on the surface of semiconductor might be poisoned thus leading to a lower photocatalytic activity for all reaction products. A comparison among the reaction products evolved from reaction systems (i, ii, iii) having H₂O as a solvent to the reaction systems (iv, v, vi) containing D₂O as a solvent (Figure 25 – 30, and Table 6, and 7) demonstrates that isotopically different solvents affect the formation rates of almost all reaction products. Moreover, a comparison between the reaction rates as well as reaction products evolved from reaction system (ii) Pt/TiO₂-CD₃COOD-H₂O, (iii) Pt/TiO₂-CH₃COOD-H₂O, (v) Pt/TiO₂-CH₃COOH-D₂O, and (vi) Pt/TiO₂-CH₃COOD-H₂O, determines that the photo-decarboxylation is faster for the CD₃COOD species than for CH₃COOH or CH₃COOD species.

It has been reported in literature that the dissociation constant (pK_a) values for carboxylic acids RCOOH having H-atoms is higher in D₂O suspension than in H₂O suspensions [168]. Robinson *et al.* [169] measured the pK_a for the following reaction systems: (1) CH₃COOH in H₂O, pK_a = 4.756, (2) CH₃COOH in D₂O, pK_a = 5.313, (3) CD₃COOD in H₂O, pK_a = 4.771, (4) CD₃COOD in D₂O, pK_a = 5.325. However, at the experimental conditions of the present study (pH \approx pD = 2), different pK_a for CH₃COOH, CD₃COOD, and CH₃COOD do not seems to affect the reaction rates. As explained in chapter 4.2.3, at pH \approx pD = 2, the interaction between positively charged TiO₂ surface and the neutral organic probe molecule will be higher. This means that organic probe molecules will be oxidized by TiO₂ valence band holes (h⁺_{VB}) in all cases (reaction systems (i - vi)) according to the Equation 6. However, it is assumed here that the oxidation of CD₃COOD is faster than CH₃COOH or CH₃COOD by h⁺_{VB} of TiO₂.

Figure 25 and 28 clearly indicate that the reaction rates are higher in the D₂O suspensions (iv, v, and vi) than in H₂O suspensions (i, ii, and iii). It has been reported by Robertson et al. [170] that the employment of isotopically different solvent (H₂O, D₂O) in a photocatalytic reaction system results in different formation rates of the reaction products. The authors claimed that the reaction proceeding by [•]OH is faster than [•]OD because [•]OD has less oxidation energy than [•]OH by a factor of 20 kJ mol⁻¹. However, the results obtained here exhibit higher formation rates (Figure 25 and 28) and corresponding formed amounts (Figure 27, 30 and Table 6) from D₂O suspensions than from H₂O suspensions. Considering the argument about higher oxidation power of [•]OH than [•]OD and the obtained results of this work, it can be concluded that at the employed experimental conditions (pH \approx pD = 2, Pt/TiO₂), the photocatalytic degradation of aqueous acetic acid proceeds mainly by the direct reaction of $TiO_2 h_{VB}^+$ with the organic probe molecule (Equation 6) yielding $^{\bullet}CH_{3}/^{\bullet}CD_{3}$, H^{+}/D^{+} and CO_{2} . Therefore, the obtained formation rates and formed amounts of reaction products are independent of the respective solvent. It should also be noted that in the same reaction system, the reaction pathway where [•]OH/[•]OD reacts with acetic acid molecule yielding [•]CH₂COOH/[•]CD₂COOH/[•]CH₂COOD (Equation 4) also exists as minor reaction pathway. These results are confirmation of proposed reaction mechanism for the photoinduced degradation of aqueous acetic acid in acidic pH media (chapter 4.2.3).

The formed H^+/D^+ according to Equation 6 reduced on the surface of co-catalyst yielding ${}^{\bullet}H/{}^{\bullet}D$, which subsequently dimerize at the surface of co-catalyst while forming H_2/D_2 . The formation of H_2 or D_2 as a major reaction product was observed to be mainly dependent on the solvent being employed.

Table 6 depicts that besides the formation of H_2 and D_2 , HD as another type reaction product was produced in lower amounts. Taking into account the H/D mixture reaction system (ii) Pt/TiO₂-CD₃COOD-H₂O, the step wise formation of H₂, D₂, and HD as a reaction product can be explain according to the Figure 51.

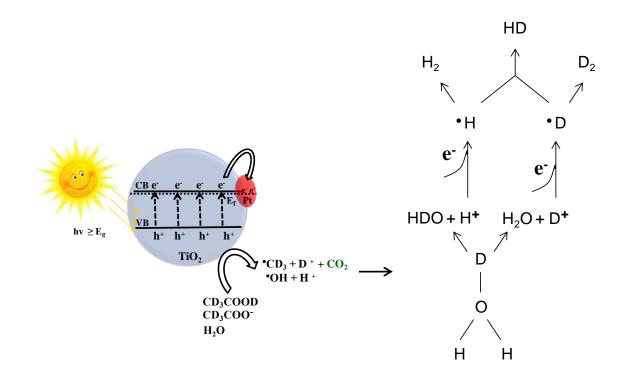


Figure 51: Reaction scheme representing the proton exchange reaction during photocatalytic decomposition of reaction systems (ii) Pt/TiO₂-CD₃COOD-H₂O.

It should also be noted that even if the proton exchange reaction is considered between the systems (ii, iii, v, and vi) where hydrogen and deuterium exist together, the significant amounts of molecular hydrogen and molecular deuterium likely originate from the solvent (Figure 30). It is therefore concluded that due to the proton exchange reaction, the formation of molecular hydrogen is a result of protons from both acetic acid as well as water. However, the ratio between the total number of molecules from acetic acid and solvent is higher. Therefore, it is obvious to get more protons participating in molecular hydrogen from water. However, it has been clarified that the photocatalytic H_2O splitting reaction into H_2 and O_2 does not exist here. The formation of molecular hydrogen coming from water molecules is a result of water dissociation reaction into H^+ and $^{\bullet}OH$ (Equation 2).

To confirm the proton exchange reaction determined by quadrupole mass spectrometer (QMS), reaction systems (ii) Pt/TiO₂-CD₃COOD-H₂O and (v) Pt/TiO₂-CH₃COOH-D₂O were also tested by nuclear magnetic resonance (NMR) spectroscopy. The NMR spectroscopy was performed for the samples (1) before illumination (Figure 34, 35) and (2) after illumination (Figure 36). It can be seen in Figure 34, 35, and 36 that new peaks appeared in the NMR spectra only for irradiated suspensions. For the reaction system (ii) Pt/TiO₂-CD₃COOD-H₂O, the formation of quintet signal exhibited by NMR spectrometer which corresponds to CD₂HCOOD(H) species evidently confirms the occurrence of a proton exchange at the methyl group of acetic acid during a photocatalytic reaction. The same results were also obtained for reaction system (v) Pt/TiO₂-CH₃COOH-D₂O, where the NMR spectrum depicts the formation of a triplet signal corresponding to CH₂DCOOH(D) species. It should also be noted that the suspensions do not show any resonance signals corresponding to new species before illumination (Figure 34, and 35). This means that the proton exchange reaction is typically a photo-induced reaction occurring at the surface of co-catalyst (Figure 52) instead of a thermal reaction. The proton exchange caused by thermal process cannot be completely excluded here because of the presence of Pt nanoparticles. However, with respect to the illumination time of the suspension, the occurrence of proton exchange by thermal process at the methyl group of acetic acid is insignificant.

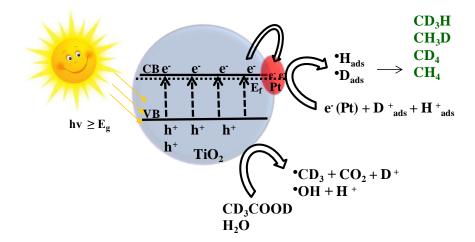


Figure 52: Reaction scheme representing the proton exchange reaction during photocatalytic decomposition of reaction systems (ii) Pt/TiO₂-CD₃COOD-H₂O.

4.3 Mechanistic considerations

4.3.1 Basic processes for the photocatalytic degradation of aqueous acetic acid

According to the above mentioned results and discussion, the fundamental process for the photoinduced transformation of aqueous acetic acid in acidic pH media over co-catalyst loaded TiO₂ can be proposed as: (1) generation of charge carriers (h_{VB}^+ and e_{CB}^-) upon light illumination (Equation 23), (2) the reactions of the photo-generated charge carriers with the species adsorbed on the surface of photocatalyst as well as co-catalyst (*i.e.*, Pt) (Equation 24 – 25) and (3) subsequent reactions between the formed transient radical intermediates (Equation 26 – 29).

$TiO_2 + hv$	\rightarrow	$TiO_2(e_{CB}^- + h_{VB}^+)$	Equation 23
$TiO_2(h_{VB}^+) + CH_3COOH$	\rightarrow	$TiO_2 + CH_3COO^{\bullet} + H^+$	Equation 24
$TiO_2(e_{CB}^-) + H_{ads}^+$	\xrightarrow{Pt}	$TiO_2 + \bullet H_{ads}$	Equation 25
$\bullet H_{ads} + \bullet H_{ads}$	\xrightarrow{Pt}	H ₂	Equation 26
CH₃COO•	\rightarrow	$^{\bullet}CH_3 + CO_2$	Equation 27
$^{\bullet}CH_3 + ^{\bullet}H_{ads}$	\xrightarrow{Pt}	CH ₄	Equation 28
$\bullet CH_3 + \bullet CH_3$	\rightarrow	C_2H_6	Equation 29

Generally, the direct transfer of h_{VB}^+ is supposed to occur among the semiconductor surfacebound species *e.g.*, H₂O molecule while forming H⁺ as well as [•]OH. Moreover, a reaction between the light-induced h_{VB}^+ and semiconductor surface adsorbed CH₃COOH molecule also occurs resulting in the formation of CH₃COO[•] followed by the decomposition of CH₃COO[•] into the methyl radical ([•]CH₃) and CO₂ as shown in Equation 24 and 27. During the photocatalytic decomposition of aqueous acetic acid employing either bare TiO₂ or metal loaded TiO₂, the generation of [•]CH₃ as a reaction intermediate has been confirmed *via* EPR studies [84, 160, 171-173]. Various published reports also demonstrated the occurrence of surface methylation due to a rapid reaction of [•]CH₃ with different metals such as Pt, Au, and Ag as well as metal-oxides *e.g.*, TiO₂, and CuO nanoparticles [174-179]. As a result of surface methylation, (1) the positively charged surface of photocatalyst at acidic pH might form the agglomerates of nanoparticles due to the reduction in the surface charge or (2) active sites required to carry out the photocatalytic reaction might be blocked. Consequently, the photocatalytic activity for the degradation of organic compound will be suppressed [180]. In addition to this, the band positions are known to be shifted due to the generation of metal-hydrogen (metal-H) as well as metal-carbon (metal-C) bonds at the surface of respective metals. Hence, an interfacial electron transfer between metal nanoparticles and the redox species is affected to a great extent [135, 136]. This might be a reason of decrease in reaction rates with increasing illumination time in all experimental runs of the present study (Figure 14, 15, 18, and 21).

During the light-induced transformation of aqueous acetic acid using metal or metal-oxide loaded TiO₂, production of the important gases that can be used as solar fuels *i.e.*, H₂ and CH₄, is defined by the reactions presented in Equation 26 and 28, respectively. Here, the e_{CB}^- act as to reduce the Pt-surface adsorbed protons (H⁺_{ads}) while resulting adsorbed H-atoms (${}^{\bullet}H_{ads}$) (Equation 25). Subsequently, a radical-radical reaction at the surface of Pt occurs while giving rise to the formation of H₂ (Equation 26) or CH₄ (Equation 28). Moreover, the formation of C₂H₆ arises by the dimerization of two ${}^{\bullet}$ CH₃ as given in Equation 29. It can be seen in Table 3 – 5 (Column 14) that from total number of ${}^{\bullet}$ CH₃ formed under experimental conditions of this study, almost 5 – 18 % dimerize evolving C₂H₆ as the final product. The estimated percentage has been calculated by doing a rough calculation of formed amounts of ${}^{\bullet}$ CH₃ (= *n*(CH₄) + 2*n*(C₂H₆)).

The reaction pathway for the photocatalytic decomposition of aqueous acetic acid at acidic pH media (Equation 23 – 29) depicts that the ratio of the formed ${}^{\bullet}CH_3$ ($n({}^{\bullet}CH_3) = n(CH_4) + 2n(C_2H_6)$) amounts and ${}^{\bullet}H$ ($n({}^{\bullet}H) = n(CH_4) + 2n(H_2)$) amounts should be equal to 1. However, Table 3 – 5 (column 15) and Figure 53 demonstrate the calculated ratio from the quantified experimental data as < 1.

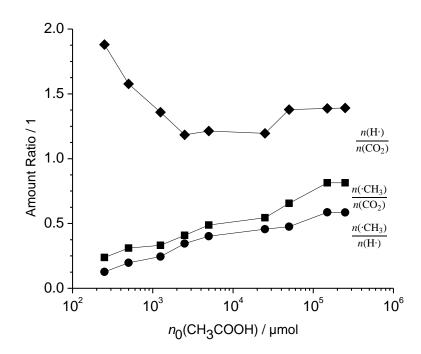


Figure 53: Ratios between the detected amounts of hydrogen atoms $n(^{\bullet}H)$, methyl radicals $n(^{\bullet}CH_3)$, and carbon dioxide $n(CO_2)$ vs. the initial amount n_0 of acetic acid. *Experimental conditions:* as in Figure 18 – 19.

This means that during the photocatalytic reaction, either (1) the oxidation of ${}^{\bullet}CH_3$ and evolved hydrocarbons took place, or (2) CH₃COOH transforms into other organic compounds (not quantified in the present study). This argument is based on the following explanation:

(1) According to the reaction Equation 27, the photo-decarboxylation of CH₃COO[•] should give a ratio between formed amounts of [•]CH₃ and CO₂ as: $\frac{n(\cdot \text{CH}_3)}{n(\text{CO}_2)} = 1$. It can be seen in Table 3 and 4 (column 16) and Figure 53 that under the experimental conditions of the current study, the maximum value calculated for $\frac{n(\cdot \text{CH}_3)}{n(\text{CO}_2)}$ ratio is equal to 0.81. (2) Based upon the stoichiometric calculations (Equation 23 – 29) during the photo-induced decomposition of aqueous acetic acid, the expected amounts for H₂ and C₂H₆ formation should be equal ($n(\text{H}_2) = n(\text{C}_2\text{H}_6)$), while the ratio between $\frac{n(\cdot\text{H})}{n(\text{CO}_2)}$ should be unity. In contrast to this, the analysis of the obtained data depicts

the formation of H₂ with comparatively higher amounts than C_2H_6 ($n(H_2) > n(C_2H_6)$) in all experimental runs as can be seen in Table 3 – 5 (column 5, and 7). The, calculated ratio between the formed amounts of [•]H and CO₂ is found to vary in the range of 1.88 – 0.73 as given in Table 3, and 4 (column 17) and Figure 39.

These calculations clearly indicate the formation of higher amounts of H_2 and CO_2 than expected from the stoichiometry of the reaction, thus, confirming the formation of other organic molecules than CH_4 and C_2H_6 . These formed organic compounds are then assumed to further decompose evolving H_2 and CO_2 as the reaction products. The formation of organic molecules other than CH_4 and C_2H_6 during the photocatalytic conversion of aqueous acetic acid can be explained according to reaction Equations 30 - 39:

\rightarrow	$TiO_2 + \bullet OH + H^+$	Equation 30
\rightarrow	$TiO_2 + ^{\bullet}OH$	Equation 31
\rightarrow	$^{\bullet}CH_{2}COOH + H_{2}O$	Equation 32
\rightarrow	C ₂ H ₅ COOH	Equation 33
\rightarrow	$\mathrm{TiO}_{2} + \mathrm{C}_{2}\mathrm{H}_{5}\mathrm{COO}^{\bullet} + \mathrm{H}^{+}$	Equation 34
\rightarrow	$^{\bullet}C_{2}H_{5} + CO_{2}$	Equation 35
$\stackrel{Pt}{\rightarrow}$	C_2H_6	Equation 36
\rightarrow	C ₃ H ₈	Equation 37
\rightarrow	CH ₃ OH	Equation 38
\rightarrow	C ₂ H ₅ OH	Equation 39
	$\begin{array}{c} \rightarrow \\ \rightarrow \\ \rightarrow \\ \rightarrow \\ \rightarrow \\ \rightarrow \\ Pt \\ \rightarrow \\ \rightarrow \\ \rightarrow \\ \rightarrow \end{array}$	$ \rightarrow \qquad TiO_2 + {}^{\circ}OH $ $ \rightarrow \qquad {}^{\circ}CH_2COOH + H_2O $ $ \rightarrow \qquad C_2H_5COOH $ $ \rightarrow \qquad TiO_2 + C_2H_5COO^{\circ} + H^+ $ $ \rightarrow \qquad {}^{\circ}C_2H_5 + CO_2 $ $ \begin{array}{c}Pt \\ \rightarrow \\ Pt \\ \rightarrow \\ C_2H_6 \end{array} $ $ \rightarrow \qquad C_3H_8 $ $ \rightarrow \qquad CH_3OH $

In general, other than the employed organic molecule (CH₃COOH in this study), the h_{VB}^+ also react with the H₂O molecules adsorbed on the surface of the TiO₂ as well as ⁻OH present at the surface of TiO₂ yielding [•]OH as a reaction intermediate (Equation 30 – 31) [14]. The abstraction of H[•] from CH₃COOH molecule by reaction with the [•]OH yields [•]CH₂COOH (Equation 32). During the photo-induced decomposition of aqueous acetic acid, the existence of [•]CH₂COOH has been confirmed *via* EPR spectroscopy [160, 171-173]. Hydrogen (H[•]) abstraction from CH₃COOH by [•]OH is known to occur only at the α -position of acetic acid as given in Equation 40. Depending on the pH values of the employed suspension, the rate constant for this reaction is reported to be $\geq 1 \times 10^9$ L mol⁻¹ s⁻¹ [181]. Therefore, the abstraction of H[•] from CH₃COOH molecule yielding CH₃COO[•] according to the reaction Equation 40 is unlikely to take place.

$$CH_3COOH + {}^{\bullet}OH \rightarrow CH_3COO^{\bullet} + H_2O$$
 Equation 40

The abstraction of H[•] from CH₃COOH molecule by its reaction with a [•]CH₃ yielding [•]CH₂COOH as reaction intermediate and CH₄ as the final reaction product (Equation 41) has been reported in literature [37, 90, 171]. Rate constants for this reaction are reported as: 2×10^2 and 6×10^2 L mol⁻¹s⁻¹ [182, 183]. This reaction is therefore assumed to be a minor reaction.

$$CH_3COOH + {}^{\bullet}CH_3 \rightarrow {}^{\bullet}CH_2COOH + CH_4$$
 Equation 41

On the contrary, the removal of H[•] from organic probe molecules by their reaction with a H[•] (Equation 42 - 44) are known to have higher rate constants (< 1×10^5 , 2.3×10^6 and 9.8×10^4 L mol⁻¹ s⁻¹) [184].

$$^{\bullet}H_{ads} + CH_4 \rightarrow H_2 + ^{\bullet}CH_3 Equation 42 ^{\bullet}H_{ads} + C_2H_6 \rightarrow H_2 + ^{\bullet}C_2H_5 Equation 43 ^{\bullet}H_{ads} + CH_3COOH \rightarrow H_2 + ^{\bullet}CH_2COOH Equation 44$$

It is assumed that the formation of ${}^{\bullet}CH_2COOH$ predominantly occurs *via* reaction 32. The reaction given by Equation 41 and 44 are only minor reaction pathways.

According to the qualitative analysis *via* QMS, traces for propane (C_3H_8) formation have been observed in this work. The formation of C_3H_8 can be defined according to the radical-radical reaction between ${}^{\bullet}CH_2COOH$ and ${}^{\bullet}CH_3$ forming propanoic acid (C_2H_5COOH) (Equation 33) followed by its oxidation by h_{VB}^+ and resulting in the formation of ${}^{\bullet}C_2H_5$ and CO_2 (Equation 34 – 35). The formed ${}^{\bullet}C_2H_5$ further reacts with a ${}^{\bullet}CH_3$ and yields C_3H_8 as the final reaction product (Equation 37).

Many reports are published in literature discussing the photocatalytic transformation of aqueous acetic acid into hydrocarbons (*e.g.*, CH₄, C₂H₆) and other organic compounds under anaerobic

suspension [35, 37, 83, 94, 112, 185]. The formation of comparatively minor amounts of propane (C₃H₈) as another hydrocarbon besides the evolution of CH₄ and C₂H₆ has also been reported [35, 112, 185, 186]. Moreover, ${}^{\bullet}C_{2}H_{5}$ can also react with ${}^{\bullet}H_{ads}$ resulting in the formation of C₂H₆ as the final reaction product (Equation 36).

It is clear from Figure 23 that the formation of organic molecules (C_xH_{2x+2} with $x \le 3$) as byproducts occurred during the photocatalytic conversion of aqueous acetic acid. Sakata et al. [37] studied the photocatalytic decomposition of aqueous acetic acid employing Pt/TiO₂ as a photocatalyst at pH 2.1. They performed vapour phase analysis of the irradiated suspensions and observed the formation of CH₃OH, C₂H₅OH, (CH₃)₂CO, and C₂H₅COOH as reaction products in the liquid phase. In comparison to the carbon bound reaction products present in the gas phase, the carbon-contents in the liquid phase calculated from the given data were approximately 1.4% only. Mozia et al. [35] also carried out the liquid phase analysis of the suspension obtained after the photocatalytic degradation reaction of aqueous acetic acid employing Fe-modified TiO_2 as a photocatalyst. The authors reported the formation of CH₃OH, C₂H₅OH, (CH₃)₂CO, CH₃CHO, and CH₃COOCH₃ as the reaction products, but the amounts of these products were detected to be \leq 10µM. Hamid and co-workers discussed the details about the possible reaction pathways for the formation of reaction products in the liquid phase [83]. As the formed amounts of liquid phase reaction products were reported to be very low, it is supposed that the oxidation of the carbon contents present in these organic probe molecules result in the formation of CO₂ and H₂ as the final reaction products.

The possible reaction paths for the formation of alcohols are given in Equations (38 - 39). It should also be kept in mind that a reaction between alkyl radicals and the surface of TiO₂ might result in the alkylation of the TiO₂ surface thus leading to the formation of methanol and other organic compounds by hydrolysis of the chemical bond as shown in Equation 45 - 46.

$\equiv \mathrm{Ti} - \mathrm{O} - \mathrm{CH}_2 \mathrm{R} + \mathrm{H}_2 \mathrm{O}$	\rightarrow	\equiv Ti – OH + RCH ₂ OH	Equation 45
$\equiv Ti - O - CH_2R + -OH$	\rightarrow	$\equiv Ti - 0^- + RCH_2OH$	Equation 46

Kandiel and co-workers [34, 187] explained the transformation of aqueous CH_3OH into HCHO and HCOOH formation, which are then subsequently oxidized to form H_2 and CO_2 as the final

reaction products. Figure 23 exhibits the traces of HCHO and HCOOH detected by QMS in the gas phase exiting the photoreactor, hence, confirming the formation of alcohols as a side product during photocatalytic decomposition of aqueous acetic acid. The reaction pathways for the oxidation of C_2H_5OH into H_2 and CO_2 are also reported in literature [188-190].

The photocatalytic reaction rates were found to be dependent on the pH value of the suspensions containing semiconductor materials and organic molecules (Figure 21). For instance, Kormann and co-workers [159] reported the effect of pH values on the photocatalytic reaction rates with respect to both electrostatic attractive and repulsive interactions among TiO₂ surface charge and organic probe molecules. The organic compound used in their studies was trichloroacetic acid and bis (2-chloroethyl) amine. In the present study, a decreasing trend in the formation of hydrocarbons was observed when the pH values increased towards more basic region (Figure 24, Table 5). It is also clear from reaction Equations 28 and 29 that the formation of hydrocarbons requires the presence of an alkyl radical as a reaction intermediate. It should also be noted that significant amounts of [•]CH₃ can only be generated when the adsorption of CH₃COOH from the side of carboxylic group (COOH) on TiO₂ surface is preferred (Figure 45). In results of such adsorption, the decomposition of acetic acid proceeds by a direct reaction between h_{VB}^+ and acetic acid molecule (Equation 24). Nevertheless, this situation is favourable only in acidic suspensions. Hamid et al. [83] investigated the effect of various pH values by photoelectrochemical studies employing Pt/TiO₂ electrodes and acetic acid. They obtained higher photocurrents during photocatalytic oxidation of acetic acid at pH 2 in comparison to the photocurrents obtained at pH 9. Thus, the authors claimed a higher adsorption of acetic acid molecule onto the surface of TiO_2 in acidic pH media than in alkaline pH medium. This means, at basic pH medium acetate molecules adsorb on the surface of TiO_2 by the side of its methyl group thus leading to the formation of [•]CH₂COO⁻ (Equation 32) intermediate in higher amounts. Consequently, the reaction will follow a different pathway leading to the other reaction products (Equation 33). Even though, the number of formed ${}^{\bullet}CH_3$ becomes less at pH \geq 7, the formation of ${}^{\bullet}CH_3$ as a reaction intermediate cannot be completely ruled out. However, the subsequent reaction products from ${}^{\bullet}CH_3$ at pH \geq 7 are different from those formed at pH \leq 7. The results obtained here, clearly indicate the formation of H₂ as the only product formed in significant amounts at $pH \ge 7$ (Figure 23, Table 5). The formation of H_2 in alkaline media can be attributed to the decomposition of alcohols or organic acids into H_2 and CO_3^2 -or HCO_3 - which was formed during the photocatalytic transformation of aqueous acetic acid [83]. It has been shown in literature that during photocatalytic transformation of alcohols, a change in pH does not affect the formation rate of H_2 evolution significantly [34].

Moreover, the formation of organic acids yielding H_2 as the reaction product can be explained according to the following reactions (Equation 47 - 49):

$$^{\circ}OH + ^{\circ}CH_2COO^- \rightarrow HOCH_2COO^-$$
 Equation 47

There is also a possibility that [•]CH₂COO⁻ reacts with the surface of TiO₂ (Equation 47):

$$\equiv Ti - 0 - CH_2COO^- + ^-OH \rightarrow \equiv Ti - 0^- + HOCH_2COO^-$$
Equation 48
HOCH_2COO^- \rightarrow CHOCOO^- + H_2 Equation 49

The formation of hydrocarbons (CH₄, C₂H₆) in smaller amounts at pH \geq 7 (Table 5) indicates that the direct hole oxidation reaction between TiO₂ h⁺_{VB} and acetate molecules exists as a minor reaction (Equation 24). Therefore, the formation of alcohols or organic acids at pH > 7 must be a rapid reaction.

4.3.2 Kolbe vs. Hofer-Moest reaction mechanism

According to the above mentioned results and discussion, it is concluded that the photocatalytic transformation of aqueous acetic acid at acidic pH values results in the formation of reaction products rich in hydrocarbons. For example, CH₄ was detected in larger amounts along with C_2H_6 and C_3H_8 as minor reaction products. This confirms that in acidic suspensions (pH < 7, 0.5 M acetic acid, and Pt/TiO₂), the photo-induced transformation of aqueous acetic acid mainly follows a photo-Kolbe reaction mechanism. According to the Kolbe mechanism, hydrocarbons as well as CO_2 are formed as main reaction products. It should also be noted that under acidic conditions the formation of alcohols as minor reaction products have also been detected in this study. This suggests that besides the photo-Kolbe mechanism, there exists another reaction pathway for the

photocatalytic decomposition of aqueous acetic acid which is known as Hofer-Moest reaction. According to the Hofer-Moest reaction, alcohols and aldehydes are formed as the reaction products. On the other hand, in alkaline suspensions (pH > 7, 0.5 M acetic acid, Pt/TiO₂), the formation of H₂ is monitored as the main reaction product while hydrocarbons are produced in negligible amounts. Hence, the dominant reaction pathway for acetic acid decomposition at pH > 7 is assumed to be the Hofer-Moest reaction. However, the existence of photo-Kolbe mechanism as minor reaction pathway at pH > 7 cannot be excluded [191-193].

4.3.3 Proton exchange reaction

It has been observed here, that the formation of the fuels such as H_2 and CH_4 requires the presence of hydrogen atom (Equation 26, and 28). Therefore, the investigations regarding the origin of hydrogen atoms participating in H_2 and CH_4 generation are very important. For this purpose, isotopic labelling experiments with different isotopes of acetic acid and water have been performed here. A detailed discussion about isotopic labelling studies has been given in chapter 4.2.4. Briefly, for a reaction system containing Pt/TiO₂ as a photocatalyst in acidic (pH \approx pD = 2) media with CD₃COOD and H₂O, a rapid proton exchange reaction exists which can be explain as follow (Equation 50):

$$CD_3COOD + H_2O$$
 \rightleftharpoons $CD_3COOH + HOD$ Equation 50

For the photocatalytic reaction systems (ii) $Pt/TiO_2-CD_3COOD-H_2O$, upon light illumination, the formation of H_2 , D_2 or HD can be explained according to the following reactions (Equation 51 – 57).

$TiO_2(h_{VB}^+) + CD_3COOD$	\rightarrow	$TiO_2 + CD_3COO^{\bullet} + D^+$	Equation 51
CD ₃ COO●	\rightarrow	$^{\bullet}\mathrm{CD}_3$ + CO_2	Equation 52
$TiO_2(e_{CB}^-) + D_{ads}^+$	$\stackrel{Pt}{\rightarrow}$	•D _{ads}	Equation 53
$TiO_2(e_{CB}^-) + H_{ads}^+$	$\stackrel{Pt}{\rightarrow}$	•H _{ads}	Equation 54

$^{\bullet}D_{ads}$ +	•D _{ads}	\xrightarrow{Pt}	D ₂	Equation 55
•H _{ads} +	•H _{ads}	\xrightarrow{Pt}	H ₂	Equation 56
•D _{ads} +	•H _{ads}	\xrightarrow{Pt}	HD	Equation 57

However, the chemistry of ${}^{\circ}CH_{3}/{}^{\circ}CD_{3}$, resulting from the light induced decomposition of carboxylic acids (Equation 27, and 52) has been discussed by many researchers using QMS and NMR spectroscopic techniques [84, 194-197]. Usually, the proton exchange reaction occurring at methyl group (CH₃/CD₃) of carboxylic acids in H/D mixture reaction systems is categorized in two types: (1) single exchange reaction, and (2) multiple exchange reaction. The responsible factors, according to which the protons exchange reaction proceeds by single exchange or multiple exchanges, are as follow: (1) particle size of co-catalyst deposited on the surface of semiconductor material, (2) temperature of the reaction system, and (3) pressure [198, 199]. Depending on the reaction conditions, if a single exchange reaction repeated multiple times (Equation 58), the same reaction products are obtained which might be formed during a multiple exchange reaction.

$$CH_3 \xrightarrow{Pt} CH_2D \xrightarrow{Pt} CHD_2 \xrightarrow{Pt} CD_3$$
 Equation 58

Kemball *et al.* [200] reported that the single exchange reaction does not require elevated temperature value for their occurrence and can be proceed at ambient temperature. In contrast to this, for a multiple exchange reaction, temperature value > 300 °C are required. The experiments of the present study have been performed at ambient temperature. Therefore, it is assumed that in this study, for the suspensions containing H/D mixtures, a single exchange reaction occurs multiple times hence resulting in the formation of methane being different in isotopic composition (Table 7). Moreover, the importance of Pt nanoparticles cannot be neglected when a proton exchange reaction is considered. It has been reported by Khodakov *et al.* [201] that the irradiation of suspensions containing isotopically different carboxylic acids results in the adsorption of ${}^{\bullet}H/{}^{\bullet}D$ and ${}^{\bullet}CH_{3}/{}^{\bullet}CD_{3}$, there appear surface methyl groups thus undergoing proton exchange according to Equation 58. It has also been reported by Khodakov and co-

workers that the size of Pt nanoparticles plays a very important role in defining the rate of proton exchange reaction. The authors claimed that the large Pt particle size results in lower proton exchange reaction rate while small particle size of Pt leads to the higher reaction rates for proton exchange reaction [201]. The particle size of the Pt nanoparticles used in the present study was found in the range of 15 - 25 nm (Figure 9 - 10). Hence, a single proton exchange reaction at the surface of Pt nanoparticles is assumed to occur in this study.

Here, blank experiments in the absence of Pt co-catalyst and TiO₂ photocatalyst employing following reaction systems have also been performed and tested by NMR: (1) TiO₂-CH₃COOH- D_2O , (2) TiO₂-CD₃COOD-H₂O, (3) CH₃COOH- D_2O , and (4) CD₃COOD-H₂O. Data obtained from both QMS and NMR spectroscopic techniques (data not shown here) do not show any proton exchange for these systems. These results lead to the conclusion that the proton exchange is a photocatalytic reaction which occurs either at the surface of Pt or TiO₂ following the pathways of single exchange reaction occurring multiple times. Moreover, due to a rapid exchange between H and D of methyl group, carboxylic group as well as solvent molecules under illumination, the protons participating in the formation of methane are assumed to come from both solvent and organic acid. However due to a big difference between the concentration of solvent and organic molecules, the main source of $^{\bullet}$ H, required for the formation of molecular hydrogen and methane is solvent.

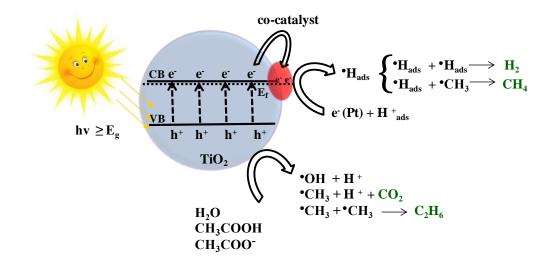
5. Summary and conclusions

The pioneering work of Bard and co-workers published in 1980's demonstrated the photocatalytic decomposition of aqueous acetic acid into carbon dioxide (CO₂), molecular hydrogen (H₂) and hydrocarbons (*i.e.*, CH₄, C₂H₆) under anaerobic conditions employing both co-catalyst loaded TiO₂ particles and TiO₂ electrodes. However, controversies still exist in literature while discussing the reaction mechanism for the photocatalytic decomposition of aqueous acetic acid. A slight change in the reaction parameters leads to an entirely different product distribution, reaction rates and reaction pathways for the photo-induced degradation of aqueous acetic acid. The scientific question of the present thesis was to investigate the factors influencing the stoichiometry and reaction mechanism for the photocatalytic degradation of aqueous acetic acid in detail.

The photocatalytic experiments were performed in a photoreactor attached to a quadrupole mass spectrometer (QMS) which allows continuous detection of the evolved gaseous products. In general, it has been observed from most of the experimental runs performed in this work that the photo-induced transformation of aqueous acetic acid results in the formation of CO_2 , H_2 , and CH_4 as major reaction products, while traces of C_2H_6 as minor reaction product were also detected. However, the formation rates and distribution of these major and minor reaction products were found to be greatly affected by the employed reaction conditions. Along with the major and minor reaction products (*i.e.*, CO_2 , H_2 , CH_4 , and C_2H_6), QMS also depicts the formation of many side-products (*e.g.*, alcohols, organic acids, and aldehydes) in the gas phase exiting the photoreactor. However, evolved amounts of these by-products was close to the detection limit of QMS, therefore, quantitative analysis for only major reaction products were carried out.

In order to check the influence of TiO_2 surface modifications on the reaction rates and product distribution resulting from the photocatalytic conversion of aqueous acetic acid, experiments were performed with bare as well as various metals and metal oxides loaded TiO_2 particles. Bare TiO_2 exhibits an insignificant photocatalytic activity for all major and minor reaction products (*i.e.*, CO_2 , H₂, CH₄, and C₂H₆) formed during photocatalytic decomposition of aqueous acetic acid. On the other hand, the loading of noble metals such as Pt, Rh, Au, Ag, and metal-oxides such as IrO_2 and RuO_2 on the surface of TiO_2 act as an efficient electron traps and significantly improves the photocatalytic activity for the light-induced decomposition of aqueous acetic acid

into CO₂, H₂, CH₄, and C₂H₆ (Scheme 1). The choice of these particular metals or metal-oxides was made on the basis of their work function values. In order to obtain higher photocatalytic activity, it is necessary to use co-catalysts having work function values larger than the work function value of the photocatalyst. The comparison of the obtained results shows that TiO_2 loaded by different metals and metal oxides results in the formation of same reaction products (*i.e.*, CO₂, H₂, CH₄, and C₂H₆) but entirely different formation rates and products distribution. The noble metal co-catalysts having higher work function values such as Pt, Rh, and Au observed to favour the reduction reaction (*i.e.*, formation of H₂) more significantly as compared to Ag having a lower value of work function. The amounts of the evolved H₂ employing various metals loaded TiO₂ increase in the following order: Ag/TiO₂ < Au/TiO₂ < Rh/TiO₂ < Pt/TiO₂. At the same time, the noble metal co-catalysts also act as to improve the separation of photogenerated charge carriers (e_{CB}^{-} and h_{VB}^{+}) thus enhancing the oxidation reaction (*i.e.*, formation of CO₂, and CH₄) in the same order. On the contrary, independent of the work function values, metal oxide co-catalysts such as IrO₂ and RuO₂ did not seem to be good candidates for H₂ evolution reaction but produced higher amounts of CO2 and CH4. The formed amounts of CO2 and CH4 employing IrO₂/TiO₂ were observed to be comparable with the amounts obtained by using Pt/TiO₂ as a photocatalyst.



Scheme 1: Schematic illustration for the photocatalytic decomposition of aqueous acetic acid over co-catalyst loaded TiO₂ particles.

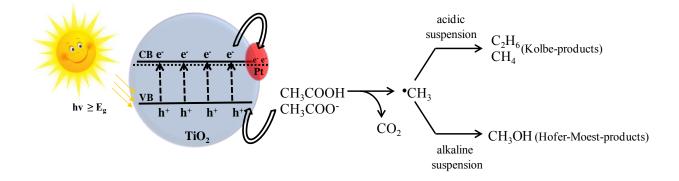
These observations suggest that the choice of a suitable co-catalyst which can carry out both oxidation and reduction reaction at the same time is very important. The idea behind this work was to choose an appropriate photocatalytic reaction system, which can be used to obtain significant amounts of future renewable energy fuels (i.e., H_2 and CH_4). Here, the data analysis shows Pt/TiO₂ photocatalyst as the aspirant resulting in the formation of both oxidation and reduction products simultaneously with significant amounts. Thus, Pt/TiO₂ was employed as the photocatalyst to answer the further scientific questions of the present study.

Generally, in a photocatalytic reaction, the concentration of an organic electron donor is known to affect the reaction rates to a great extent. To study the effect of probe compound on the reaction rates and product distribution, experiments were performed employing various initial concentrations (c_0) of acetic acid using Pt/TiO₂ as a photocatalyst at pH 2. Once again, the obtained results from all experiments resulted in the formation of CO₂, H₂, CH₄, and C₂H₆ as main reaction products. However, the product distribution was observed to vary greatly. An increase in the initial concentration from 0.005 M to 0.05 M was found to favour the formation of the H₂ as the principal reaction product while the formation of CH₄ was comparatively suppressed at these concentration values. Comparatively, a further increase in the initial concentration values between 0.05 M $< c_0 \leq 5$ M gives the reaction products rich in hydrocarbons (i.e., CH₄). Moreover, an increase in the initial concentration of acetic acid from 0.005 M to 5 M (0.005 M $\leq c_0 \leq 5$ M) was found to show a decrease in the ratio $\frac{n(H_2)}{n(CO_2)}$ and an increase in the ratio $\frac{n(CH_4)}{n(CO_2)}$ while the ratio $\frac{n(C_2H_6)}{n(CH_4)}$ was observed to be constant for all employed concentration values. An overall analysis of the obtained results determines that at 0.5 M concentration of acetic acid, both important energy fuels (i.e., H₂ and CH₄) can be obtained in significant amounts. Therefore, the concentration of acetic acid was chosen to be 0.5 M for further analysis in this research.

The experiments for the photocatalytic decomposition of 0.5 M aqueous acetic acid employing Pt/TiO₂ as a photocatalyst were performed for $2 \le pH \le 11$. The obtained results at pH < 7 exhibit that the initial step for the light-induced decomposition of aqueous acetic acid predominantly follows the photo-Kolbe reaction mechanism. According to the photo-Kolbe mechanism, under light illumination, a direct reaction between TiO₂ photo-generated h_{VB}^+ and CH₃COOH adsorbed on the surface of TiO₂ results in the formation of °CH₃ as a reaction intermediate and CO₂ as reaction product. The formed °CH₃ then gives alkanes (Scheme 2) as the

reaction product. According to the stoichiometric calculations of CH₃COOH, it is expected that the photo-induced transformation of aqueous acetic acid should result in the following atomic ratios: $\binom{n(C)}{n(O)}=1$, $\frac{n(H)}{n(O)}=2$, and $\frac{n(H)}{n(C)}=2$). However, the obtained atomic ratios of the reaction products at pH 2 are: $(0.6 < \frac{n(C)}{n(O)} < 0.9, 1.0 < \frac{n(H)}{n(O)} < 2.0, and <math>1.4 < \frac{n(H)}{n(C)} < 2.1$). These calculations clearly demonstrate that there exist other products instead of the main reaction products (CO₂, H₂, CH₄, and C₂H₆). The qualitative analysis from QMS also confirms the formation of other organic probe molecules (C_xH_{2x+2}, x ≤ 3) formed during the photocatalytic transformation of aqueous acetic acid. This means that besides the photo-Kolbe reaction mechanism, the photocatalytic decomposition of aqueous acetic acid simultaneously follows another reaction pathway which is called as Hofer-Moest reaction. According to the Hofer-Moest reaction products. The initial step for Hofer-Moest reaction also includes the direct oxidation of CH₃COOH into [•]CH₃ and CO₂ by TiO₂ h⁺_{VB}. Afterwards, the formed [•]CH₃ results in the formation of alcohols (Scheme 2).

The formation rates and the product distribution were observed to be strongly affected by change in initial pH values of the employed suspensions. For example, an increase in the pH value from 2 to 5 exhibits a slight decrease in the formed amounts of H₂, while CH₄ and CO₂ remained almost constant. A further increase in pH value between $5 < pH \le 9$, depicts almost constant and significant amounts of H₂ evolution while a rapid decrease in the formed amounts of CO₂, CH₄, and C_2H_6 was observed. At pH > 7, CO₂ cannot be detected in the gas phase due to its conversion into carbonate/bicarbonate (CO_3^{2-} and $HCO_{3^{-}}$) which stays in the liquid phase in the suspension. However, the suppression of hydrocarbons at pH > 7 clearly indicates that the photo-Kolbe reaction mechanism exists here as a minor reaction pathway. Also, H_2 formation at pH > 7 as the only reaction product evolved in significant amounts demonstrates that the reaction proceeds mainly by a Hofer-Moest mechanism. The formed Hofer-Moest reaction products such as alcohols and organic acids are further oxidized resulting in the formation of H₂ and CO₂ as the final reaction products. For pH > 7, insignificant amounts of evolved hydrocarbons depict that, under alkaline pH regime, Kolbe mechanism also exists as a minor reaction pathway. Further analysis shows that pH > 9 results in a decreasing trend for H_2 evolution. Studies confirmed that at pH \geq 10, TiO₂ particles exhibit surface agglomeration, hence, affecting the photocatalytic activity. This argument matches well with the obtained results of the present investigation. Thus, the pH 2 was found to be optimized value where both H_2 and CH_4 can be obtained with maximum observed formation rates.



Scheme 2: Schematic illustration for the Photo-Kolbe vs. Hofer-Moest reaction mechanisms.

Isotopic labelling experiments were performed by using isotopically different (1) solvents (H_2O/D_2O) and (2) organic molecule (CH₃COOH, CD₃COOD, CH₃COOD) employing Pt/TiO₂ as a photocatalyst at pH = pD \approx 2. The detail of reaction systems is as follow: (i) Pt/TiO₂-CH₃COOH-H₂O, (ii) Pt/TiO₂-CD₃COOD-H₂O, (iii) Pt/TiO₂-CH₃COOD-H₂O, (iv) Pt/TiO₂-CD₃COOD-H₂O, (v) Pt/TiO₂-CH₃COOH-D₂O, and (vi) Pt/TiO₂-CH₃COOD-D₂O.

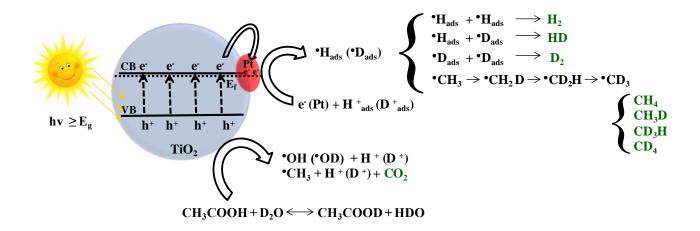
From all six reaction systems (i – vi), an obvious difference in the formed amounts of CO₂ was observed. The reaction systems containing D₂O as a solvent (iv, v, and vi) exhibited higher reaction rates for CO₂ formation in comparison to the reaction systems (i, ii, and iii) having H₂O as a solvent. However, independent from the employed solvent, the photo-decarboxylation rate of CD₃COOD was found to be faster than CH₃COOH and CH₃COOD. These results suggested that in acidic suspensions, the photocatalytic decomposition of aqueous acetic acid mainly proceed by a direct reaction between the TiO₂ valence band hole (h_{VB}^+) and acetic acid molecule yielding Kolbe-products. However, the occurrence of Hofer-Moest reaction as a minor pathway cannot be excluded.

The analyses of data for hydrogen evolution reaction from all reaction systems (i - vi) determines that the main source for molecular hydrogen evolution is the solvent. For example, the reaction systems (i, ii, and iii) containing H₂O as a solvent yield H₂ as a major reaction product. On the other hand, the reaction systems (iv, v, and vi) having D₂O as a solvent yield D₂ as the main reaction product. Considering a proton exchange reaction between the reaction systems being

5. Summary and conclusions

different in isotopic composition (ii, iii, v, and vi)), it was concluded that the protons participating in the formation of molecular hydrogen originates from both organic molecule and the solvent. However, due to a large excess of solvent molecules in comparison to organic molecule, the main source for molecular hydrogen formation was the solvent. Nevertheless, the participation of proton coming from organic acid in the formation of molecular hydrogen cannot be neglected.

The results obtained by quadrupole mass spectrometer (QMS) depict the formation of four types of methane being different in isotopic composition (*i.e.*, CH₄, CH₃D, CD₃H, and CD₄). A proton exchange was found at both the methyl group and the carboxylic group of acetic acid. The observed proton exchange mainly at the methyl group of acetic acid was further confirmed *via* nuclear magnetic resonance (NMR) spectroscopy. It was revealed by ¹H NMR that during a photocatalytic reaction for systems (ii) Pt/TiO₂-CD₃COOD-H₂O and (v) Pt/TiO₂-CH₃COOH-D₂O, the transformations exist as follow: CD₃COOD \rightarrow CHD₂HCOOH(D) and CH₃COOH \rightarrow CDH₂HCOOH(D), respectively. A schematic illustration for proton exchange reaction is given in Scheme 3.



Scheme 3: Schematic illustration for the proton exchange reaction during photocatalytic decomposition of aqueous acetic acid over Pt/TiO_2 particles.

Blank experiments such as: (1) before illumination (ii) $Pt/TiO_2-CD_3COOD-H_2O$, and (v) $Pt/TiO_2-CH_3COOH-D_2O$, and (2) after illumination (vii) $TiO_2-CD_3COOD-H_2O$, and (viii) $TiO_2-CH_3COOH-D_2O$, were also performed and tested by NMR spectroscopy. Blank experiments confirmed that the proton exchange between the solvent and reactant is a photo-induced reaction which occurs mainly at the surface of Pt co-catalyst. Due to the proton exchange reaction at both methyl and carboxylic group of acetic acid, once again it is concluded that the protons participating in the formation of methane originates from both reactant acid and the solvent.

Hence, the obtained experimental results within this thesis suggest that, with a suitable combination of co-catalyst loaded photocatalyst, the photocatalytic degradation of industrial waste can be efficiently obtained either in the favour of a mixture of gasses rich in hydrocarbons and poor in molecular hydrogen or vice versa. This terminology would be greatly helpful to fulfil the requirements of natural gases.

6. References

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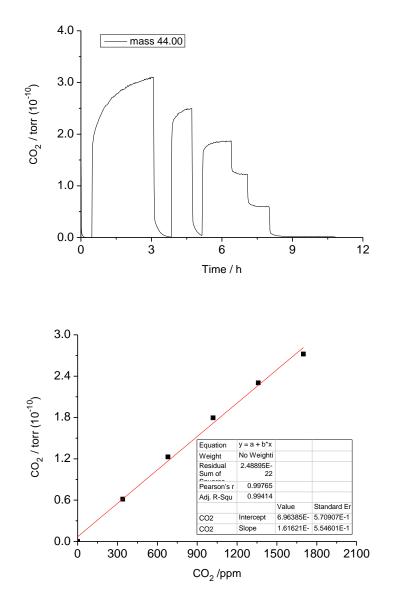
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7. Appendix

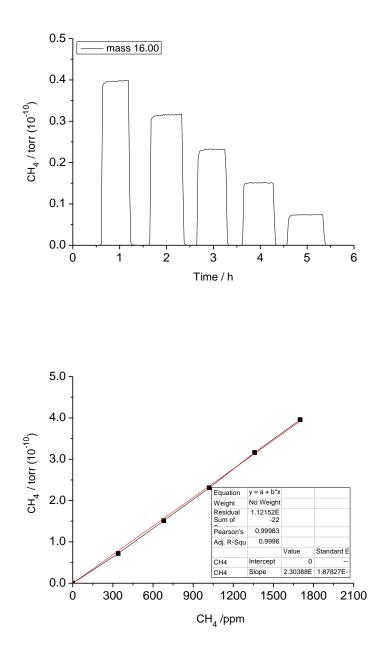
7.1 Additional information

Calibration curves for the main reaction products obtained by QMS.

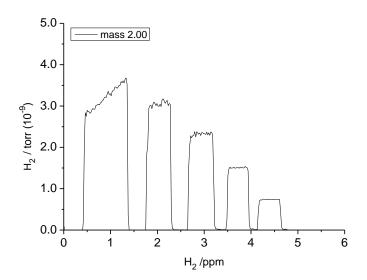
• $CO_2 = mass \ 44.00$

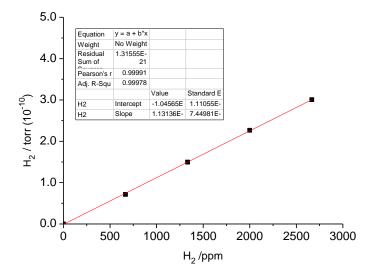


• $CH_4 = mass \ 16.00$



• $H_2 = mass \ 2.00$





7.2 Publications

Published papers

1. **S. Hamid**, R. Dillert, D.W. Bahnemann, Photocatalytic reforming of aqueous acetic acid into molecular hydrogen and hydrocarbons over cocatalyst-loaded TiO₂: shifting the product distribution, Journal of Physical Chemistry C (2018), *In press*.

2. **S. Hamid**, I. Ivanova, T.H. Jeon, R. Dillert, W. Choi, D.W. Bahnemann, Photocatalytic conversion of acetate into molecular hydrogen and hydrocarbons over Pt/TiO_2 : pH dependent formation of Kolbe and Hofer-Moest products, Journal of Catalysis, 349 (2017) 128 – 135.

3. H. Belhadj, **S. Hamid**, P.K. Robertson, D.W. Bahnemann, Mechanisms of Simultaneous Hydrogen Production and Formaldehyde Oxidation in H_2O and D_2O over Platinized TiO₂, ACS Catalysis, 7 (2017) 4753 – 4758.

4. I. Ivanova, **S. Hamid**, J. Schneider, D. W. Bahnemann, New insights into the photocatalytic hydrogen production: mechanistic aspects and material design, Current Topics in Catalysis, 12 (2016) 81 – 99.

5. J. Nie, A.O. Patrocinio, **S. Hamid**, F. Sieland, J. Sann, S. Xia, D. W. Bahnemann, J. Schneider, New Insights into the Plasmonic Enhancement for Photocatalytic H_2 Production by Cu-TiO₂ upon Visible Light Illumination, Physical Chemistry Chemical Physics, (2018) 5264 – 5273.

6. S. Naskar, F. Lübkemann, S. Hamid, A. Freytag, A. Wolf, J. Koch, I. Ivanova, H. Pfnür, D. Dorfs, D.W. Bahnemann, Synthesis of Ternary and Quaternary Au and Pt Decorated CdSe/CdS Heteronanoplatelets with Controllable Morphology, Advanced Functional Materials, 27 (2017) 1 -11.

7. G. Yang, D. Chen, H. Ding, J. Feng, J.Z. Zhang, Y. Zhu, **S. Hamid**, D.W. Bahnemann, Welldesigned 3D ZnIn₂S₄ nanosheets/TiO₂ nanobelts as direct Z-scheme photocatalysts for CO₂ photoreduction into renewable hydrocarbon fuel with high efficiency, Applied Catalysis B: Environmental, 219 (2017) 611 - 618.

Submitted papers

1. **S. Hamid**, J. Schneider, R. Dillert, D.W. Bahnemann, Spectroscopic analysis of proton exchange during the photocatalytic decomposition of aqueous acetic acid: an Isotopic study on product distribution and reaction rate, Revision submitted to ACS Catalysis (2018).

2. N. Karamat, M. F. Ehsan, M. N. Ashiq, S. Ijaz, M. N. Haq, **S. Hamid**, D. W. Bahnemann, LaNdZr₂O₇ supported SnSe nanocomposites for the photocatalytic CO_2 reduction and Foron blue dye degradation, Major revision submitted to Applied Surface Science (2018).

7.3 Conferences and presentations

7.3.1 Oral presentations

<u>S. Hamid</u>, I. Ivanova, T.H. Jeon, R. Dillert, W. Choi, D.W. Bahnemann, 'Photocatalytic conversion of acetate into molecular hydrogen and hydrocarbons over surface modified TiO_2 : pH dependent formation of Kolbe and Hofer-Moest products' at 28th International Conference on Photochemistry (ICP), Strasbourg, France, July 16 – 21, 2017.

<u>S. Hamid</u>, J. Schneider, R. Dillert, D.W. Bahnemann, 'Spectroscopic analysis of proton exchange for the photocatalytic transformation of aqueous acetic acid: an isotopic study', AdvPhotoCat-E 2017, Heraklion, Greece, July 14 - 16, 2017.

<u>S. Hamid</u>, I. Ivanova, R. Dillert, D.W. Bahnemann 'Factors influencing the photocatalytic decomposition of aqueous acetic acid over TiO_2 : a mechanistic study", The 21st International Conference on Semiconductor Photocatalysis Solar Energy Conversion (SPASEC-21), Atlanta, Georgia, United States of America, November 13 – 17, 2016.

<u>S. Hamid</u>, I. Ivanova, R. Dillert, D.W. Bahnemann, 'The pH dependent photocatalytic decomposition of aqueous acetic acid into hydrogen and hydrocarbons over platinized-TiO₂', New Photocatalytic Materials for Environment, Energy and Sustainability (NPM-1), Gottingen, Germany, June 6 - 10, 2016.

<u>S. Hamid</u>, I. Ivanova, D.W. Bahnemann, 'Effect of various sacrificial reagents on the TiO_2 photocatalyzed hydrogen production', 3rd German Russian summer school, Saint Petersburg, Peterhof, Russia, June 15 – 18, 2015.

7.3.2 Poster presentations

<u>S. Hamid</u>, I. Ivanova, D.W. Bahnemann, 'The pH dependent photocatalytic decomposition of aqueous acetic acid into hydrogen and hydrocarbons over platinized- TiO_2 ', Nanoday 2016, Laboratoriumfür Nano- und Quantenengineering, Hannover, Germany, September 29, 2016.

<u>S. Hamid</u>, I. Ivanova, D.W. Bahnemann, 'Methanol and aodiumacetate as electron donors for the photocatalyzedhydrogen production on surface-modified-TiO₂', Nanoday 2015, Laboratoriumfür Nano- und Quantenengineering, Hannover, Germany, October 1st, 2015.

<u>S. Hamid</u>, I. Ivanova, D.W. Bahnemann, 'Methanol and sodium acetate as electron donors for the photocatalyzed hydrogen production on surface-modified-TiO₂', Photocatalytic and Advanced Oxidation Technologies for the Treatment of Water, Air, Soil and Surfaces (PAOT-3), Gdansk, Poland, September 1 - 4, 2015.

8. Curriculum vitae

Personal information:

Last Name, First Name	Hamid, Saher
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Marital Status	Married

Education and training:

From 03/2015 to 06/2018: PhD Student/ Research Assistant at Institut für Technische Chemie (Photocatalysis and Nanotechnology), Leibniz Universität Hannover under the supervision of Prof. Dr. Detlef W. Bahnemann.

From 09/2013 to 11/2014: Research Assistant at National Centre for Nanoscience and Technology, University of Chinese Academy of Sciences, Beijing, China.

From 12/2010 to 10/2012: Masters of Science (M.S.) in Nanotechnology, Centre of Excellence in Solid State Physics, University of the Punjab, Lahore, Pakistan.

From 10/2006 to 08/2010: Bachelors of Science (B.sc (Hons.)) in Computational Physics, Centre for High Energy Physics, University of the Punjab, Lahore, Pakistan.